

1  
2  
3  
4  
5  
6  
7  
8  
9  
10  
11  
12  
13  
14  
15  
16  
17  
18  
19  
20  
21  
22  
23  
24  
25  
26

## Functionalized halloysite nanotubes for enhanced removal of lead(II) ions from aqueous solutions

Salvatore Cataldo<sup>a</sup>, Giuseppe Lazzara<sup>a</sup>, Marina Massaro<sup>b</sup>, Nicola Muratore<sup>a</sup>, Alberto Pettignano<sup>a\*</sup>,  
Serena Riela<sup>b\*</sup>

<sup>a</sup> Dipartimento di Fisica e Chimica, Università di Palermo, Viale delle Scienze, I-90128 Palermo, Italy

<sup>b</sup> Dipartimento di Scienze e Tecnologie Biologiche, Chimiche e Farmaceutiche. Università di Palermo, Viale delle Scienze, I-90128, Palermo, Italy

\* Corresponding authors: Tel: +39-091-23897959

E-mail addresses: [alberto.pettignano@unipa.it](mailto:alberto.pettignano@unipa.it); [serena.riela@unipa.it](mailto:serena.riela@unipa.it)

---

### ABSTRACT

In this study, environmental friendly halloysite nanotubes and their amino derivatives were used as adsorbent materials for lead(II) ions. The adsorption ability of both nanomaterials towards Pb<sup>2+</sup> ions has been studied in NaCl<sub>aq</sub>, at  $I = 0.1 \text{ mol L}^{-1}$ , in the pH range 3 – 6. Moreover, the effect of ionic strength on the adsorption process was evaluated at the pH of maximum efficiency of the adsorbent materials. Kinetic and equilibrium experiments were carried out by using the Differential Pulse Anodic Stripping Voltammetry (DP-ASV) technique to check the metal ion concentration in solution after contact with the two adsorbents. Different isotherm and kinetic equations were used to fit the experimental data. The speciation of metal ion and the characterization of the adsorbents with different techniques were considered in order to establish the suitable experimental conditions for the metal ion removal. The collected data showed that the functionalization of halloysite

27 enhances the adsorption ability of the clay mineral and it makes the nanoclay a good candidate for  
28 metal removal from aqueous solutions.

29

30 **Keywords:** Halloysite, grafting, lead(II), adsorption, ionic strength.

---

31

## 32 **1. Introduction**

33 Industrial and agricultural activities, together with vehicle traffic emission, are the main causes of  
34 heavy metals pollution. Toxic metals are persistent in the environment and accumulate in terrestrial  
35 and aquatic ecosystems with serious consequences for human health (Förstner et al., 1995). Among  
36 them, lead is considered one of the most toxic towards living organisms and a long term exposure  
37 can cause a serious damage to different organs and disease of cardiovascular, nervous and immune  
38 systems. (Mason et al., 2014; Gidlow, 2015)

39 During the last decade various nanomaterials are extensively used in the heavy metal ions removal  
40 from aqueous solutions or from soils. Among them, clay minerals have gathered particular interest  
41 owing to their unique features such as, high specific surface area, low toxicity and natural  
42 availability at low price (Dong et al., 2012; Cataldo et al., 2015). Halloysite nanotubes (Hal) are  
43 particular clay minerals with a predominantly hollow tubular structure (Joussein et al., 2005). Hal  
44 are chemically similar to the platy kaolin and possess a peculiar chemical composition of the  
45 surfaces. They consist in 10-15 aluminosilicate layers with an external surface constituted by  
46 siloxane groups and an inner lumen composed of aluminol groups. Owing to this peculiar  
47 composition, Hal are positively charged in the interior whereas a negative charge is present on the  
48 external surface in a wide pH range. This charge separation is related to the acid-base properties of  
49 functional groups of Hal studied in a recent article (Bretti et al., 2016). The different surface  
50 chemistry allows to the selective functionalization at the inner or outer side making possible the  
51 synthesis of several nanomaterials with hierarchical nanostructure (Cavallaro et al., 2014). The  
52 covalent modification of the outer surface is most commonly achieved by grafting silanes via

53 condensation between hydrolyzed silanes and the surface hydroxyl groups of the Hal located on the  
54 edges or on external surface defects (Yuan et al., 2008; Yuan et al., 2012; Tan et al., 2016; Sabbagh  
55 et al., 2017). According to Yuan et al. the Al-OH groups present in the Hal lumen possess high  
56 degree of chemical reactivity towards organosilane. On the contrary, the external surface of Hal  
57 nanotubes consists of siloxane (Si-O-Si) groups and few silanols (Si-OH). However, due to the  
58 presence of some surface defects more hydroxyl groups exist on the surface of Hal nanotubes.  
59 These hydroxyl groups are the potential reactive sites for the surface modification on the external  
60 surface of Hal nanotubes which increased the interaction of organosilanes with Hal nanotubes  
61 (Yuan et al., 2008) as reported by other authors (Rawtani et al., 2017; Sadjadi and Atai, 2018).

62 The functionalization of Hal surfaces opens up several application fields, where halloysite hybrids  
63 can be successful applied. Therefore, functionalized halloysite was used as filler for polymer or  
64 hydrogel matrices (Liu et al., 2010; Fan et al., 2013; Silva et al., 2013), drug carrier and delivery  
65 (Lvov et al., 2015; Liu et al., 2016; Lvov et al., 2016; Massaro et al., 2016a), catalyst support  
66 (Massaro et al., 2016b) as well as adsorbent (Peng et al., 2015). In this context Hal have been  
67 considered ideal alternatives for the preparation of adsorbents for removal of different kinds of toxic  
68 metal ions or organic contaminants from wastewaters or from polluted soils (Zhao et al., 2013;  
69 Kurczewska et al., 2015; Maziarz et al., 2015; Hebbbar et al., 2016; Matusik, 2016; Meng et al.,  
70 2016; Zeng et al., 2016; Zhu et al., 2017). Indeed, respect to other nanoclay, the possibility to  
71 adsorb pollutants both in Hal lumen and on Hal external surface, increases the removal efficiency  
72 (Zhao et al., 2013).

73 Generally, pristine Hal (p-Hal) can remove heavy metal ions from aqueous media through the  
74 mechanisms of site geometry, physical and/or chemisorption and so on. However, application of  
75 these materials as adsorbents of pollutants is limited by their low loading capacity, less metal ion  
76 binding active-sites, and low selectivity to specific metals. (Zhu et al., 2017) To enhance the  
77 loading capacity and the affinity toward heavy metal ions, p-Hal can be functionalized with some  
78 interesting nanomaterials and/or functional groups to endow them with the extra mechanism of

79 complexation (Matusik, 2014; Massaro et al., 2017). Zhu et al. (Zhu et al., 2017) reported the  
80 synthesis of a new nanoadsorbent based on Hal for the simultaneous removal of Cr(VI) and Sb(V)  
81 from wastewater. In order to improve heavy metal adsorption efficiency halloysite was also  
82 functionalized with hexadecyltrimethylammonium bromide. The as prepared adsorbent was applied  
83 to remove Cr(VI) from aqueous solution showing faster adsorption rate and higher adsorption  
84 capacity.(Jinhua et al., 2010)

85 With the final goal to obtain good adsorbent for toxic metal ions herein we report a thorough study  
86 of the amino functionalized halloysite (Hal-NH<sub>2</sub>) adsorption ability towards Pb<sup>2+</sup> ions. FT-IR, TGA  
87 and SEM techniques and contact angle measurements were used to characterize the adsorbent  
88 material whilst Differential Pulse Anodic Stripping Voltammetry (DP-ASV) technique was used to  
89 check the metal ion concentration in solution during the batch kinetic and thermodynamic  
90 adsorption experiments. A speciation study of p-Hal and of Pb<sup>2+</sup> ions using literature formation  
91 constants (Baes and Mesmer, 1976; Luo and Millero, 2007; Bretti et al., 2016) was done to find the  
92 best experimental conditions for the metal ion removal. Sodium chloride was used as background  
93 and different ionic strengths were considered in the experiments.

94

## 95 **2. Materials and Methods**

96

### 97 **2.1 Reagents.**

98 p-Hal were a commercial product (Sigma, lot MKBQ8631V) and were used after washing with  
99 ultra pure water and drying in oven at  $T = 110$  °C. The 3-azidopropyltrimethoxysilane was  
100 synthesized as previously reported (Massaro et al., 2016b). NaCl salt (Riedel-de Haën, puriss.) used  
101 to set the ionic strength of the solutions at desired values was weighed after drying in oven at 110  
102 °C for 2 h. Hydrochloric acid and sodium hydroxide used to adjust the pH of the metal ion solutions  
103 were prepared by diluting concentrated Fluka ampoules and standardized against sodium carbonate  
104 and potassium hydrogen phthalate, respectively, previously dried in an oven at  $T = 110$  °C. Pb(II)

105 ion solutions were prepared by weighing the  $\text{Pb}(\text{NO}_3)_2$  (Aldrich, analytical grade) salt. Standard  
106 solutions of  $\text{Pb}(\text{II})$  ions used for calibration curves were prepared by diluting a  $1000 \text{ mg L}^{-1}$   
107 standard solution in 2%  $\text{HNO}_3$  ( $C \pm 0,2\%$  - trace select quality, FLUKA). All the solutions were  
108 prepared using freshly,  $\text{CO}_2$ -free ultra pure water ( $\rho \geq 18 \text{ M}\Omega \text{ cm}$ ) and grade A glassware.

109

## 110 ***2.2 Synthetic run and characterization of Hal-NH<sub>2</sub> nanomaterial***

111 In a typical synthetic run, 4 g of 3-azidopropyl trimethoxysilane were dissolved in 60 mL of dry  
112 toluene and 2 g of clay mineral powder were added. The clay mineral was first dispersed under  
113 ultrasonic irradiation for 15 min, and then refluxed for 48 h under stirring. Afterwards, the crude  
114 solid was filtered off, washed with several aliquots of  $\text{CH}_2\text{Cl}_2$  and  $\text{CH}_3\text{OH}$  and dried overnight at 80  
115 °C under vacuum. The so obtained nanomaterial was re-suspended in DMF and triphenylphosphine  
116 ( $\text{PPh}_3$ ) was added to the reaction mixture. The dispersion was left to stir at room temperature for 1h.  
117 After this time a  $\text{NH}_3$  aqueous solution (2 mL) was added dropwise. After 5 days the solvent was  
118 filtered off and the powder was washed several times with  $\text{CH}_2\text{Cl}_2$  and finally dried at 50 °C under  
119 vacuum.

120 Contact angle measurements were performed by using an optical contact angle apparatus (OCA 20,  
121 Data Physics Instruments) equipped with a video measuring system having a high-resolution CCD  
122 camera and a high-performance digitizing adapter. SCA 20 software (Data Physics Instruments)  
123 was used for data acquisition. To obtain a tablet, the powder like material was pressed under  $104 \text{ kg}$   
124  $\text{cm}^{-2}$  for 10 min. The contact angle of water in air was measured by the sessile drop method. The  
125 water droplet volume was  $10.0 \pm 0.5 \text{ mL}$ . Temperature was set at  $25.0 \pm 0.1 \text{ °C}$  for the support and  
126 the injecting syringe as well. Images were collected 25 times per second. From the data analysis the  
127 contact angle, the volume and the contact area of the drop were calculated. The volume of the  
128 droplet was constant within the time of the experiment.

129 FT-IR spectra in KBr were determined at room temperature in the spectral region 400–4000  $\text{cm}^{-1}$  by  
130 means of an FT-IR spectrophotometer (Agilent Technologies Cary 630). An average of 30 scans per  
131 sample using a nominal resolution of 4  $\text{cm}^{-1}$  was registered.

132 The thermogravimetric analysis was performed by means of a Q5000 IR apparatus (TA  
133 Instruments) under the nitrogen flow of 25  $\text{mL min}^{-1}$  for the sample and 10  $\text{mL min}^{-1}$  for the  
134 balance. The mass of each sample was ca. 5 mg. The calibration was carried out by means of Curie  
135 temperature of standards (nickel, cobalt, and their alloys). The sample was heated from room  
136 temperature to 900  $^{\circ}\text{C}$  with a scanning rate of 20  $^{\circ}\text{C min}^{-1}$ . The degradation temperature ( $T_d$ ) was  
137 taken at the maximum of the first order derivative curve of mass loss versus temperature (DTG  
138 curves).

139 The microscope ESEM FEI QUANTA 200F was used to study the morphology of the  
140 functionalized Hal. Before each experiment, the sample was coated with gold in argon by means of  
141 an Edwards Sputter Coater S150A to avoid charging under electron beam.

142

### 143 ***2.3 Procedures for kinetic and thermodynamic experiments***

144 The kinetic experiments for  $\text{Pb}^{2+}$  ion adsorption by p-Hal and Hal- $\text{NH}_2$  were carried out in NaCl  
145 aqueous solution, at  $I = 0.1 \text{ mol L}^{-1}$ , in the pH range 3 – 6 and at  $T = 25 \text{ }^{\circ}\text{C}$ . ~15 mg of p-Hal or  
146 Hal- $\text{NH}_2$  were added to 25 mL of the metal ion solution ( $C_{\text{Pb}^{2+}} = 30 \text{ mg L}^{-1}$ ) placed in a  
147 voltammetric cell under constant and regular agitation. The metal ion concentration in solution was  
148 measured at various adsorbent/solution contact times in the interval 0 - 360 min. The solution pH  
149 was monitored during the experiments.

150 The adsorption isotherm experiments were carried out in the same ionic medium and pH range of  
151 kinetic ones, at  $I = 0.10 \text{ mol L}^{-1}$  and  $T = 25 \text{ }^{\circ}\text{C}$ . Moreover, at pH = 5 the experiments were extended  
152 at the ionic strengths 0.25 and 0.5  $\text{mol L}^{-1}$ . For each pH and ionic strength, ~ 15 mg of p-Hal or Hal-  
153  $\text{NH}_2$  were placed in 9 Erlenmeyer flasks containing 25 mL of Pb(II) solution at different

154 concentrations in the range  $5 \leq C_{\text{Pb}^{2+}} / \text{mg L}^{-1} \leq 50$ . The solutions were stirred at 180 rpm for twelve  
155 hours using an orbital mixer (model M201-OR, MPM Instruments) and then were separated from  
156 the adsorbent before measuring the pH and the  $\text{Pb}^{2+}$  concentration.

157 Recycling and reuse experiments were done on the Hal-NH<sub>2</sub> material. To this end, ~40 mg of the  
158 adsorbent were placed in an Erlenmeyer flask containing 25 mL of Pb(II) solution ( $C_{\text{Pb}^{2+}} \approx 30 \text{ mg L}^{-1}$ )  
159 in NaCl, at  $I = 0.1 \text{ mol L}^{-1}$  and stirred for 6 hours. Then the supernatant was collected for  $\text{Pb}^{2+}$   
160 analysis. The adsorbent was rinsed with ultra pure water and then treated with 25 mL of HCl  $0.1$   
161  $\text{mol L}^{-1}$  to extract the  $\text{Pb}^{2+}$ . The extractant was separated after 6 hours and collected for  $\text{Pb}^{2+}$   
162 analysis. The Hal-NH<sub>2</sub> was left in NaOH  $0.1 \text{ mol L}^{-1}$  for 1 hour and then rinsed with ultra pure  
163 water and reused. The same procedure was repeated three times.

164 The  $\text{Pb}^{2+}$  concentration in solutions collected during the experiments was measured by Differential  
165 Pulse Anodic Stripping Voltammetry (DP-ASV) technique. The voltammetric apparatus was  
166 constituted by a Metrohm 663 VA stand combined with the Autolab potentiostat in conjunction  
167 with the IME663 interface. The voltammetric apparatus was controlled by NOVA v. 1.10 software.  
168 The VA stand was equipped with a three electrode system consisting of i) a Multi Mode Electrode  
169 Pro (Metrohm, code 6.1246.120) working in the Static Mercury Drop Electrode (SMDE) mode, ii) a  
170 glassy carbon auxiliary electrode (code 6.1247.000), and iii) a double junction Ag/AgCl/KCl ( $3 \text{ mol}$   
171  $\text{L}^{-1}$ ) reference electrode (code 6.0728.030). The DP-ASV measurements were performed after  
172 bubbling purified N<sub>2</sub> gas into the solutions for 150 s. The experimental electrochemical conditions  
173 were chosen in order to optimize the quality parameters, as signal/noise ratio, repeatability and  
174 accuracy and are reported in Table 1S of Supplementary Materials.

175 Calibration curves of  $\text{Pb}^{2+}$  ion were done at the same experimental conditions of kinetic and  
176 thermodynamic adsorption/desorption experiments. To this end, 25 mL of aqueous solution at the  
177 appropriate pH and ionic strength (NaCl) were placed in the voltammetric cell. A voltammogram of  
178 the solution was recorded as blank. Then, voltammograms after addition of different aliquots of the

179 standard solution of  $Pb^{2+}$  ( $100 \text{ mgL}^{-1}$ ) at the same pH and ionic strength were collected. The  
180 concentration range of the calibration curves was  $3 - 50 \text{ mg L}^{-1}$ .

181 The pH of the  $Pb^{2+}$  solutions was measured with a combined ISE- $H^+$  glass electrode (Ross type  
182 8102). The ISE- $H^+$  electrode was previously calibrated at the same experimental conditions of the  
183 adsorption experiments. To this end, 25 mL of standardized HCl solution was titrated with NaOH  
184 by using a potentiometric titration system (Metrohm, Model 888 Titrand) controlled by the  
185 TIAMO software.

186

#### 187 ***2.4. Models for kinetic and isotherm studies of $Pb^{2+}$ adsorption.***

188 Several models have been proposed by different authors to model equilibrium isotherms and  
189 kinetics of metal ion adsorption onto several bio-adsorbents.(Park et al., 2010).

190 Here, the pseudo-first order equation of Lagergren (PFO) (eq. 1), the pseudo-second order equation  
191 (PSO) (eq. 2) and the intraparticle diffusion equation of Vermeulen (Ver) (eq. 3) were used to fit the  
192 kinetic data (Ho, 2006; Park et al., 2010) and references therein:

(1)

$$\frac{dq_t}{dt} = k_1(q_e - q_t)$$

$$\frac{dq_t}{dt} = k_2(q_e - q_t)^2$$

(2)

$$\frac{dq_t}{dt} = k_v \frac{(q_e^2 - q_t^2)}{q_t}$$

(3)

193 where  $q_t$  and  $q_e$  are the adsorption ability of the adsorbent material ( $\text{mg g}^{-1}$ ) at time  $t$  and at the  
194 equilibrium and  $k_1$  ( $\text{min}^{-1}$ ),  $k_2$  ( $\text{g mg}^{-1} \text{ min}$ ) and  $k_v$  ( $\text{min}^{-1}$ ) are the rate constants of adsorption.

195 Integrating eqs for the boundary conditions  $t = 0$  to  $t = t$  and  $q_t = 0$  to  $q_t = q_t$  in the non linear form  
196 are listed below:

$$q_t = q_e(1 - e^{-k_1 t}) \quad (4)$$

$$q_t = \frac{q_e^2 \cdot k_2 \cdot t}{1 + q_e \cdot k_2 \cdot t} \quad (5)$$

$$q_t = q_e \cdot (1 - e^{-2k_1 t})^{0.5} \quad (6)$$

197 Batch equilibrium isotherm curves have been obtained processing the experimental data with three  
 198 empirical models namely the two parameters models of Freundlich (eq. 7) and Langmuir (eq. 8) and  
 199 the three parameters model of Sips (eq. 9)(Gerente et al., 2007; Park et al., 2010) and references  
 200 therein:

$$q_e = K_F \cdot C_e^{1/n} \quad (7)$$

$$q_e = \frac{q_m \cdot K_L \cdot C_e}{1 + K_L \cdot C_e} \quad (8)$$

$$q_e = \frac{q_m \cdot K_S \cdot C_e^{1/s}}{1 + K_S \cdot C_e^{1/s}} \quad (9)$$

201 where  $q_m$  ( $\text{mg g}^{-1}$ ) is the maximum adsorption capacity of the material,  $C_e$  ( $\text{mg L}^{-1}$ ) is the metal  
 202 concentration in solution at equilibrium;  $K_F$  ( $\text{L}^{1/n} \text{g}^{-1} \text{mg}^{1-1/n}$ ),  $K_L$  ( $\text{L} \cdot \text{mg}^{-1}$ ) and  $K_S$  ( $\text{L}^{1/s} \text{mg}^{-1/s}$ ) are the  
 203 constants of Freundlich, Langumir and Sips models, respectively. Freundlich model takes into  
 204 account the heterogeneity of surface or of the binding sites of the adsorbent.  $K_F$  and  $n$  are related to  
 205 the binding capacity and the affinity of the adsorbent toward the adsorbate. Langmuir model  
 206 describes the adsorption on equivalent sites of the material which can be saturated obtaining a  
 207 monolayer.  $K_L$  is related to the initial slope of the isotherm. Finally, in the Sips model both  
 208 heterogeneous adsorptions as well as saturation conditions are taken into account introducing a third  
 209 parameter ( $s$ ) in the equation.

210 The metal ion adsorption capacity at different contact times  $t$  ( $q_t$ ,  $\text{mg g}^{-1}$ ) in kinetic study, or at  
 211 different metal / adsorbent ratio in equilibrium study ( $q_e$ ,  $\text{mg g}^{-1}$ ) was calculated by the eq. 10:

$$q_t \text{ or } q_e = \frac{V \cdot (C_0 - C_t)}{m} \quad (10)$$

212 where  $V$  (L) is the volume of the metal solution and  $m$  is the mass of p-Hal or Hal-NH<sub>2</sub> (g);  $C_0$  and  
213  $C_t$  are the metal ion concentrations in solution (mg L<sup>-1</sup> of Pb<sup>2+</sup>) at  $t = 0$  and  $t = t$ , respectively. At the  
214 equilibrium condition, eq. 10 was applied by replacing  $C_t$  with  $C_e$  to calculate  $q_e$ .

215 The Linear and Non Linear data Analysis home-made computer program LIANA and OriginLab  
216 suite were used to fit kinetic and isotherm equations to experimental data (De Stefano et al., 1997).

217

### 218 **3. Results and Discussion**

#### 219 **3.1 Synthesis and characterization of Hal-NH<sub>2</sub> nanomaterial**

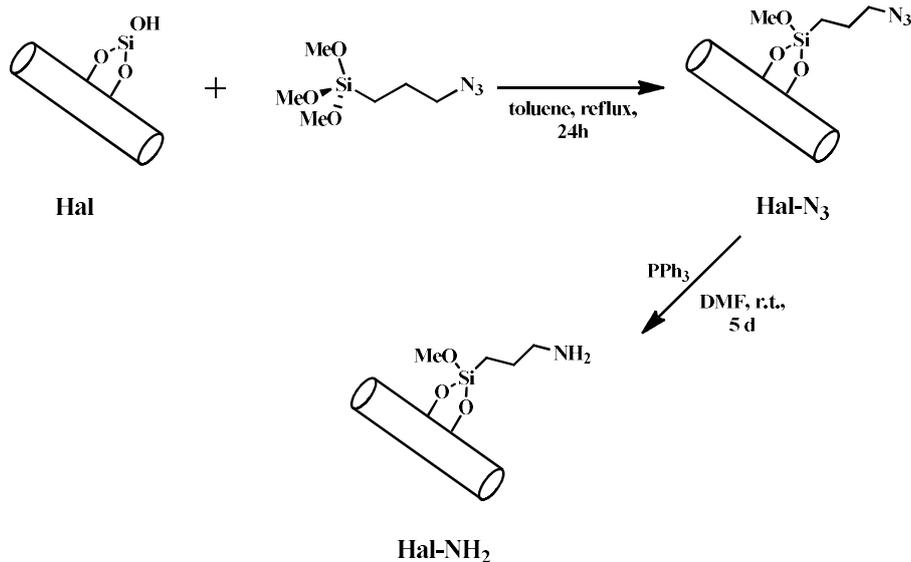
220 Halloysite nanotubes reacted with an excess of 3-azidopropyltrimethoxysilane in toluene at reflux,  
221 affording the Hal-N<sub>3</sub> nanomaterial, following a procedure reported elsewhere (Riela et al., 2014).

222 After the work up, the -N<sub>3</sub> groups loading with respect to p-Hal, estimated by TGA, was ca.  $2.4 \pm$   
223  $0.2$  wt%. Successively, the quantitative reduction with PPh<sub>3</sub> of Hal-N<sub>3</sub>, gave amino-functionalized  
224 Hal-NH<sub>2</sub> that represents the adsorbent material (see Figure 1).

225 To confirm that the functionalization occurs on the external surface, contact angle measurements  
226 were performed obtaining the  $\theta$  values of  $21.9 \pm 1.3^\circ$  and  $61.2 \pm 1.3^\circ$ , for p-Hal and Hal-NH<sub>2</sub>,  
227 respectively.

228

229



230

231 **Figure 1.** Schematic representation of the synthesis of Hal-NH<sub>2</sub> nanomaterial.

232

233 The two-step synthesis was adopted in order to ensure the highest loading on halloysite external  
 234 surface; for comparison, indeed, we also performed a one-step modification with 3-  
 235 aminopropyltrimethoxysilane, which gave a percent loading of about 1 wt% whereas the  
 236 introduction of the azido group and the following reduction allowed us to obtain a loading of 2.4  
 237 wt%.

238 Compared to p-Hal, (Massaro et al., 2016a) Hal-N<sub>3</sub> nanomaterial exhibits the vibration bands for C-  
 239 H stretching of methylene groups around 2980 cm<sup>-1</sup> and a strong band around 2100 cm<sup>-1</sup> due to the  
 240 -N<sub>3</sub> groups of azido silane. The intensity for -N<sub>3</sub> band decreases after reduction confirming the  
 241 presence of the NH<sub>2</sub> groups on halloysite external surface. These findings provide evidence for the  
 242 presence of organic moieties in the new material (Figure 2a). Based on the unaltered frequency of  
 243 the stretching bands of OH groups of the alumina inner-surface, we can conclude that the grafting  
 244 has taken place only on the external surface of Hal, as reported elsewhere (Rawtani et al., 2017;  
 245 Sadjadi and Atai, 2018).

246 Thermogravimetric analyses (TGA) confirmed the functionalization on p-Hal external surface and it  
 247 allowed calculating 2.4 wt% loading of organic moiety on the Hal-NH<sub>2</sub> nanomaterial as follow:

248

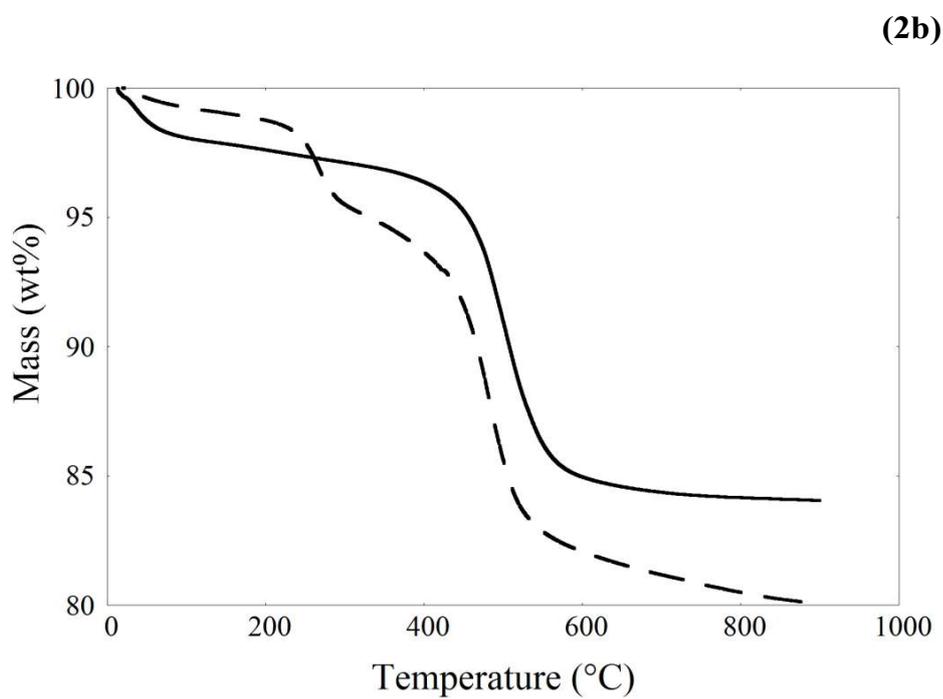
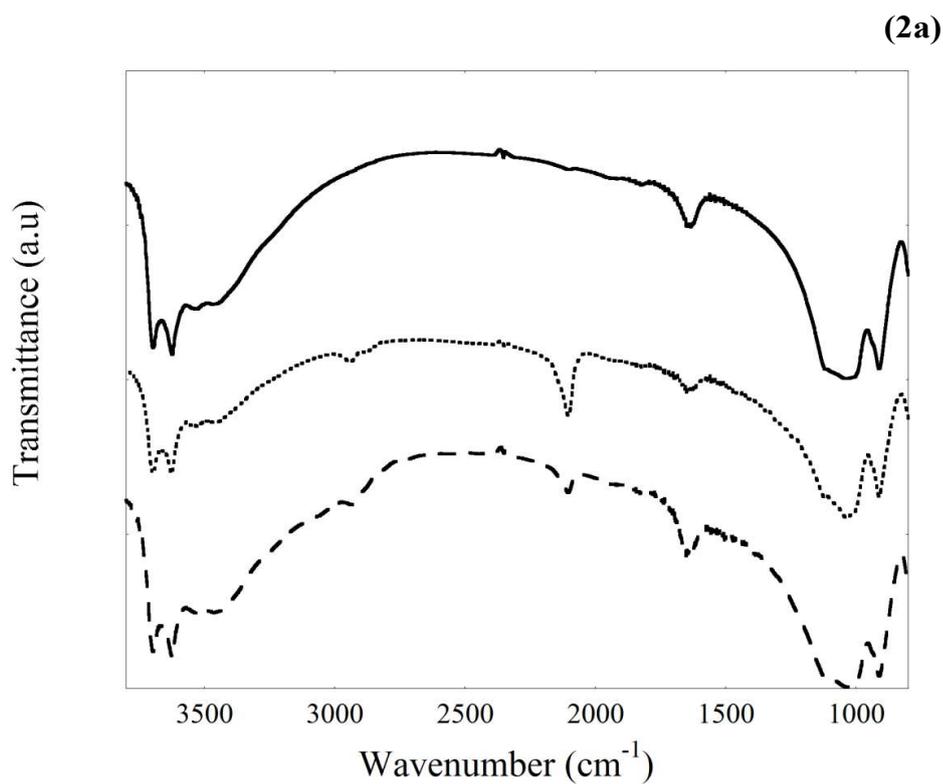
$$wt\% = 100[1 - (MR_{600-Hal-NH_2} + ML_{150-Hal-NH_2}) / (MR_{600-p-Hal} + ML_{150-p-Hal})] \quad (11)$$

249

250 where  $MR_{600-Hal-NH_2}$  and  $MR_{600-p-Hal}$  are the residual mass at 600 °C obtained from TG curves of  
251 amine functionalized halloysite and pristine halloysite, respectively, while  $ML_{150}$  is the mass loss  
252 between 25 and 150 °C representing the water content of the investigated material.

253 The curves (Figure 2b) clearly show that the residual of the nanomaterials is stepwise changing,  
254 from the p-Hal to the Hal-NH<sub>2</sub>, due to the organic compounds linked on the surface of the  
255 nanotubes. The thermograms were corrected for the different moisture contents to underline the  
256 mass losses of p-Hal and organic compounds. Above 100 °C the p-Hal curve reveals the  
257 characteristic mass loss at 500 °C attributed to the expulsion of two water molecules from p-Hal  
258 interlayer (Massaro et al., 2016b). The Hal-NH<sub>2</sub>, instead, showed an additional mass loss at 250 °C  
259 due to the organic moiety with NH<sub>2</sub> termination (Cavallaro et al., 2015).

260

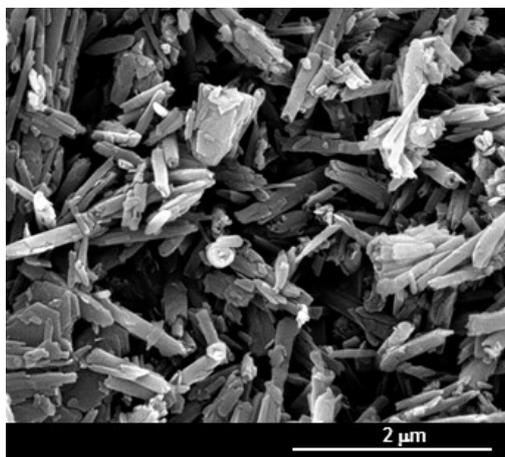


261 **Figure 2.** FT-IR spectra of p-Hal (solid line), Hal-N<sub>3</sub> (dotted line) and Hal-NH<sub>2</sub> (dashed line) (2a);

262 thermoanalytical curves of p-Hal (solid line) and Hal-NH<sub>2</sub> (dashed line) (2b).

263

264 The morphology of functionalized Hal was characterized by electron scanning microscopy (SEM)  
265 (see Figure 3). SEM image shows that in the Hal-NH<sub>2</sub> compound the morphology of Hal was  
266 preserved after organosilane grafting and the nanomaterial shows the typical rod-shaped structure of  
267 halloysite.



268

269 **Figure 3.** SEM image of Hal-NH<sub>2</sub>.

270

### 271 **3.2 Speciation Analysis**

272 An efficient metal ion adsorption onto an adsorbent mainly depends on the chemical form of the  
273 adsorbent and adsorbate in the aqueous solution to be treated.

274 In particular, the metal ion has to be present in solution as positively or negatively charged species  
275 able to interact with binding groups with opposite charge on the adsorbent.

276 The chemical form of metal ion, as well as that of the adsorbent material depends on the  
277 experimental conditions of the aqueous solution (ionic medium, ionic strength, pH, etc.) and only an  
278 accurate speciation study gives the possibility to know the best conditions in terms of adsorption  
279 ability of the adsorbent towards the toxic metal ion.

280 As it is known, the inner and outer surfaces of halloysite nanotubes contain AlOH and SiOH  
281 groups, respectively. Due to their acid-base properties, in a wide pH range there is a charge  
282 separation between the external (negative) and internal (positive) surfaces of the nanotubes. In

283 addition, in the functionalized halloysite Hal-NH<sub>2</sub> also the propylamine groups bound to the outer  
284 surface have to be considered.

285 The protonation equilibria of p-Hal have been studied in a previous article in different ionic media  
286 and ionic strengths (Bretti et al., 2016). Two units namely p-Hal<sub>1</sub> and p-Hal<sub>2</sub> containing AlOH and  
287 SiOH groups, respectively were considered to model the protonation equilibria of halloysite.  
288 Different models, previously tested for natural and synthetic polyelectrolytes, were used to calculate  
289 protonation constants. Here, the protonation constants calculated with diprotic like model have been  
290 used to draw the distribution diagrams of protonated/unprotonated p-Hal species in NaCl medium  
291 chosen in adsorption experiments. As an example, Figure 1S of Supplementary Materials reports  
292 the distribution diagram of p-Hal<sub>1</sub> and p-Hal<sub>2</sub> species in NaCl<sub>aq</sub>, at  $I = 0.1 \text{ mol L}^{-1}$  and  $T = 25 \text{ }^\circ\text{C}$ .

293 In the ionic medium and pH range considered, Pb<sup>2+</sup> ion forms several hydroxo and chloride species  
294 differently charged [Pb(OH)<sub>n</sub><sup>z</sup>, PbCl<sub>n</sub><sup>z</sup> and PbCl(OH)<sub>n</sub> n = 0 to 3, z = from 2+ to 1-]. Also the  
295 formation and distribution of metal species have been evaluated using the stability constants in  
296 NaCl medium reported in the literature (Baes and Mesmer, 1976; Luo and Millero, 2007). As an  
297 example, the speciation diagram of Pb<sup>2+</sup> species in NaCl aqueous solution at  $I = 0.1 \text{ mol L}^{-1}$  is  
298 reported in Figure 2S of Supplementary materials.

299 Table 1 reports the percentages of p-Hal and Pb<sup>2+</sup> species as function of pH and ionic strength in  
300 NaCl medium and at  $T = 25 \text{ }^\circ\text{C}$ . These data, and those at lower and higher pH values (not reported  
301 here) have been taken into account to establish the best experimental conditions used in adsorption  
302 experiments and they are discussed in section 3.4.

303

304

305 **Table 1.** Percentages of Pb(II) and p-Hal species<sup>a</sup> in NaCl aqueous solution, at different ionic  
306 strengths and pH and at  $T = 25 \text{ }^\circ\text{C}$

---

species

%

<b>pH</b>	<b>3</b>	<b>4</b>	<b>5</b>	<b>5</b>	<b>5</b>	<b>6</b>
<b><i>I</i> (mol L<sup>-1</sup>)</b>	<b>0.10</b>	<b>0.10</b>	<b>0.10</b>	<b>0.25</b>	<b>0.50</b>	<b>0.10</b>
p-Hal <sub>1</sub>	0	0	0	0	0	0
H(p-Hal <sub>1</sub> ) <sup>+</sup>	0	0.01	0.1	0.11	0.09	0.97
H <sub>2</sub> (p-Hal <sub>1</sub> ) <sup>2+</sup>	100	99.99	99.9	99.89	99.81	99.03
pHal <sub>2</sub> <sup>-</sup>	6	38.96	86.45	84.18	82.55	98.46
H(p-Hal <sub>2</sub> )	94	61.04	13.55	15.82	17.45	1.54
Pb <sup>2+</sup>	24.5	24.5	24.3	11.7	5.8	22.8
PbCl <sup>+</sup>	56.0	56.0	55.6	48.6	36.5	52.3
PbCl <sub>2</sub>	18.5	18.5	18.4	35.0	46.0	17.3
PbCl <sub>3</sub> <sup>-</sup>	1.0	1.0	1.0	4.4	11.5	0.9
Pb(OH) <sup>+</sup>	0	0.1	0.7	0.3	0.2	6.6
PbCl(OH)	0	0	0	0	0	0.1

307 <sup>a</sup> calculated from distribution diagrams made by using the formation constants of p-Hal and Pb(II)  
308 species reported in ref. (Baes and Mesmer, 1976; Luo and Millero, 2007; Bretti et al., 2016) and the  
309 same concentrations used in the adsorption experiments.

### 311 **3.3 Kinetics of Pb(II) adsorption on p-Hal and Hal-NH<sub>2</sub> materials**

312  
313 The Pb<sup>2+</sup> adsorption rate onto p-Hal and Hal-NH<sub>2</sub> has been studied in NaCl aqueous solution at *I* =  
314 0.1 mol L<sup>-1</sup>, *C*<sub>Pb<sup>2+</sup></sub> = 30 mg L<sup>-1</sup>, in the pH range 3 - 6. Independently of pH, the adsorption  
315 equilibrium in Pb<sup>2+</sup> - p-Hal system was reached very quickly (~ 40 min). The same behaviour was  
316 found with Hal-NH<sub>2</sub> at pH = 3, whilst at higher pH, after an initial rapid Pb<sup>2+</sup> adsorption (~ 40 min),  
317 there was a slow and continue adsorption until ~ 240 min (see Figures 3S and 4S).

318 In order to understand the adsorption dynamics, different kinetic models were used to fit  
 319 experimental data (see section 2.4). The values of kinetic parameters of PFO, PSO and Ver models  
 320 are reported in Table 2S together with  $R^2$  and  $\sigma$  of the fits. The most suitable kinetic model for  $Pb^{2+}$   
 321 -p-Hal system at every pH and for  $Pb^{2+}$  - Hal-NH<sub>2</sub> system at pH = 3 was the PFO, whilst, at higher  
 322 pH the Ver model better described the experimental data of  $Pb^{2+}$  - Hal-NH<sub>2</sub> system (see Table 2). It  
 323 can be explained considering that at pH = 3 the great part of binding groups of both adsorbents are  
 324 protonated, their adsorption capacity is low and their behaviour is very similar. At higher pH the  
 325 deprotonation of SiOH groups of halloysite favours the adsorption of both adsorbents; moreover  
 326 also amino groups contribute to the  $Pb^{2+}$  adsorption of Hal-NH<sub>2</sub> increasing its adsorption ability  
 327 (e.g.  $q_e = 4.30$  and  $18.6 \text{ mg g}^{-1}$  at pH = 5 for p-Hal and Hal-NH<sub>2</sub>, respectively) and changing the  
 328 adsorption dynamics of the functionalized p-Hal (Ver model fit better than PFO model; see  $R^2$  and  
 329  $\sigma$  values in Table 2S). The  $q_e$  trends of the two adsorbents vs pH are shown in Figure 5S of  
 330 Supplementary Materials.

331

332 **Table 2.** Parameters of PFO and Ver kinetic equations for Pb(II) adsorption on p-Hal and Hal-NH<sub>2</sub>,  
 333 at different pH values, in NaCl<sub>aq</sub>, at  $I = 0.1 \text{ mol L}^{-1}$  and at  $T = 25 \text{ }^\circ\text{C}$ .

Kinetic model	adsorbent	pH	$q_e^a$	$k_i^{b,c}$	$R^2$	$\sigma^d$
PFO	p-Hal	3	$3.00 \pm 0.01$	$0.154 \pm 0.005$	0.9848	0.0849
PFO	Hal-NH <sub>2</sub>		$3.74 \pm 0.02$	$0.187 \pm 0.009$	0.9715	0.1417
PFO	p-Hal	4	$3.27 \pm 0.02$	$0.139 \pm 0.005$	0.9856	0.0940
Ver	Hal-NH <sub>2</sub>		$13.1 \pm 0.4$	$0.003 \pm 0.001$	0.9888	0.3831
PFO	p-Hal	5	$4.30 \pm 0.03$	$0.21 \pm 0.01$	0.9749	0.1413
Ver	Hal-NH <sub>2</sub>		$18.6 \pm 0.4$	$0.0034 \pm 0.0001$	0.9902	0.4934
PFO	p-Hal	6	$5.03 \pm 0.05$	$0.101 \pm 0.006$	0.9576	0.2654
Ver	Hal-NH <sub>2</sub>		$19.7 \pm 0.7$	$0.0022 \pm 0.0002$	0.9880	0.5651

334 <sup>a</sup>  $\text{mg g}^{-1}$ ; <sup>b</sup>  $\text{min}^{-1}$  for both  $k_l$  and  $k_v$ ; <sup>c</sup> subscript  $i$  is 1 or v according to the model; <sup>d</sup> std. dev of the fit.

335

### 336 **3.4 Modelling of equilibria of Pb(II) uptake by p-Hal and Hal-NH<sub>2</sub> materials**

337 Adsorption equilibria of Pb<sup>2+</sup> onto p-Hal and Hal-NH<sub>2</sub> have been studied in NaCl aqueous solutions  
338 in the pH range 3 – 6 chosen on the basis of speciation analysis (see section 3.2). The solution pH  
339 was measured at the end of experiments and is reported in Table 3 together with parameters of the  
340 most suitable isotherm equation for each experimental data set. Among the tested isotherm models,  
341 Sips equation was the best or it was equivalent to Langmuir isotherm ( $s \approx 1$ ) in terms of quality of  
342 fit for all the systems investigated. Although isotherm models do not necessarily give information  
343 about the mechanism of the adsorption of metal ion they can be useful to predict or optimize the  
344 uptake processes, e.g., through the calculation of  $q_m$  parameter that gives information about the  
345 maximum amount of metal ion adsorbed by 1 g of adsorbent. The parameters of all isotherm  
346 equations tested are reported in Table 3S of Supplementary Materials together with the R<sup>2</sup> and  $\sigma$  of  
347 the fits. In batch experiments, a significant increase of pH of solutions (1.5 – 2 units) at the  
348 adsorption equilibrium was found only with Hal-NH<sub>2</sub> adsorbent at initial pH = 4, 5 and 6 and can be  
349 attributed to the protonation of amino groups not bound to Pb<sup>2+</sup> ions. In fact, considering the  
350 concentration of Pb<sup>2+</sup> and the amount of adsorbent used in batch experiments, NH<sub>2</sub> groups of  
351 adsorbent are always in excess with respect to the metal ion.

352 The experimental points together with the curve fits of the three isotherm equations for all the Pb(II)  
353 – adsorbent investigated systems are reported in Figure 4 and in Figures 6S and 7S of  
354 Supplementary Materials. The adsorption ability of both pristine and functionalized Hal increases  
355 with the increasing of pH and with the decreasing of ionic strength (see Figures 5 and 6). Looking  
356 at the species percentages reported in Table 1, in the pH and ionic strength ranges investigated the  
357 great part of Pb(II) is present as positively charged species [Pb<sup>2+</sup>, PbCl<sup>+</sup> and Pb(OH)<sup>+</sup>] easily  
358 bounded by silanol and amino groups of adsorbent materials. Moreover, at  $I = 0.1 \text{ mol L}^{-1}$  the % of  
359 Pb species, as well as the % of p-Hal<sub>1</sub> species do not change with the changing of pH from 3 to 6.  
360 Therefore, the increase of  $q_m$  with pH for both p-Hal and Hal-NH<sub>2</sub> can be ascribed to the

361 deprotonation of SiOH groups of p-Hal<sub>2</sub> units (Bretti et al., 2016) of halloysite (% p-Hal<sub>2</sub><sup>-</sup> = 6 and  
 362 98 at pH 3 and 6, respectively) and to the presence of NH<sub>2</sub> groups in Hal-NH<sub>2</sub> material that are fully  
 363 protonated at pH = 3 and becomes gradually available to bind Pb<sup>2+</sup> ions at higher pH values. At pH  
 364 = 5, the increase of ionic strength from 0.1 to 0.5 mol L<sup>-1</sup> causes a decrease of positively charged Pb  
 365 species (substituted by chlorinated PbCl<sub>2</sub> and PbCl<sub>3</sub><sup>-</sup> species) that is responsible of the lowering of  
 366  $q_m$  of p-Hal and of Hal-NH<sub>2</sub>.

367 Independently of the experimental conditions, the adsorption ability, as well as the affinity of Hal-  
 368 NH<sub>2</sub> towards Pb<sup>2+</sup> are higher than p-Hal (higher  $q_m$  and  $K_s$  values) and the differences in adsorptive  
 369 performances of the two materials are more pronounced at higher pH values (e.g.,  $q_m$  = 6 and 46 mg  
 370 g<sup>-1</sup>,  $K_s$  = 0.017 and 0.43 L<sup>1/s</sup> mg<sup>-1/s</sup> at pH = 6 for p-Hal and Hal-NH<sub>2</sub>, respectively).

371 Considering i) the changing of pH during adsorption, ii) the speciation analysis of p-Hal and of Pb<sup>2+</sup>  
 372 ion in aqueous solution and iii) the dependence on pH and ionic strength of adsorption ability of p-  
 373 Hal and Hal-NH<sub>2</sub>, an adsorption mechanism mainly based on positively charged Pb<sup>2+</sup> species [Pb<sup>2+</sup>,  
 374 Pb(OH)<sup>+</sup> and PbCl<sup>+</sup>] chelation by silanol and amino groups can be hypothesized.

375

376

377 **Table 3.** Sips isotherm parameters for the Pb(II) adsorption on p-Hal and Hal-NH<sub>2</sub> in NaCl<sub>aq</sub>, at  
 378 different pH and ionic strengths and at  $T = 25$  °C.

adsorbent	pH <sub>i</sub> <sup>a</sup>	pH <sub>f</sub> <sup>a</sup>	$I$ <sup>b</sup>	$q_m$ <sup>c</sup>	$K_s$ <sup>d</sup>	$s$	$R^2$	$\sigma$ <sup>e</sup>
p-Hal	3.0±0.2	3.1±0.2	0.10	3.10±0.03	0.016±0.003	0.80±0.06	0.9974	0.0469
Hal-NH <sub>2</sub>	2.9±0.3	3.1±0.4		5±1	0.010±0.004	0.7±0.1	0.9848	0.1420
p-Hal	4.0±0.3	4.0±0.3	0.10	3.5±0.4	0.013±0.001	0.84±0.06	0.9982	0.0282
Hal-NH <sub>2</sub>	4.0±0.3	6.0±0.2		19.1±0.4	0.57±0.04	1.00±0.01	0.9979	0.2627
p-Hal	5.0±0.2	5.3±0.3	0.10	4.5±0.2	0.03±0.01	0.66±0.08	0.9907	0.1378
Hal-NH <sub>2</sub>	5.0±0.2	6.7±0.6		37±2	0.69±0.08	2.1±0.2	0.9978	0.4640

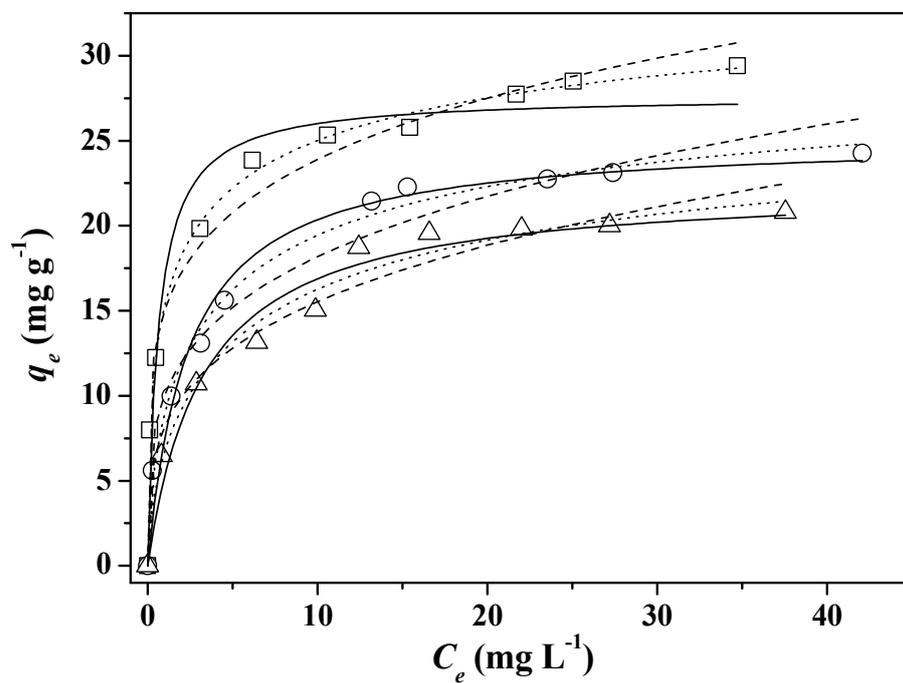
p-Hal	5.0±0.2	5.2±0.3	0.25	3.3±0.6	0.037±0.009	0.9±0.2	0.9847	0.1013
Hal-NH <sub>2</sub>	5.0±0.2	6.3±0.5		31±2	0.41±0.5	1.6±0.2	0.9926	0.7261
p-Hal	5.0±0.2	5.2±0.2	0.50	1.40±0.04	0.009±0.003	0.50±0.04	0.9944	0.0365
Hal-NH <sub>2</sub>	5.0±0.2	6.2±0.5		28±6	0.31±0.7	1.6±0.4	0.9791	1.0020
p-Hal	6.0±0.2	6.1±0.2	0.10	6±1	0.017±0.002	0.98±0.08	0.9972	0.0474
Hal-NH <sub>2</sub>	6.0±0.2	6.8±0.4		46±7	0.43±0.09	2.1±0.3	0.9943	0.7821

379 <sup>a</sup> solutions pH before (pH<sub>i</sub>) and after (pH<sub>f</sub>) contact with adsorbents; <sup>b</sup> mol L<sup>-1</sup>; <sup>c</sup> mg g<sup>-1</sup>; <sup>d</sup> L<sup>1/s</sup> mg<sup>-1/s</sup>; <sup>e</sup>

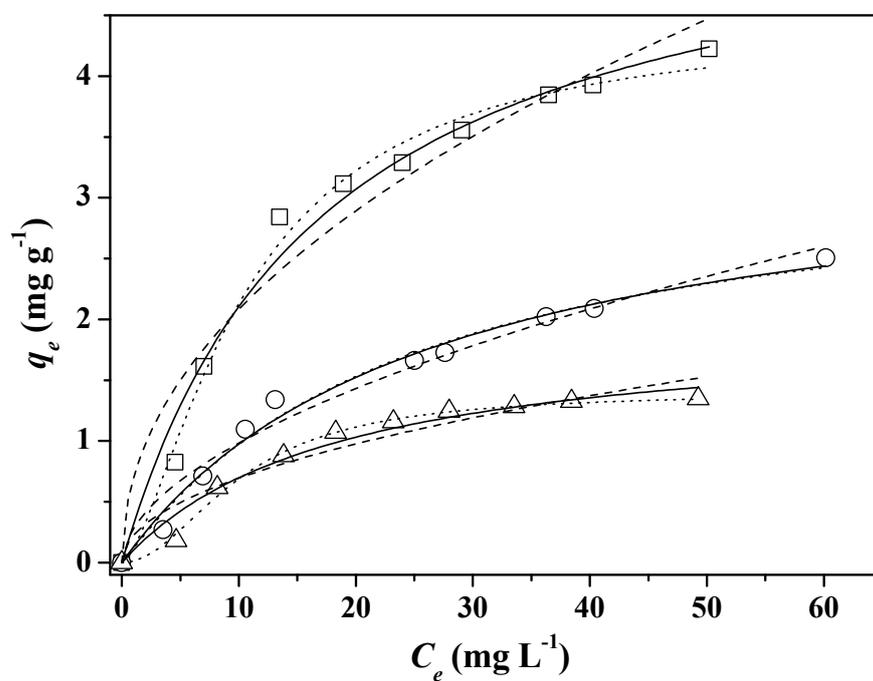
380 std. dev of the fit.

381

(4a)

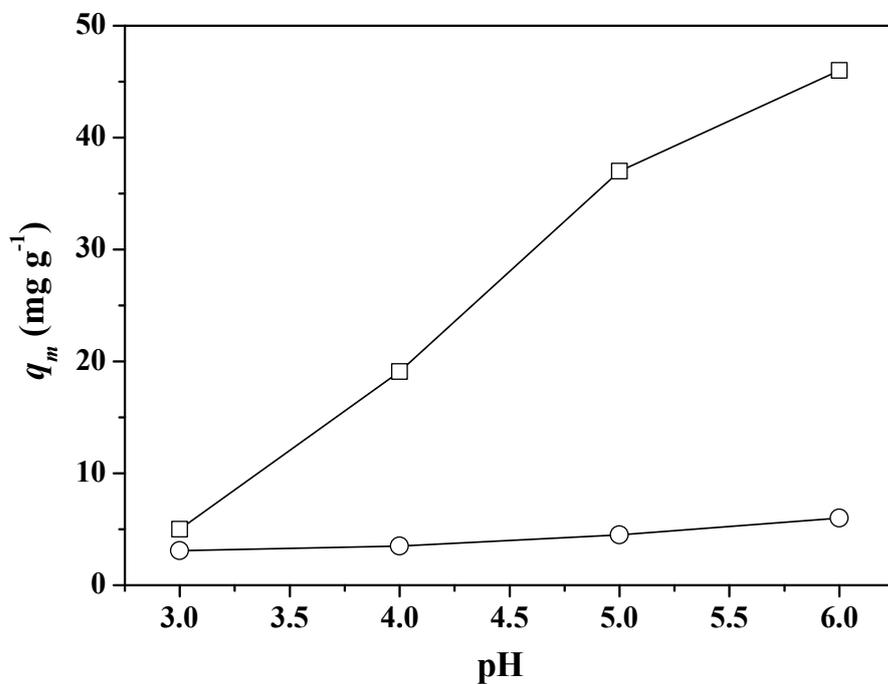


(4b)



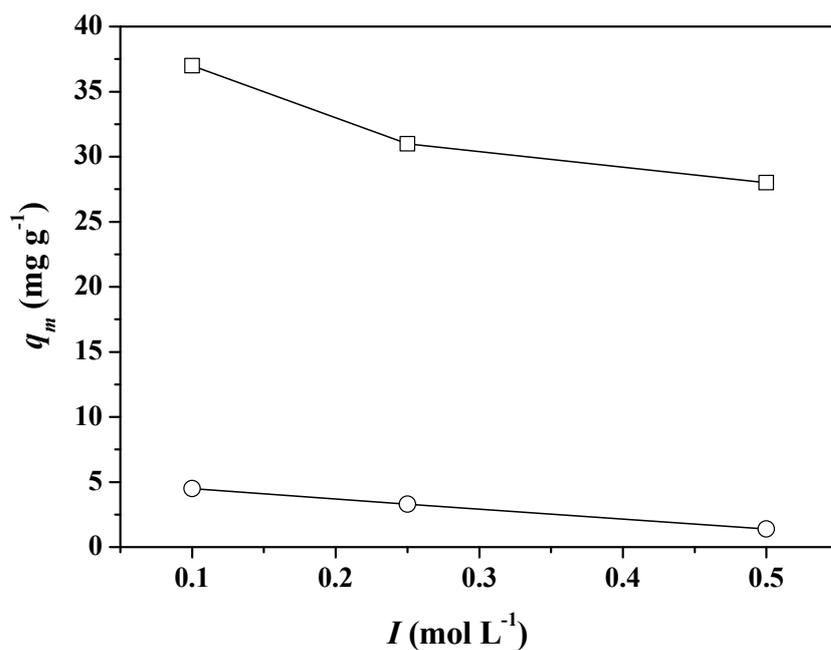
382 **Figure 4.** Adsorption isotherms of  $\text{Pb}^{2+}$  on Hal-NH<sub>2</sub> (Fig. 3a) and p-Hal (Fig. 3b) from aqueous  
383 solutions at pH = 5 containing NaCl 0.10 ( $\square$ ), 0.25 ( $\circ$ ), 0.50 ( $\triangle$ ) mol L<sup>-1</sup> and at  $T = 25$  °C.

384 Experimental data fitted with Freundlich (dashed lines), Langmuir (continuous lines) and Sips  
385 (dotted lines) models.



386  
387 **Figure 5.** Experimental  $q_m$  values vs pH for the  $\text{Pb}^{2+}$  adsorption onto p-Hal (○) and Hal-NH<sub>2</sub> (□)  
388 adsorbent materials in  $\text{NaCl}_{\text{aq}}$ , at  $I = 0.10 \text{ mol L}^{-1}$  and  $T = 25 \text{ }^\circ\text{C}$ .

389



390

391 **Figure 6.** Experimental  $q_m$  values vs  $I$  (mol L<sup>-1</sup>) for the Pb<sup>2+</sup> adsorption onto p-Hal (○) and Hal-

392 NH<sub>2</sub> (□) adsorbent materials in NaCl<sub>aq</sub>, at pH = 5 and  $T = 25$  °C.

393

394 The possibility of recycle and reuse of Hal-NH<sub>2</sub> material has been evaluated. The results of

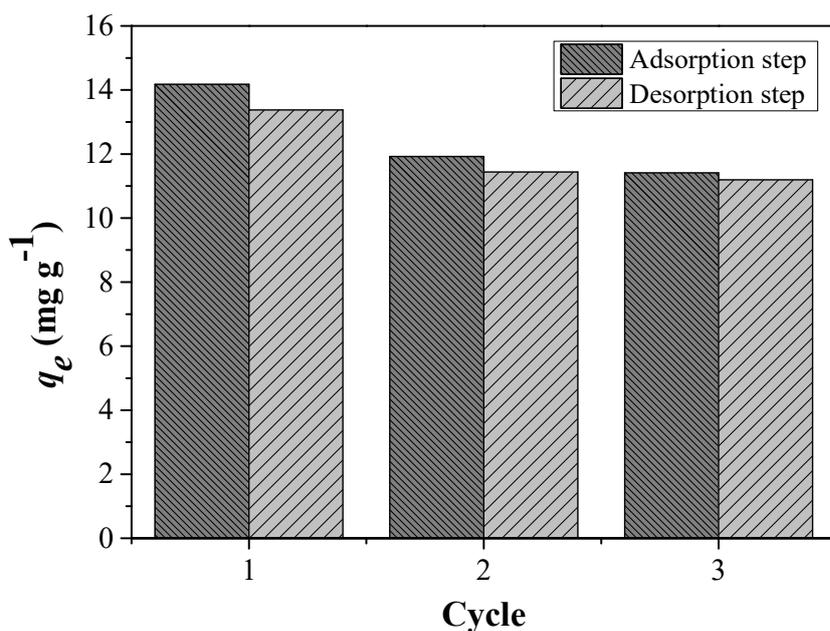
395 adsorption/desorption cycles are shown in Figure 7. As can be seen, at the conditions used in the

396 experiments, the adsorbent exhibits a good reuse capacity with slight variations of

397 adsorbed/desorbed amount of Pb<sup>2+</sup> in the first three cycles.

398

399



400

401 **Figure 7.**  $q_e$  values of adsorption and desorption steps. Experimental details: amount of Hal-NH<sub>2</sub> =  
 402 40 mg,  $C_{\text{Pb}^{2+}} = 30 \text{ mg L}^{-1}$  in NaCl, at  $I = 0.1 \text{ mol L}^{-1}$ .

403

### 404 3.5 Literature data comparison

405 In the last decades a lot of articles and reviews have been published on the adsorption ability of  
 406 different pristine or modified clay minerals towards Pb<sup>2+</sup> ions (Jiang et al., 2009; Oubagaranadin  
 407 and Murthy, 2009; He et al., 2013; Matusik and Wscislo, 2014; Maziarz et al., 2015; Yuan et al.,  
 408 2015; Sdiri et al., 2016; Hu et al., 2017; Uddin, 2017). A comparison of the adsorption capacity of  
 409 the different clay adsorbents is very difficult because it depends on many variables of the metal –  
 410 adsorbent system investigated such as: the origin of the clay, the type of modification, the loading  
 411 percent (in case of functionalization), the experimental conditions of metal ion solution (pH, ionic  
 412 medium, ionic strength, metal ion concentration, temperature). In Table 4 are reported the ranges of  
 413 maximum adsorption capacity values ( $q_m$ ) of different pristine and modified clay minerals towards  
 414 Pb<sup>2+</sup> recently reported in literature. On average, the adsorption ability of p-Hal toward Pb<sup>2+</sup> is lower

415 than other clay minerals. However, p-Hal has a good dispersability in water and does not need  
 416 exfoliation to expose large surface area in an efficient way.

417 Considering the experimental differences, the adsorption results here obtained for p-Hal towards  
 418  $Pb^{2+}$  ion are comparable with those reported in literature by (Matusik and Wscislo, 2014) and  
 419 (Maziarz et al., 2015). The authors reported a  $q_m = 8$  and  $7.7 \text{ mg g}^{-1}$ , respectively, at  $pH = 5$  and  
 420 without ionic medium. Considering the absence of Pb-Cl species and the consequently higher  
 421 percent of positively charged Pb species in solution, these  $q_m$  values are in line with the  $q_m = 4.5 \text{ mg}$   
 422  $\text{g}^{-1}$  that we found at the same pH, in  $NaCl_{aq}$  at  $I = 0.1 \text{ mol L}^{-1}$ . Two functionalized Hal with  
 423 diethanolamine (HD) and triethanolamine (HT) were also tested as adsorbent materials towards  
 424  $Pb^{2+}$  ion by (Matusik and Wscislo, 2014). The  $q_m = 37 \text{ mg g}^{-1}$  found by us for Hal- $NH_2$  at  $pH = 5$   
 425 and  $I = 0.1 \text{ mol L}^{-1}$  is significantly higher than  $13.28$  and  $12.18 \text{ mg g}^{-1}$  found at the same pH and  
 426 without chloride medium for HD and HT, respectively. These differences in  $q_m$  values could be  
 427 attributed to the steric hindrance produced by the two or three ethanol groups of HD and HT that  
 428 hampered the  $Pb^{2+}$  interaction with amino groups of the functionalized Hal. Moreover, the  
 429 functionalization of Hal in HD and HT adsorbents occurs in the interlayers of Hal.

430

431 **Table 4.** Literature maximum adsorption capacity values ( $q_m$ ) of different clay minerals

<b>p or m clay<sup>a</sup></b>	<b><math>q_m^b</math></b>	<b>ref</b>
p-kaol <sup>c</sup>	0.12–11.50	(Jiang et al., 2009; Oubagaranadin and Murthy, 2009; Uddin, 2017)
m-Kaol	25.13–82.65	(Jiang et al., 2009; Uddin, 2017)
p-Mont	31.10–37.16	(Sdiri et al., 2016; Uddin, 2017)
m-Mont	71.92-121.95	(Hu et al., 2017; Uddin, 2017)
p-Smec	3.13 – 75.35	(Uddin, 2017)
p-Sep	30.5	(Sdiri et al., 2016)
p-Bent	28.00 - 51.19	(Sdiri et al., 2016; Uddin, 2017)

m-Bent	110	(Uddin, 2017)
p-Pal	62.1	(Oubagaranadin and Murthy, 2009)
p-Hal	6 - 8	(Matusik and Wscislo, 2014; Maziarz et al., 2015), this work
m-Hal	12.18 - 46	(He et al., 2013; Matusik and Wscislo, 2014), this work

432 <sup>a</sup> p = pristine, m = modified; <sup>b</sup> mg g<sup>-1</sup>; c Kaol = Kaolinite; Mont = Montmorillonite; Smec =  
433 Smectite; Sep = Sepiolite, Bent = Bentonite, Pal = Palygorskite.

434

#### 435 **4. Conclusions**

436 Functionalized halloysite nanotubes with amino groups (Hal-NH<sub>2</sub>) have been successfully  
437 employed as adsorbent for Pb<sup>2+</sup> ions. Their adsorption ability was kinetically and  
438 thermodynamically studied. Results were compared with that of p-Hal in NaCl aqueous solutions  
439 and in the pH range 3 -6. The best experimental conditions for the metal ion removal were  
440 established on the basis of a speciation study of Pb<sup>2+</sup> and of the p-Hal. The results obtained can be  
441 summarized as follows:

- 442 1. FT-IR, TGA and contact angle analysis on Hal-NH<sub>2</sub> material confirm the successful outcome  
443 of synthesis with a 2.4 wt% loading of organic moiety on the nanomaterial, whilst, the  
444 preservation of morphology of p-Hal after organosilane grafting was showed by SEM  
445 analysis;
- 446 2. several kinetic and isotherm equations were used to fit experimental data and the parameters  
447 of the most suitable models were analyzed to discuss the adsorption performances of the two  
448 adsorbent materials;
- 449 3. an improvement of the adsorption ability of both pristine and functionalized p-Hal materials  
450 was found with the increasing of pH and the decreasing of ionic strength;
- 451 4. the adsorption ability of amino-functionalized Hal-NH<sub>2</sub> towards Pb<sup>2+</sup> is considerable higher  
452 than that of p-Hal and of other functionalized halloysite reported in literature.

453 5. The Hal-NH<sub>2</sub> shows a noticeable reuse capability that encourages the use of this material as  
454 adsorbent of Pb<sup>2+</sup> ions in the pH and ionic strength ranges considered.

455

#### 456 **Acknowledgements**

457 We thank the Italian Ministero dell'Istruzione, dell'Università e della Ricerca (MIUR, PRIN project  
458 2015MP34H3\_004) for financial support.

459

460

461 **References**

- 462 Baes, C.F., Mesmer, R.E., 1976. *The Hydrolysis of Cations*. John Wiley & Sons, New York.
- 463 Bretti, C., Cataldo, S., Gianguzza, A., Lando, G., Lazzara, G., Pettignano, A., Sammartano, S.,  
464 2016. Thermodynamics of Proton Binding of Halloysite Nanotubes. *J. Phys. Chem. C* 120, 7849-  
465 7859.
- 466 Cataldo, S., Muratore, N., Orecchio, S., Pettignano, A., 2015. Enhancement of adsorption ability of  
467 calcium alginate gel beads towards Pd(II) ion. A kinetic and equilibrium study on hybrid Laponite  
468 and Montmorillonite-alginate gel beads. *Appl. Clay Sci.* 118, 162-170.
- 469 Cavallaro, G., Lazzara, G., Massaro, M., Milioto, S., Noto, R., Parisi, F., Riela, S., 2015.  
470 Biocompatible Poly(N-isopropylacrylamide)-halloysite Nanotubes for Thermoresponsive Curcumin  
471 Release. *J. Phys. Chem. C* 119, 8944-8951.
- 472 Cavallaro, G., Lazzara, G., Milioto, S., Parisi, F., Sanzillo, V., 2014. Modified Halloysite  
473 Nanotubes: Nanoarchitectures for Enhancing the Capture of Oils from Vapor and Liquid Phases.  
474 *ACS Appl. Mater. Inter.* 6, 606-612.
- 475 De Stefano, C., Sammartano, S., Mineo, P., Rigano, C., 1997. Computer Tools for the Speciation of  
476 Natural Fluids, in: Gianguzza, A., Pelizzetti, E., Sammartano, S. (Eds.), *Marine Chemistry - An  
477 Environmental Analytical Chemistry Approach*. Kluwer Academic Publishers, Amsterdam, pp. 71-  
478 83.
- 479 Dong, Y., Liu, Z., Chen, L., 2012. Removal of Zn(II) from aqueous solution by natural halloysite  
480 nanotubes. *J. Radioanal. Nucl. Chem.* 292, 435-443.
- 481 Fan, L., Zhang, J., Wang, A., 2013. In situ generation of sodium alginate/hydroxyapatite/halloysite  
482 nanotubes nanocomposite hydrogel beads as drug-controlled release matrices. *J. Mater. Chem. B* 1,  
483 6261-6270.
- 484 Förstner, U., Salomons, W., Mader, P., eds., 1995. *Heavy Metals, Problems and Solutions*.  
485 Springer-Verlag Berlin Heidelberg.
- 486 Gerente, C., Lee, V.K.C., Cloirec, P.L., McKay, G., 2007. Application of Chitosan for the Removal  
487 of Metals From Wastewaters by Adsorption-Mechanisms and Models Review. *Crit. Rev. Env. Sci.*  
488 *Technol.* 37, 41-127.
- 489 Gidlow, D.A., 2015. Lead toxicity. *Occupational Medicine* 65, 348-356.
- 490 He, Q., Yang, D., Deng, X., Wu, Q., Li, R., Zhai, Y., Zhang, L., 2013. Preparation, characterization  
491 and application of N-2-Pyridylsuccinamic acid-functionalized halloysite nanotubes for solid-phase  
492 extraction of Pb(II). *Water Research* 47, 3976-3983.
- 493 Hebbar, R.S., Isloor, A.M., Ananda, K., Ismail, A.F., 2016. Fabrication of polydopamine  
494 functionalized halloysite nanotube/polyetherimide membranes for heavy metal removal. *J. Mater.*  
495 *Chem. A* 4, 764-774.
- 496 Ho, Y.-S., 2006. Review of second-order models for adsorption systems. *J. Hazard. Mater.* 136,  
497 681-689.
- 498 Hu, C., Zhu, P., Cai, M., Hu, H., Fu, Q., 2017. Comparative adsorption of Pb(II), Cu(II) and Cd(II)  
499 on chitosan saturated montmorillonite: Kinetic, thermodynamic and equilibrium studies. *Appl. Clay  
500 Sci.* 143, 320-326.
- 501 Jiang, M.-q., Wang, Q.-p., Jin, X.-y., Chen, Z.-l., 2009. Removal of Pb(II) from aqueous solution  
502 using modified and unmodified kaolinite clay. *J. Hazard. Mater.* 170, 332-339.
- 503 Jinhua, W., Xiang, Z., Bing, Z., Yafei, Z., Rui, Z., Jindun, L., Rongfeng, C., 2010. Rapid adsorption  
504 of Cr (VI) on modified halloysite nanotubes. *Desalination* 259, 22-28.
- 505 Joussein, E., Petit, S., Churchman, J., Theng, B., Righi, D., Delvaux, B., 2005. Halloysite clay  
506 minerals - a review. *Clay Miner.* 40, 383-426.
- 507 Kurczewska, J., Grzesiak, P., Lukaszyk, J., Gabala, E., Schroeder, G., 2015. High decrease in soil  
508 metal bioavailability by metal immobilization with halloysite clay. *Environ. Chem. Lett.* 13, 319-  
509 325.

510 Liu, M., Chang, Y., Yang, J., You, Y., He, R., Chen, T., Zhou, C., 2016. Functionalized halloysite  
511 nanotube by chitosan grafting for drug delivery of curcumin to achieve enhanced anticancer  
512 efficacy. *J. Mater. Chem. B* 4, 2253-2263.

513 Liu, M., Jia, Z., Liu, F., Jia, D., Guo, B., 2010. Tailoring the wettability of polypropylene surfaces  
514 with halloysite nanotubes. *J. Colloid Interf. Sci.* 350, 186-193.

515 Luo, Y., Millero, F.J., 2007. Stability constants for the formation of lead chloride complexes as a  
516 function of temperature and ionic strength. *Geochim. Cosmochim. Ac.* 71, 326-334.

517 Lvov, Y., Wang, W., Zhang, L., Fakhrullin, R., 2015. Halloysite Clay Nanotubes for Loading and  
518 Sustained Release of Functional Compounds. *Advanced Materials* 28, 1227-1250.

519 Lvov, Y.M., DeVilliers, M.M., Fakhrullin, R.F., 2016. The application of halloysite tubule nanoclay  
520 in drug delivery. *Expert Opinion on Drug Delivery* 13, 977-986.

521 Mason, L.H., Harp, J.P., Han, D.Y., 2014. Pb Neurotoxicity: Neuropsychological Effects of Lead  
522 Toxicity. *BioMed Res. Int.* 2014, 8.

523 Massaro, M., Colletti, C.G., Lazzara, G., Guernelli, S., Noto, R., Riela, S., 2017. Synthesis and  
524 Characterization of Halloysite - Cyclodextrin Nanosponges for Enhanced Dyes Adsorption. *ACS*  
525 *Sust. Chem. Eng.* 5, 3346 - 3352.

526 Massaro, M., Riela, S., Baiamonte, C., Blanco, J.L.J., Giordano, C., Lo Meo, P., Milioto, S., Noto,  
527 R., Parisi, F., Pizzolanti, G., Lazzara, G., 2016a. Dual drug-loaded halloysite hybrid-based  
528 glycocluster for sustained release of hydrophobic molecules. *RSC Advances* 6, 87935-87944.

529 Massaro, M., Schembri, V., Campisciano, V., Cavallaro, G., Lazzara, G., Milioto, S., Noto, R.,  
530 Parisi, F., Riela, S., 2016b. Design of PNIPAAm covalently grafted on halloysite nanotubes as a  
531 support for metal-based catalysts. *RSC Advances* 6, 55312-55318.

532 Matusik, J., 2014. Arsenate, orthophosphate, sulfate, and nitrate sorption equilibria and kinetics for  
533 halloysite and kaolinites with an induced positive charge. *Chemical Engineering Journal* 246, 244-  
534 253.

535 Matusik, J., 2016. Halloysite for Adsorption and Pollution Remediation, in: Yuan, P., Thill, A.,  
536 Bergaya, F. (Eds.), *Nanosized Tubular Clay Minerals - Halloysite and Imogolite* Elsevier, pp. 606-  
537 627.

538 Matusik, J., Wscislo, A., 2014. Enhanced heavy metal adsorption on functionalized nanotubular  
539 halloysite interlayer grafted with aminoalcohols. *Appl. Clay Sci.* 100, 50-59.

540 Maziarz, P., Prokop, A., Matusik, J., 2015. A comparative study on the removal of Pb(II), Zn(II),  
541 Cd(II) and As(V) by natural, acid activated and calcinated halloysite. *Geol. Geophys. Env.* 41, 108-  
542 109.

543 Meng, Q., Chen, H., Lin, J., Lin, Z., Sun, J., 2016. Zeolite A synthesized from alkaline assisted pre-  
544 activated halloysite for efficient heavy metal removal in polluted river water and industrial  
545 wastewater. *J. Environ. Sci.*, in press.

546 Oubagaranadin, J.U.K., Murthy, Z.V.P., 2009. Adsorption of Divalent Lead on a Montmorillonite -  
547 Illite Type of Clay. *Ind. Eng. Chem. Res.* 48, 10627-10636.

548 Park, D., Yun, Y.-S., Park, J.M., 2010. The past, present, and future trends of biosorption.  
549 *Biotechnol. Bioproc. E.* 15, 86-102.

550 Peng, Q., Liu, M., Zheng, J., Zhou, C., 2015. Adsorption of dyes in aqueous solutions by chitosan -  
551 halloysite nanotubes composite hydrogel beads. *Micropor. Mesopor. Mat.* 201, 190-201.

552 Rawtani, D., Pandey, G., Tharmavaram, M., Pathak, P., Akkireddy, S., Agrawal, Y.K., 2017.  
553 Development of a novel "nanocarrier" system based on Halloysite Nanotubes to overcome the  
554 complexation of ciprofloxacin with iron: An in vitro approach. *Appl. Clay Sci.* 150, 293-302.

555 Riela, S., Massaro, M., Colletti, C.G., Bommarito, A., Giordano, C., Milioto, S., Noto, R., Poma, P.,  
556 Lazzara, G., 2014. Development and characterization of co-loaded curcumin/triazole-halloysite  
557 systems and evaluation of their potential anticancer activity. *Int. J. Pharm.* 475, 613-623.

558 Sabbagh, N., Akbari, A., Arsalani, N., Eftekhari-Sis, B., Hamishekar, H., 2017. Halloysite-based  
559 hybrid bionanocomposite hydrogels as potential drug delivery systems. *Appl. Clay Sci.* 148, 48-55.

560 Sadjadi, S., Atai, M., 2018. Ternary hybrid system of halloysite nanotubes, polyacrylamides and  
561 cyclodextrin: an efficient support for immobilization of Pd nanoparticles for catalyzing coupling  
562 reaction. *Appl. Clay Sci.* 153, 78-89.

563 Sdiri, A., Khairy, M., Bouaziz, S., El-Safty, S., 2016. A natural clayey adsorbent for selective  
564 removal of lead from aqueous solutions. *Appl. Clay Sci.* 126, 89-97.

565 Silva, R.T.D., Pooria, P., Goh, K.L., Chai, S.P., Chen, J., 2013. Synthesis and characterisation of  
566 poly (lactic acid)/halloysite bionanocomposite films. *J. Compos. Mater.* 48, 3705-3717.

567 Tan, D., Yuan, P., Liu, D., Du, P., 2016. Surface Modifications of Halloysite, in: Yuan, P., Thill,  
568 A., Bergaya, F. (Eds.), *Nanosized Tubular Clay Minerals - Halloysite and Imogolite*. Elsevier, pp.  
569 167-201.

570 Uddin, M.K., 2017. A review on the adsorption of heavy metals by clay minerals, with special focus  
571 on the past decade. *Chemical Engineering Journal* 308, 438-462.

572 Yuan, P., Southon, P.D., Liu, Z., Green, M.E.R., Hook, J.M., Antill, S.J., Kepert, C.J., 2008.  
573 Functionalization of Halloysite Clay Nanotubes by Grafting with  $\gamma$ -Aminopropyltriethoxysilane. *J.*  
574 *Phys. Chem. C* 112, 15742-15751.

575 Yuan, P., Southon, P.D., Liu, Z., Kepert, C.J., 2012. Organosilane functionalization of halloysite  
576 nanotubes for enhanced loading and controlled release. *Nanotechnology* 23, 375705.

577 Yuan, P., Tan, D., Bergaya, F.A., 2015. Properties and applications of halloysite nanotubes: recent  
578 research advances and future prospects. *Appl. Clay Sci.* 112-113, 75-93.

579 Zeng, G., He, Y., Zhan, Y., Zhang, L., Pan, Y., Zhang, C., Yu, Z., 2016. Novel polyvinylidene  
580 fluoride nanofiltration membrane blended with functionalized halloysite nanotubes for dye and  
581 heavy metal ions removal. *J. Hazard. Mater.* 317, 60-72.

582 Zhao, Y., Abdullayev, E., Vasiliev, A., Lvov, Y., 2013. Halloysite nanotubule clay for efficient  
583 water purification. *J. Colloid Interf. Sci.* 406, 121-129.

584 Zhu, K., Duan, Y., Wang, F., Gao, P., Jia, H., Ma, C., Wang, C., 2017. Silane-modified  
585 halloysite/Fe<sub>3</sub>O<sub>4</sub> nanocomposites: Simultaneous removal of Cr(VI) and Sb(V) and positive effects  
586 of Cr(VI) on Sb(V) adsorption. *Chem. Eng. J.* 311, 236-246.

587  
588  
589