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# Effect of pruning-derived biochar on heavy metals removal and water dynamics

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**Abstract** Biomass-derived biochar is considered as a promising heavy metal adsorbent, due to abundance of polar functional groups, such as carboxylic, hydroxyl, and amino groups, which are available for heavy metal removal. The aims of this study were to evaluate the effectiveness of an orchard pruning-derived biochar in removing some heavy metals (through the evaluation of isotherms) and to study water dynamics at the solid-liquid interface as affected by heavy metal adsorption (through an innovative nuclear magnetic resonance (NMR) relaxometry approach). Both isotherms and NMR spectra revealed that Pb and Cr showed a good affinity for the biochar surface ( $Pb > Cr$ ), while Cu was less affine. Accordingly, higher amounts of Pb and Cr were adsorbed by biochar as compared to those of Cu in the single systems. In binary systems (i.e., when two metals were applied simultaneously), Pb showed the highest inhibition of the adsorption of the other two metals, whereas the opposite was evidenced when Cu was used; the competitive adsorption was also strongly influenced by the metal residence time on biochar surface. In ternary systems (i.e., when all metals were applied simultaneously), even in the presence of high amounts of Pb and Cr, considerable adsorption of Cu occurred, indicating that some biochar adsorption sites were highly specific for a single metal.

**Keywords** Biochar · Heavy metals · Lead · Chromium · Copper · Water dynamics · NMR relaxometry

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## Introduction

Heavy metals, such as lead (Pb), chromium (Cr), and copper (Cu) pose a risk to public health because of their toxic and non-biodegradable nature and widespread occurrence in natural and human-altered environments (Inyang et al. 2012; Regmi et al. 2012). They are mainly introduced into aquatic environments from point sources as discharges from mining, metal processing, tanneries, pharmaceuticals, pesticides, organic chemicals, rubber and plastics, and lumber and wood products (Shi et al. 2009). Conventional technologies for the removal and recovery of heavy metals from wastewaters include chemical precipitation, ion exchange, electrochemistry removal, membrane separation, microbe separation, adsorption by activated carbon, and so on (Srivastava and Majumder 2008). However, most of these methods suffer from some drawbacks, such as high capital, high operational cost, and the disposal of resulting sludge. Therefore, it is needed to develop a novel method, which is not only cost-effective but also readily implemented. Adsorption appears to be a good choice if a low-cost adsorbent is applied (Shi et al. 2009). Biomass-derived biochar is considered as a promising heavy metal adsorbent (Mohan et al. 2007; Qiu et al. 2008; Liu and Zhang 2009; Beesley and Marmiroli 2011; Li et al. 2013), due to abundance of polar functional groups, such as carboxylic, hydroxyl, and amino groups, which are available for heavy metal removal (Cao et al. 2009; Hsu et al. 2009; Wang et al. 2010). Biochar is a fine-grained carbonaceous solid residue, produced by pyrolysis of carbon-rich biomass under oxygen-limited conditions (Chen et al. 2011; Xu et al. 2013). In recent years, biochar has also received considerable interest as a large-scale soil amendment to enhance crop productivity and soil fertility (Major et al. 2010; Vaccari et al. 2011; Farrell et al. 2014; Prayogo et al. 2014; Song et al. 2014), to increase soil water holding capacity (Kammann et al. 2011; Baronti et al. 2014), to decrease nutrient leaching

(Laird et al. 2010), and to serve as a recalcitrant carbon stock (Lehmann 2007a, b; Laird 2008) to potentially mitigating climate changes (Conte et al. 2013; Cimò et al. 2014) by reducing greenhouse gas emissions (Castaldi et al. 2011; Stewart et al. 2013). Biochar has many properties, such as a relatively structured carbon matrix, high degree of microporosity, extensive surface area, and high pH and cation exchange capacity (CEC); therefore, it may act as a surface adsorbent (Jiang et al. 2012a, b). Given that it is highly recalcitrant, the beneficial effects of its application may be prolonged over a long period of time (Fellet et al. 2011; De Pasquale et al. 2012). Charred biomasses, on the other hand, are estimated to have mean residence times of thousands of years in soils (Lehmann et al. 2008). Many studies have investigated the adsorption of Pb, Cr, and Cu on biochar in single sorbate systems (Liu and Zhang 2009; Mohan et al. 2011; Tong et al. 2011; Lu et al. 2012; Shen et al. 2012; Li et al. 2013). However, as metals usually coexist in the environment and undergo competitive sorption (Zhu et al. 2010; Chen et al. 2011), the study of systems with a mixture of contaminants is paramount. In the present study, we studied the following: (i) Pb, Cr, and Cu adsorption capacities of a commercial orchard pruning-derived biochar, at pH 4.5 and 20 °C, in single sorbate systems; (ii) the competitive adsorption of metals in binary and ternary systems, affected by their initial concentration and residence time on biochar surface; and (iii) the water molecular dynamics on the surface of the porous biochar, as affected by metal adsorption, by fast-field-cycling nuclear magnetic resonance (NMR) relaxometry. The latter technique allowed us to investigate the water movement inside biochar pores through the measurement of the longitudinal relaxation times ( $T_1$ ), which provide information on the way as water molecules are constricted in a porous media. Knowledge of water movement in porous media containing adsorbed metals is very important in order to understand the role of metals in the nutrient transport toward plant roots. In addition, the study of water movements in biochar pores, before and after Pb, Cr, and/or Cu adsorption is also useful for the recognition of the nature of biochar-metal bonds at the solid-liquid interface.

## Materials and methods

### Biochar collection

The orchard pruning-derived biochar applied in the present study is a commercial charcoal made by Romagna Carbone snc (Italy), obtained from orchard pruning biomass through a slow pyrolysis process at temperature of 500 °C, in a transportable ring kiln of 2.2 m in diameter and holding around 2 t of feedstock. The biochar at the end of the pyrolysis was

crushed into <5-cm particles before selling (Baronti et al. 2014). A suitable amount of this biochar was allowed to air-dry, milled in a china mortar, and subsequently passed through a sieve having 500  $\mu\text{m}$  of pore diameters, in order to obtain an homogeneous sample for adsorption experiments and NMR relaxometry investigations.

### Biochar characterization

In order to determine the functional groups in the biochar sample, the Fourier transform infrared (FT-IR) spectrum was acquired in the range of 400–4000  $\text{cm}^{-1}$  by Perkin-Elmer Frontier FT-IR/NIR Spectrometer (Perkin Elmer USA), with a spectral resolution of 1  $\text{cm}^{-1}$ .

### NMR relaxometry investigations

All samples were first suspended in deionized water, then analyzed by a Stelar Spinmaster Fast Field Cycling Relaxometry instrument at a constant temperature of 25 °C. The bases for the FFC NMR relaxometry have been reported by Conte and Alonzo (2013). For this reason, here, we only report the experimental conditions applied in the present study. Namely, all experiments were conducted at the fixed relaxation field ( $B_{RLX}$ ) of 0.5 T, with the period  $\tau$ , during which  $B_{RLX}$  was applied, varying on 32 logarithmic spaced time sets; 16 scans were set with a recycle delay of 2 s. No polarization field ( $B_{POL}$ ) has been applied so that all measurements were done in non-polarized (NP) mode. A  $^1\text{H}$  90° pulse was applied at an acquisition field ( $B_{ACQ}$ ) of 0.18 T in order to retrieve the free induction decay (FID) with a time domain of 100  $\mu\text{s}$  and 512 points. Field switching time was 3 ms, while spectrometer dead time was 15  $\mu\text{s}$ . All recovery curves were evaluated by the UPEN algorithm (Alma Mater Studiorum, Università di Bologna, Italy) (Conte and Alonzo 2013) with the aim to obtain the longitudinal relaxation time ( $T_1$ ) distributions, and therefore, information on the way water molecules are trapped in each sample (Conte et al. 2013). The  $T_1$  distribution curves were exported to OriginPro 7.5 SR6 (version 7.5885, OriginLab Corporation, Northampton, MA, USA) in order to perform deconvolution with Gaussian functions and to recover the different components giving rise to the longitudinal relaxation time distributions. The Gaussian curves were combined to obtain the best fitting of experimental data. Deconvolution was considered optimum when the coefficient of determination ( $R^2$ ) for the best fitting resulted  $\geq 0.98$ .

### Adsorption isotherms

Suitable volumes of 50  $\text{mmol L}^{-1}$  solutions containing Pb as  $\text{Pb}^{\text{II}}(\text{NO}_3)_2$ , Cr as  $\text{Cr}^{\text{III}}(\text{NO}_3)_3$ , or Cu as  $\text{Cu}^{\text{II}}(\text{NO}_3)_2$  (Sigma-Aldrich, USA) were added to 100 mg of biochar samples in



50-mL conical flasks. Initial Pb and Cr concentrations ranged from 0.05 to 1.0 mmol L<sup>-1</sup>, whereas Cu concentration ranged from 0.03 to 0.75 mmol L<sup>-1</sup>. The final volume was adjusted to 20 mL with 1.0 mM KNO<sub>3</sub>, in order to have an initial biochar/solution ratio of 5 g L<sup>-1</sup>. The pH of each suspension was kept constant at 4.5 for 5 h at 20 °C by adding 10 mM HNO<sub>3</sub> or 10 mM KOH using an automatic titrator (Potentiograph E536 Metrom Herisau) connected to an automatic syringe (burette 655 Dosimat). The operation was done in order to avoid metal precipitation, which can occur at pH values higher than 4.5 (Zhu et al. 2010). The final suspension was centrifuged at 10,000g for 20 min and filtered through Nalgene acetate membrane (pore size <0.22 μm). The concentration of metals in the final solution was determined by flame atomic adsorption spectrometry using a Perkin-Elmer AAnalyst 700. The adsorption of metals by biochar was calculated by the difference between the amounts of metals initially added and those remained in the supernatant; in preliminary experiments, the washing after metal adsorption removed negligible amounts of metals.

#### Competitive adsorption in binary and ternary systems

Competitive adsorption of Pb, Cr, and Cu in binary systems was observed at pH 4.5, by adding simultaneously Pb and Cr, Pb and Cu, or Cr and Cu to 100 mg of biochar samples in 50-mL conical flasks. The concentration of Pb or Cr in the Pb–Cr binary system ranged from 25 to 75 mmol kg<sup>-1</sup>, whereas the concentration of Pb, Cr, or Cu in the Pb–Cu and Cr–Cu binary systems ranged from 20 to 60 mmol kg<sup>-1</sup>, so as to have initial Pb/Cr, Pb/Cu, or Cr/Cu molar ratios ( $R_i$ ) ranging between 0.33 and 3.0. Experiments were also carried out by adding a metal (Pb, Cr, or Cu) to 100 mg of biochar 1 h before the second metal, and then the metal mixture was incubated with biochar for 5 h at pH 4.5 and 20 °C, so as to evaluate the relationships between the metal residence time and the biochar adsorption capacity. Competitive adsorption of Pb, Cr, and Cu in ternary systems was investigated at pH 4.5, by adding simultaneously Pb, Cr, and Cu to 100 mg of biochar samples in 50-mL conical flasks. The concentration of each metal ranged from 20 to 60 mmol kg<sup>-1</sup>, with different initial Pb/Cr/Cu molar ratios. The final volume of each suspension of binary and ternary systems was adjusted to 20 mL with 1.0 mM KNO<sub>3</sub>, in order to have an initial biochar/solution ratio of 5 g L<sup>-1</sup>. The pH was kept constant at 4.5 for 5 h at 20 °C by adding 10 mM HNO<sub>3</sub> or 10 mM KOH using an automatic titrator (Potentiograph E536 Metrom Herisau) connected to an automatic syringe (burette 655 Dosimat). The final suspension was centrifuged at 10,000g for 20 min and filtered through Nalgene acetate membrane (pore size <0.22 μm). The supernatant was collected, and the concentration of heavy metals was determined as described above.

**Table 1** FT-IR assignments

Wavenumber (cm <sup>-1</sup> )	Possible assignments
3,546	Oxydrils and unsubstituted amides involved in H bonds
3,470	N-monosubstituted amides
3,413	–NH in amine groups
3,232, 3,118, 2,034	C–H in aromatic compounds
1,637	NN-disubstituted amides
1,617, 1,400	Carboxylate groups
1,126	C–O groups

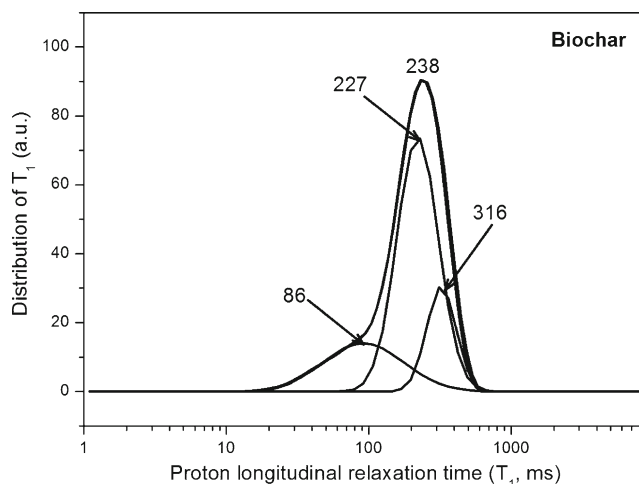
## Results

### Nature of the biochar

The physicochemical properties of the pruning-derived biochar have been described by Baronti et al. (2014). The total biochar porosity was 2,722 mm<sup>3</sup> g<sup>-1</sup>, while the specific surface area resulted 410±6 m<sup>2</sup> g<sup>-1</sup>. Moreover, three kinds of pores was identified: transmission (≥50 μm), storage (0.5–50 μm), and residual (<0.5 μm) pores, which accounted for 10, 75, and 15 % of the total porosity, respectively. Table 1 reports the main FT-IR bands with all the possible assignments of the functional groups present in the biochar. In addition, the physical properties of biochar and the heavy metal contaminated biochar have been investigated by low field <sup>1</sup>H NMR relaxometry with fast field cycling setup. Figures 1, 2, 3, and 4 report all the proton longitudinal relaxation ( $T_1$ ) distributions.

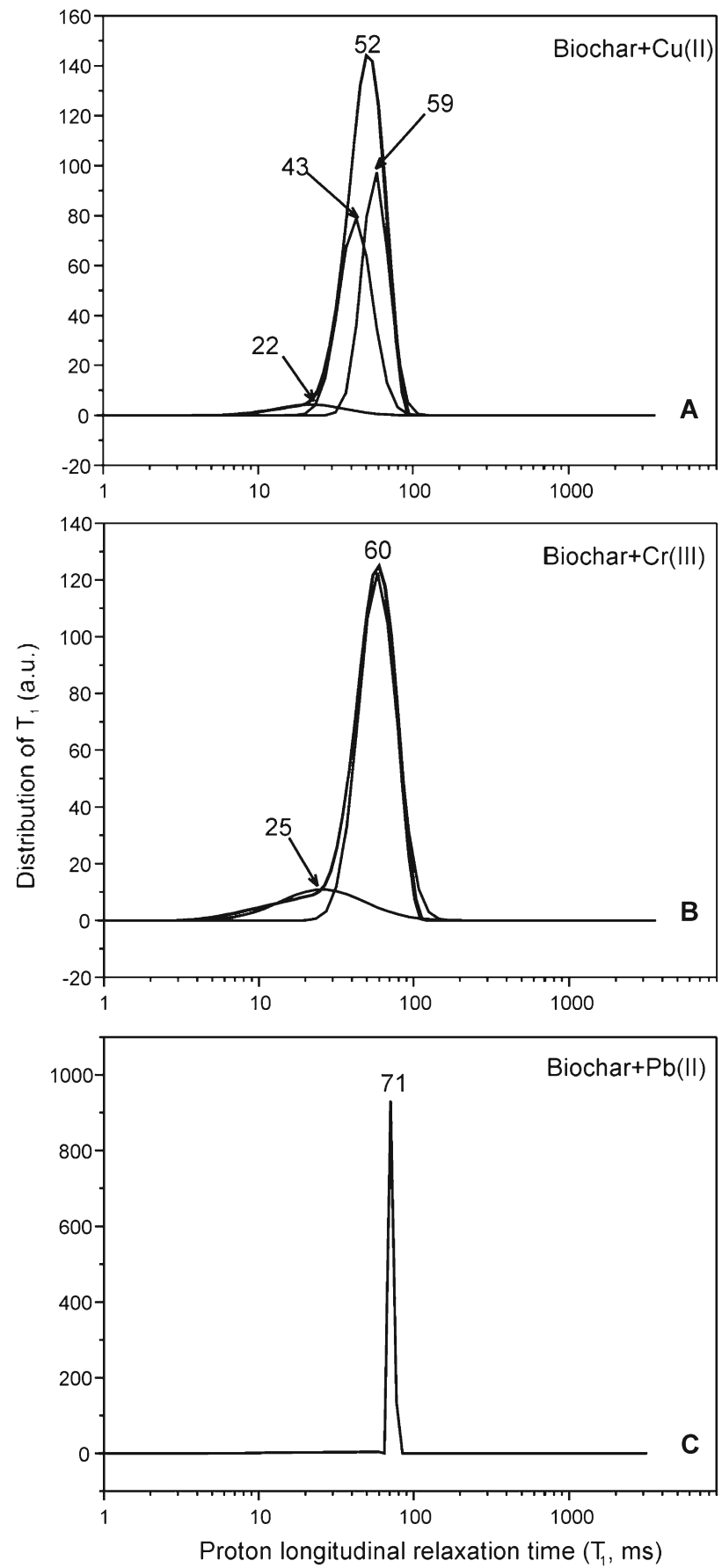
### Adsorption isotherms

The adsorption isotherms of Pb, Cr, and Cu, added individually onto biochar samples at pH 4.5, are shown in Fig. 5 and

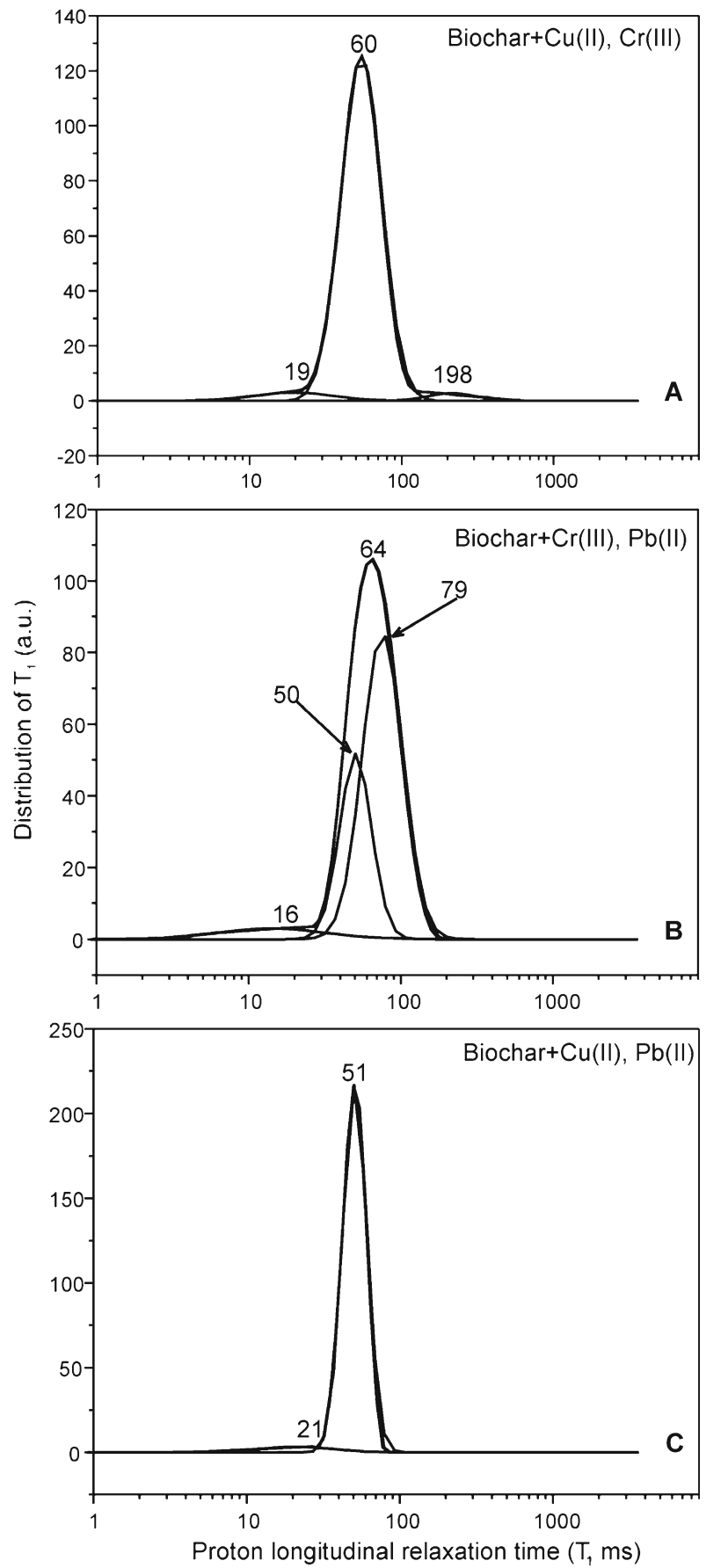


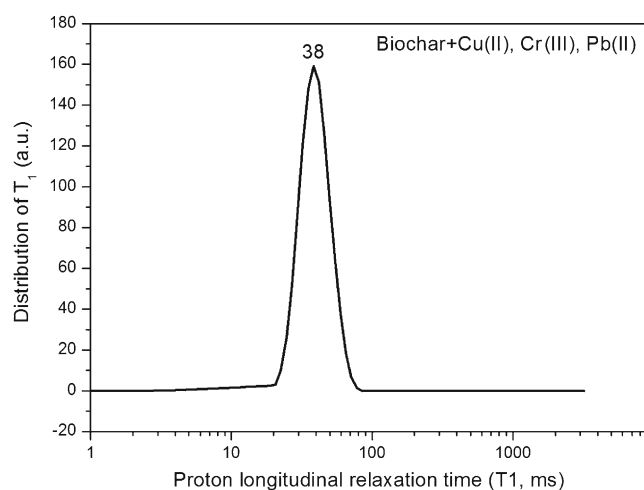
**Fig. 1** Longitudinal relaxation times ( $T_1$ ): distribution of the sole biochar

**Fig. 2** Longitudinal relaxation times ( $T_1$ ): distributions of Cu-adsorbed (a), Cr-adsorbed (b), and Pb-adsorbed (c) biochar samples



**Fig. 3** Longitudinal relaxation times ( $T_1$ ): distributions of Cu,Cr-adsorbed (a), Cr,Pb-adsorbed (b), and Cu,Pb-adsorbed (c) biochar samples



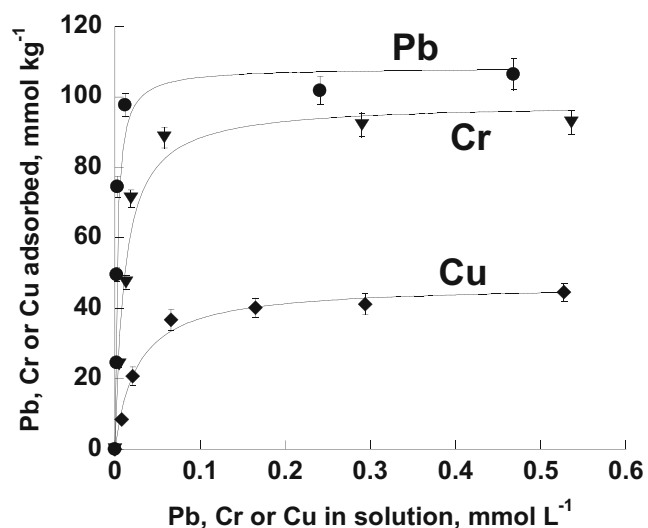


**Fig. 4** Longitudinal relaxation times ( $T_1$ ): distribution of Cu, Cr, Pb-adsorbed biochar

described by Langmuir equation:  $S = S_m Kc / (1 + Kc)$ , where  $S$  is the amount of each metal adsorbed per unit mass of adsorbent ( $\text{mmol kg}^{-1}$ ),  $S_m$  is the maximum amount that may be bound to the adsorbent (adsorption capacity) (Table 2),  $c$  is the equilibrium concentration ( $\text{mmol L}^{-1}$ ), and  $K$  is a constant related to the binding energy (Table 2).

#### Competitive adsorption of Pb, Cr, and Cu in binary systems

The competitive adsorption of Pb vs. Cr, Pb vs. Cu, and Cr vs. Cu on biochar was reported in Tables 3, 4, and 5, respectively. In the binary systems, Pb showed the highest inhibition of the adsorption of the other two metals, with a reduction of Cr and Cu adsorption on biochar surface by 36.2 and 73.5 %, respectively, as compared to the amounts adsorbed from single sorbate systems (Tables 3 and 4). Chromium also strongly



**Fig. 5** Adsorption isotherms of Pb, Cr, and Cu on biochar at pH 4.5 and 20 °C, after 5 h of reaction time.

**Table 2** Langmuir adsorption capacities ( $S_m$ ) and  $K$  constant for Pb, Cr, and Cu, as obtained from the adsorption isotherms of the biochar at pH 4.5 and 20 °C, after 5 h of reaction time

Heavy metal	$S_m$ ( $\text{mmol kg}^{-1}$ )	$K$	$R^2$
Pb	108.2 (0.264)	21.4	0.97
Cr	98.3 (0.240)	15.8	0.96
Cu	46.5 (0.113)	4.5	0.99

Numbers in brackets indicate the amount of Pb, Cr, and Cu adsorbed as  $\mu\text{mol m}^{-2}$ . Specific surface area ( $410 \text{ m}^2 \text{ g}^{-1}$ ) of biochar was determined by Baronti et al. (2014), by the dynamic Brunauer-Emmett-Teller (BET) method with  $\text{N}_2$  as adsorbate

inhibited Cu adsorption on biochar because of its greater adsorption affinity (Table 5). The presence of many high-affinity adsorption sites for Pb and Cr on biochar surface determined a relatively low inhibition of metal adsorption by biochar, in the Pb–Cr binary system (Table 3), especially at the lowest concentration ( $25 \text{ mmol kg}^{-1}$ ).

#### Effect of metal residence time on biochar adsorption capacity

The adsorption of Pb, Cr, and Cu on biochar in binary systems was also affected by metal residence time on biochar surface (Figs. 6, 7, and 8). Unlike the binary systems described above, where two metals were simultaneously added to biochar samples, here, the first metal was added 1 h before the second metal, followed by incubation of the metal mixture with biochar for 5 h at pH 4.5. We found that the adsorption of the first metal added on biochar was higher if compared to that obtained with the simultaneous addition of two metals, whereas the opposite was shown for the second metal added to the system (Figs. 6, 7, and 8); we also noted that the intensity of change in adsorption of three metals was strictly related to the affinity of these toxicants for biochar surface. When Pb was added as first metal, we observed that its adsorption on biochar increased more intensely than adsorption of the other two metals; vice versa, when Pb was added as second metal, its adsorption decreased to a lesser extent if compared to those of Cr and Cu (Figs. 6, 7, and 8). Being the kinetics of Pb, Cr, and Cu adsorption very fast (around the 80–90 % of the metal initially added was adsorbed by biochar in the first hour of reaction, followed by a much slower adsorption rate in the subsequent 4 h with negligible adsorption after 5 h) (data not shown), it is conceivable that the first metal added on biochar surface readily occupied most of the adsorption sites.

#### Competitive adsorption of Pb, Cr, and Cu in ternary systems

Competitive adsorption studies were also carried out by adding Pb, Cr, and Cu simultaneously on biochar samples at pH 4.5 (Table 6). When equimolar amounts of each metal were initially added (20, 40, or  $60 \text{ mmol kg}^{-1}$ ) to biochar, the



**Table 3** Competitive adsorption of Pb and Cr on biochar at pH 4.5 and 20 °C, after 5 h of incubation

Added amounts (mmol kg <sup>-1</sup> )		Adsorbed amounts (mmol kg <sup>-1</sup> )		Initial ratio ( $R_i$ ) <sup>a</sup>	Final ratio ( $R_f$ ) <sup>b</sup>	Adsorption inhibition (%) <sup>c</sup>	
Pb	Cr	Pb	Cr	Pb/Cr		Pb	Cr
25	25	23±1	20.4±0.9	1.00	1.12	7.4	11.2
25	50	22±1	38±2	0.50	0.56	12.4	15.3
25	75	19.8±0.9	57±4	0.33	0.35	19.4	17.1
50	25	43±2	19±1	2.00	2.32	12.6	18.3
50	50	42±2	36±2	1.00	1.18	15.8	21.4
50	75	39±3	53±4	0.67	0.74	20.7	22.6
75	25	61±3	17.3±0.7	3.00	3.52	18.0	24.3
75	50	57±3	32±2	1.50	1.78	23.3	28.8
75	75	50±3	44±3	1.00	1.14	33.3	36.2

Adsorbed amounts of Pb and Cr are the average of at least three different replicates ( $n=3$ )

<sup>a</sup>  $R_i$  stands for the Pb/Cr molar ratio initially added on biochar samples

<sup>b</sup>  $R_f$  indicates the Pb/Cr molar ratio finally adsorbed on biochar surface

<sup>c</sup> Inhibition (%) of Pb or Cr adsorption was calculated by subtracting the amount of Pb or Cr adsorbed in presence of the other metal from that adsorbed in the absence of the other metal, divided by the amount adsorbed in the absence of the other metal, multiplied per 100

adsorbing surface was covered by 42.3–53.6 % with Pb, 35.5–38.6 % with Cr, and 7.8–22.2 % with Cu (Table 6). It is noteworthy that even adding an initial Pb concentration twice or triple higher than that of Cr and Cu (Pb, Cr, and Cu added amounts of 40, 20, and 20 or 60, 20, and 20 mmol kg<sup>-1</sup>), biochar adsorption sites were still occupied by Cu (12.5 or 6.7 %, respectively). Therefore, a significant number of adsorption sites had a high affinity for Cu. However, unlike the other two metals, even in presence of twice or triple concentrations of Cu than those of Pb and Cr (Pb, Cr, and Cu added amounts of 20, 20, and 40 or 20, 20, and 60 mmol kg<sup>-1</sup>), the

biochar adsorption sites were mostly occupied by Pb and Cr than Cu (Table 6).

## Discussion

### FT-IR characterization of biochar

The used biochar has been obtained through pyrolysis at 500 °C (see [Materials and methods](#)). According to Cimò et al. (2014), pyrolysis at the aforementioned temperature

**Table 4** Competitive adsorption of Pb and Cu on biochar at pH 4.5 and 20 °C, after 5 h of incubation

Added amounts (mmol kg <sup>-1</sup> )		Adsorbed amounts (mmol kg <sup>-1</sup> )		Initial ratio ( $R_i$ ) <sup>a</sup>	Final ratio ( $R_f$ ) <sup>b</sup>	Adsorption inhibition (%) <sup>c</sup>	
Pb	Cu	Pb	Cu	Pb/Cu		Pb	Cu
20	20	19±1	10.6±0.4	1.00	1.80	4.1	42.6
20	40	18±1	13.9±0.7	0.50	1.29	9.0	56.5
20	60	17.1±0.8	14.2±0.6	0.33	1.20	13.4	65.1
40	20	36±2	9.1±0.5	2.00	3.96	8.5	50.5
40	40	35±2	12.5±0.5	1.00	2.79	11.8	61.0
40	60	32±1	13±0.6	0.67	2.49	17.8	68.2
60	20	52±3	7.7±0.3	3.00	6.66	12.4	57.9
60	40	49±3	10.2±0.5	1.50	4.82	16.0	68.0
60	60	47±3	10.8±0.5	1.00	4.32	20.6	73.5

Adsorbed amounts of Pb and Cu are the average of at least three different replicates ( $n=3$ )

<sup>a</sup>  $R_i$  stands for the Pb/Cu molar ratio initially added on biochar samples

<sup>b</sup>  $R_f$  indicates the Pb/Cu molar ratio finally adsorbed on biochar surface

<sup>c</sup> Inhibition (%) of Pb or Cu adsorption was calculated by subtracting the amount of Pb or Cu adsorbed in presence of the other metal from that adsorbed in the absence of the other metal, divided by the amount adsorbed in the absence of the other metal, multiplied per 100

**Table 5** Competitive adsorption of Cr and Cu on biochar at pH 4.5 and 20 °C, after 5 h of incubation

Added amounts (mmol kg <sup>-1</sup> )		Adsorbed amounts (mmol kg <sup>-1</sup> )		Initial ratio ( $R_i$ ) <sup>a</sup>	Final ratio ( $R_f$ ) <sup>b</sup>	Adsorption inhibition (%) <sup>c</sup>	
Cr	Cu	Cr	Cu	Cr/Cu		Cr	Cu
20	20	17.2±0.7	11.8±0.6	1.00	1.46	6.4	35.8
20	40	16.5±0.9	16.5±0.8	0.50	1.00	10.2	48.4
20	60	15±1	17.4±1.0	0.33	0.86	18.6	57.4
40	20	33±2	10.8±0.5	2.00	3.07	9.0	41.2
40	40	32±2	15.4±0.6	1.00	2.09	11.7	51.9
40	60	29±1	16.6±0.8	0.67	1.75	20.1	59.3
60	20	49±2	9.4±0.5	3.00	5.14	10.0	48.6
60	40	45±2	12±0.6	1.50	3.64	17.2	61.6
60	60	40±2	12.9±0.8	1.00	3.13	25.5	68.5

Adsorbed amounts of Cr and Cu are the average of at least three different replicates ( $n=3$ )

<sup>a</sup>  $R_i$  stands for the Cr/Cu molar ratio initially added on biochar samples

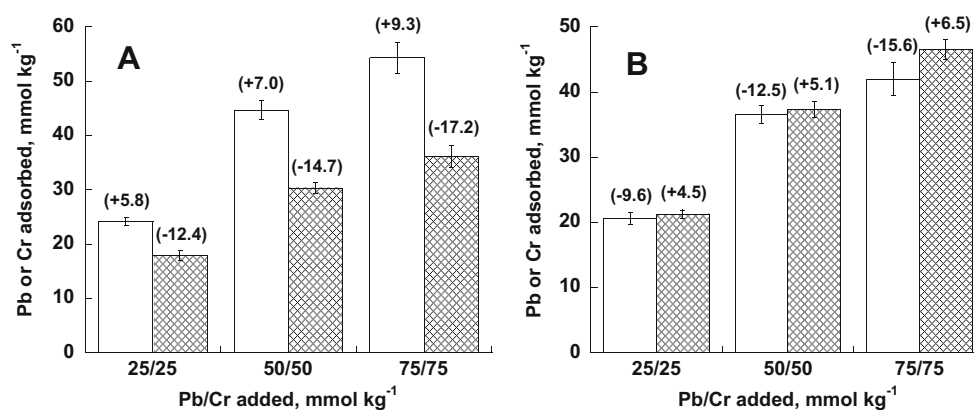
<sup>b</sup>  $R_f$  indicates the Cr/Cu molar ratio finally adsorbed on biochar surface

<sup>c</sup> Inhibition (%) of Cr or Cu adsorption was calculated by subtracting the amount of Cr or Cu adsorbed in presence of the other metal from that adsorbed in the absence of the other metal, divided by the amount adsorbed in the absence of the other metal, multiplied per 100

produces a biochar with a small amount of alkyl components and a main aromatic moiety. However, the FT-IR spectrum of our biochar shows that the pore surface contains some polar molecular groups (Table 1). In fact, the bands at 3,546, 3,470, 3,413, and 1,637 cm<sup>-1</sup> are due to the presence of unsubstituted (3,546 cm<sup>-1</sup>), mono-substituted (3,470 cm<sup>-1</sup>) and disubstituted (1,637 cm<sup>-1</sup>) amides, and to NH stretching of amine groups (3413 cm<sup>-1</sup>). Presence of oxygenated functions has been also observed. The O-containing groups produced bands at 1,617 and 1,400 cm<sup>-1</sup>, due to unprotonated carboxyls, and at 1,126 cm<sup>-1</sup>, due to oxygenated C (C–O). As already reported by Conte et al. (2014), polar groups may affect water dynamics on the surface of biochar due to formation of both conventional and non-conventional hydrogen bonds (see below).

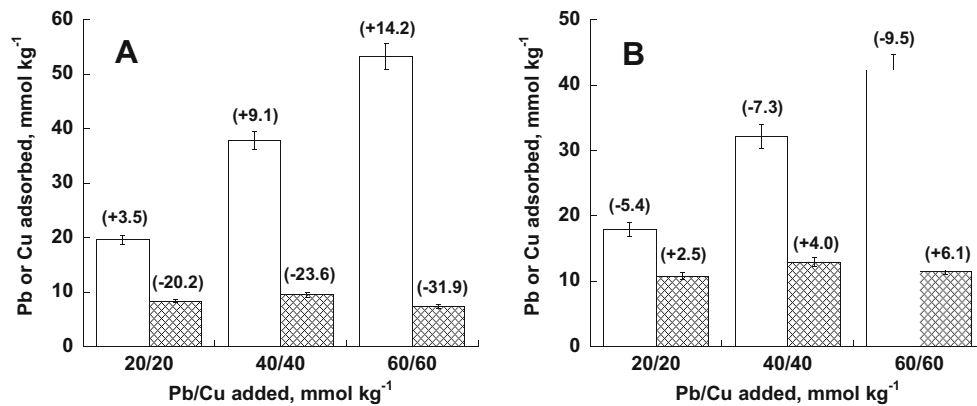
### <sup>1</sup>H NMR relaxometry

Figure 1 reports the relaxogram of the biochar sample resolved in three components according to  $T_1$  values of 86, 227, and 316 ms, respectively, which represent the shorter, the intermediate, and the longest  $T_1$  values, respectively. As previously reported (Conte et al. 2014), the fastest  $T_1$  value (at 86 ms) can be attributed to water molecules located in residual pores (<0.5 μm), the intermediate  $T_1$  value (at 227 ms) to water molecules moving in storage pores (0.5–50 μm), and the longest  $T_1$  value (at 316 ms) to water moving rapidly within the transmission pores (≥50 μm). As Cu, Cr, and Pb (either sole or in combination) are adsorbed on the surface of the biochar, a change in the distribution of relaxation times is



**Fig. 6** Effect of residence time on Pb (white bars) and Cr (grid bars) adsorption on biochar. In **a**, Pb was added 1 h before Cr on biochar, then the metal mixture was incubated with biochar for 5 h at pH 4.5 and 20 °C, while the opposite was done in **b**. The bars are the average of at least three

different replicates ( $n=3$ ). Values in brackets are the percent change of Pb and Cr adsorption on biochar vs. the adsorbed amounts of two metals by a simultaneous addition (as shown in Table 3)



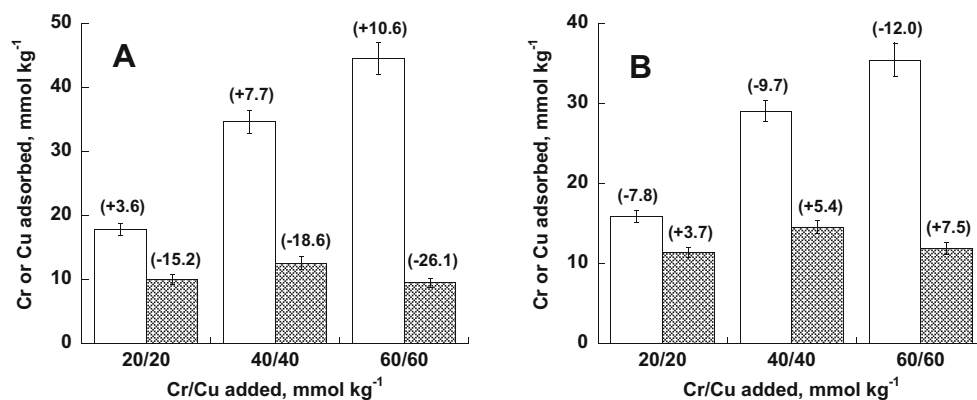
**Fig. 7** Effect of residence time on Pb (white bars) and Cu (grid bars) adsorption on biochar. In **a**, Pb was added 1 h before Cu on biochar, then the metal mixture was incubated with biochar for 5 h at pH 4.5 and 20 °C, while the opposite was done in **b**. The bars are the average of at least three

different replicates ( $n=3$ ). Values in brackets are the percent change of Pb and Cu adsorption on biochar vs. the adsorbed amounts of two metals by a simultaneous addition (as shown in Table 4)

observed. After Cu adsorption, the main relaxometry band is centered at a  $T_1$  value of 52 ms, which is shorter than that observed for the sole biochar (i.e., 238 ms) (Fig. 2a). Reduction of  $T_1$  is due to Cu paramagnetism. In fact, paramagnetism fastens nuclear relaxation with currents generated by unpaired electrons. However, as for the sole biochar, the deconvolution of the relaxogram in Fig. 2a revealed three type of water movements, occurring in residual ( $T_1=22$  ms), storage ( $T_1=43$  ms), and transmission ( $T_1=59$  ms) pores, respectively. Conceivably, the similarity among the number of relaxometry components in Figs. 1 and 2a indicates that Cu was homogeneously distributed within the three kinds of pores on the biochar surface. In the case of Cr application, the relaxograms showed two  $T_1$  values (Fig. 2b). The shortest  $T_1$  value (25 ms) can be attributed to Cr ions adsorbed into the residual pores. Conversely, most of the Cr ions were present into storage and transmission pores, thereby shrinking two water movement components into only one centered at  $T_1$  value of 60 ms. In the case of Pb application (Fig. 2c), only

a  $T_1$  value of 71 ms was observed, probably due to a homogeneous distribution of Pb into all the three kinds of pores. In particular, water movement resulted unaffected by pore size distribution, but it was only affected by the homogeneous Pb layer covering the whole biochar surface.

In the case of application of two metals (i.e., Cu + Cr, Cr + Pb, and Cu + Pb), relaxogram shapes differed from those previously discussed. The application of Cu and Cr gave a major water movement component centered at around 60 ms together with two small bands at 19 and 198 ms, respectively (Fig. 3a). This can be attributed to water moving into residual ( $T_1=19$  ms), storage ( $T_1=60$  ms), and transmission ( $T_1=198$  ms) pores. Since the major component at 60 ms was also shown by using Cr alone, probably the effect of Cr adsorption predominated over that of Cu adsorption on biochar surface. As Cr was combined with Pb, the relaxogram (Fig. 3b) showed three components again due to water moving in residual ( $T_1=16$  ms), storage ( $T_1=50$  ms), and transmission ( $T_1=79$  ms) pores. This indicates that probably there was no



**Fig. 8** Effect of residence time on Cr (white bars) and Cu (grid bars) adsorption on biochar. In **a** Cr was added 1 h before Cu on biochar, then the metal mixture was incubated with biochar for 5 h at pH 4.5 and 20 °C, while the opposite was done in **b**. The bars are the average of at least three

different replicates ( $n=3$ ). Values in brackets are the percent change of Cr and Cu adsorption on biochar vs. the adsorbed amounts of two metals by a simultaneous addition (as shown in Table 5)

**Table 6** Competitive adsorption of Pb, Cr, and Cu on biochar at pH 4.5 and 20 °C, after 5 h of incubation

Added amounts (mmol kg <sup>-1</sup> )			Adsorbed amounts (mmol kg <sup>-1</sup> )			Partition of adsorbing surface (%) <sup>a</sup>			Adsorption inhibition (%) <sup>b</sup>		
Pb	Cr	Cu	Pb	Cr	Cu	Pb	Cr	Cu	Pb	Cr	Cu
20	20	20	15.5±0.9	13.0±0.9	8.1±0.5	42.3	35.5	22.2	21.9	29.4	55.9
40	40	40	25±1	20±1	9.5±0.5	46.1	36.5	17.4	36.4	45.4	70.4
60	60	60	30±1	22±1	4.3±0.3	53.6	38.6	7.8	49.8	60.6	89.4
40	20	20	29±1	11.1±0.8	5.6±0.3	63.0	24.5	12.5	27.5	39.8	69.3
60	20	20	36±2	9.0±0.6	3.2±0.2	74.6	18.7	6.7	39.0	50.9	82.5
20	40	20	14.6±0.8	22±1	7.0±0.4	33.5	50.5	16.0	26.2	39.4	62.1
20	60	20	12.7±0.7	26±1	4.7±0.3	29.4	59.7	10.9	35.7	52.0	74.4
20	20	40	15.1±0.8	12.2±0.6	10.6±0.6	39.8	32.2	28.0	23.7	33.6	66.8
20	20	60	14.4±0.7	10.9±0.6	10.1±0.6	40.6	30.9	28.5	27.5	40.8	75.3

Adsorbed amounts of Pb, Cr and Cu are the average of at least three different replicates ( $n=3$ )

<sup>a</sup> Partition of adsorbing surface by Pb, Cr, or Cu was calculated by subtracting the adsorbed amount of Pb, Cr, or Cu from the total amount of three metals adsorbed by biochar (Pb+Cr+Cu), divided by the total amount of three metals adsorbed by biochar (Pb+Cr+Cu), multiplied per 100

<sup>b</sup> Inhibition (%) of Pb, Cr, or Cu adsorption was calculated by subtracting the amount of Pb, Cr, or Cu adsorbed in presence of the other two metals from that adsorbed in the absence of the other two metals, divided by the amount adsorbed in the absence of the other two metals, multiplied per 100

competition between Pb and Cr for adsorption on biochar sites. In the case of Cu and Pb application, a very broad and intense component was observed at 51 ms together with a negligible component at 21 ms (Fig. 3c). The predominant band at 51 ms indicates that Pb was preferentially adsorbed on the biochar surface. However, the fact that this value was shorter than that reported in Fig. 2c indicates that also paramagnetic Cu contributes to water relaxation. The <sup>1</sup>H NMR relaxogram obtained by experiments done on the biochar treated with three metals only showed one band placed at 38 ms (Fig. 4). Our hypothesis is that Pb was predominantly adsorbed on biochar surface, with a paramagnetic effect due to Cu which shifts the band to the very short  $T_1$  value.

#### Adsorption properties of biochar

The shape of Pb and Cr adsorption isotherms indicated a high affinity behavior (H-type), while the Cu isotherm revealed a lower affinity for biochar surface (L-type) (Fig. 5). The Langmuir  $K$  values obtained from three isotherms (Table 2) also confirmed the high affinity of Pb and Cr for biochar adsorption sites (Pb > Cr), followed by Cu. Greater  $K$  values, in fact, indicate higher affinity of the adsorbent for solutes (Sparks 2002). However, in spite of the significant difference in the binding energies ( $K$  values), the maximum Pb and Cr adsorption capacities ( $S_m$ ) were quite similar (108.2 and 98.3 mmol kg<sup>-1</sup>, respectively), much higher than that obtained from Cu isotherm (46.5 mmol kg<sup>-1</sup>) (Table 2). The higher adsorption of Pb than Cr and Cu by biochar may be due to the stronger surface electrostatic attraction, since the electronegativity constant of Pb is quite high (2.33) and this is responsible for specific Pb adsorption (Inyang et al. 2012). However, the

electronegativity constants of Cr and Cu are 1.90 and 1.66, respectively, and these values do not explain the heavy metal removal trend (Pb > Cr >> Cu) observed using this biochar as an adsorbent. Chromium has a higher charge density than Cu; hence, the coulombic attraction toward the superficial sites of the adsorbent is higher (Shi et al. 2009). However, in addition to the surface electrostatic interaction, other mechanisms (e.g., surface complexation) can be involved in the ion adsorption (Uchimiya et al. 2011; Inyang et al. 2012). Indeed, the quantity of the adsorbed ions on the adsorbing surface is also strongly affected by other factors, such as the ionic potential, radius of the hydrated ion, and hydrolysis constant (Shi et al. 2009; Zhu et al. 2010). The higher sorption of Cr than Cu by our biochar may be also due to the higher first hydrolysis constant of Cr ( $10^{-4}$ ) than Cu ( $10^{-8}$ ). The acidic conditions (pH 4.5) of our experiments may have played an important role on the metal adsorption. For instance, Cr adsorption by seven sludge-derived biochars was pH-dependent at pH values of 2.0–5.0, with a maximum adsorption at pH 2.0 (Zhang et al. 2013). The pH-dependent Cr adsorption on biochar was also shown by others (Demirbas et al. 2004; Dong et al. 2011; Mohan et al. 2011). Zhang et al. (2013) also noted that the highest Pb adsorption on seven biochars occurred at pH 5.0, a value similar to that of our experiments (i.e., 4.5); moreover, these authors showed that Pb adsorption was stronger than that of Cr, by comparing the shape of the adsorption isotherms of Pb (at pH 5.0) and Cr (at pH 2.0). A previous study (Xu et al. 2013) revealed that Cu removal by dairy manure-derived biochar from aqueous solutions was mainly attributed to the formation of Cu phosphate and Cu carbonate precipitates. The release of anions as phosphate and carbonate from biochar, able to precipitate heavy metals, can

cause additional metal disappearance from the solute (Uchimiya et al. 2010). However, since Cu adsorption on our biochar occurred at pH 4.5, we assume that Cu precipitation, due to release of phosphate and carbonate ions from biochar, was probably negligible; this hypothesis can, at least in part, explain the low Cu removal by biochar from solutions. A much higher removal of Pb than Cu by biochar was observed with digested dairy waste biochar, digested whole sugar beet biochar (Inyang et al. 2012), and poultry litter-derived biochar (Uchimiya et al. 2010) used as adsorbents. The competitive adsorption of Pb, Cr, and Cu on biochar was mainly influenced by the affinity of metals for biochar surface. The higher the affinity, the higher the ability of the metal to occupy adsorption sites. The slight increase of the final Pb/Cr molar ratio ( $R_f$ ) in comparison with the initial molar ratio ( $R_i$ ) revealed that Pb was able to prevent more efficiently the Cr adsorption on biochar than Cr in preventing Pb adsorption. A significantly higher increase of  $R_f$  vs.  $R_i$  was obtained in the Cr–Cu binary system (Table 5) and, even more, in the Pb–Cu binary system (Table 4), where  $R_f$  resulted to be up to threefold (in the former case) and fourfold (in the latter case) higher than  $R_i$ , because of the much higher affinity of Pb and Cr than Cu for biochar adsorption sites. Our findings agree with those by Chen et al. (2011), who found that Cu inhibited Zn removal by hardwood-derived and corn-straw-derived biochars, because of the higher affinity of the former than the latter metal for adsorption sites of two adsorbents. We have also found that an increase in residence time of each metal on the biochar surface increased the adsorption of the metal if compared to that observed by the simultaneous addition with another metal, probably because of the better diffusion inside the adsorbent structure and formation of stronger bonds between metal and biochar adsorption sites during the pre-equilibration phase. A similar trend was found by Zhu et al. (2010), in a competitive study of Pb, Cr, and Cu adsorption on ferrihydrite and two organomineral complexes.

## Conclusions

This study provided important information regarding the potential use of biochar as adsorbent of heavy metals, such as Pb, Cr, and Cu, from aqueous mono- and multi-contaminated environments. Biomass-derived biochar combines an effective removal of water contaminants with low costs of remediation. The water movement on the biochar pores was affected by metal adsorption, as shown by FFC NMR relaxometry, which is a novel and promising technique to identify the nature of biochar-metal bonds at the solid-liquid interface. However, more studies are needed to demonstrate the feasibility of biochar as adsorbent for an effective and safe removal of heavy metals from contaminated waters in situ.

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