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Ultrafast photodegradation of isoxazole and isothiazolinones by UV254 and UV254/H₂O₂ photolysis in a microcapillary reactor

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1 Ultrafast photodegradation of isoxazole and isothiazolinones by

2 UV₂₅₄ and UV₂₅₄/H₂O₂ photolysis in a microcapillary reactor

3
4 Danilo Russo^{a,d*}, Kristin H. Cochran^b, Danielle Westerman^b, Gianluca Li Puma^c, Raffaele
5 Marotta^d, Roberto Andreozzi^d, Susan D. Richardson^{b,*}.

6
7 ^a Present address: Department of Chemical Engineering and Biotechnology, University of
8 Cambridge, UK.

9 ^b Department of Chemistry and Biochemistry, University of South Carolina, USA.

10 ^c Environmental Nanocatalysis & Photoreaction Engineering, Department of Chemical
11 Engineering, Loughborough University, UK.

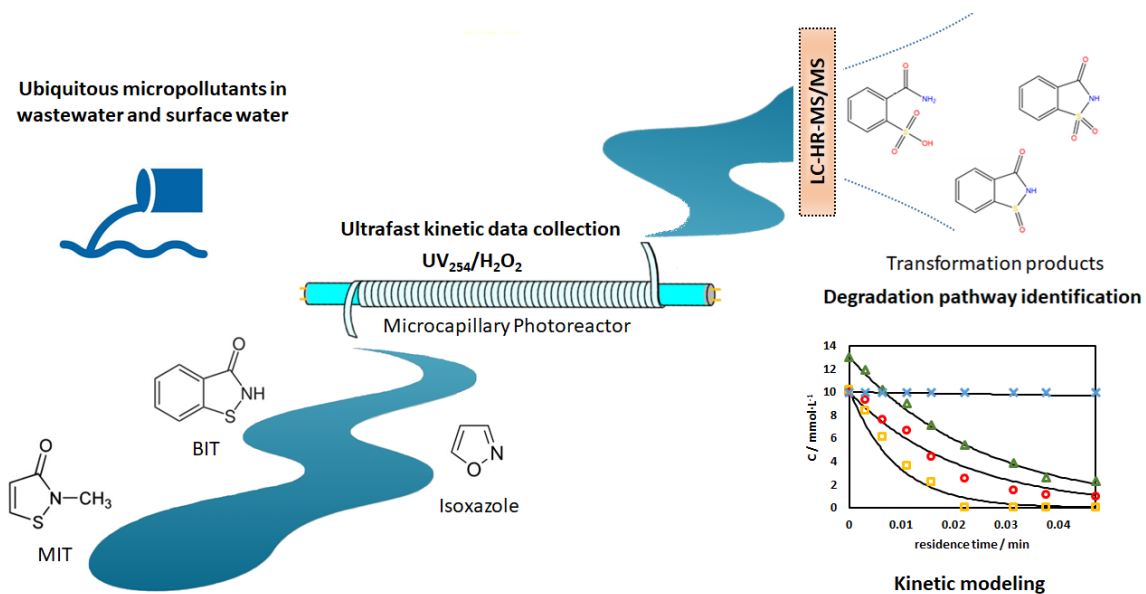
12 ^d Dipartimento di Ingegneria Chimica, dei Materiali e della Produzione Industriale,
13 Università di Napoli Federico II, Italy.

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15 *Corresponding author: Danilo Russo: danilo.russo3@unina.it; dr473@cam.ac.uk; Susan D.
16 Richardson, RICHA545@mailbox.sc.edu.

17
18 Keywords: micropollutants; advanced oxidation processes; isoxazole; water reclamation;
19 water treatment; isothiazolinones.

20 *Highlights*

- 21 • H₂O₂/UV₂₅₄ and UV₂₅₄ for the removal of isothiazolinones and isoxazole
- 22 • A convenient ultrafast microcapillary photoreactor was adopted for AOP studies
- 23 • Photokinetic parameters of target isothiazolinones and isoxazole were estimated
- 24 • The main oxidized BIT transformation products were tentatively identified
- 25 • A novel mechanistic degradation pathway was proposed for BIT



26

27

28 Abstract

29 The photodegradation process of methylisothiazolinone (MIT), benzisothiazolinone (BIT), and
 30 isoxazole (ISOX) in ultrapure water and synthetic wastewater by means of UV₂₅₄ photolysis
 31 and by UV₂₅₄/H₂O₂ advanced oxidation process were investigated in a microcapillary
 32 photoreactor designed for ultrafast photochemical transformation of microcontaminants. For
 33 the first time, we estimated key photo-kinetic parameters, i.e. quantum yields ($35.4 \text{ mmol}\cdot\text{ein}^{-1}$
 34 1 for MIT, and 13.5 and $55.8 \text{ mmol}\cdot\text{ein}^{-1}$ for BIT at pH = 4-6 and 8, respectively) and rate
 35 constants of the reaction of photo-generated OH radicals with MIT and BIT ($2.09\cdot 10^9$ and
 36 $5.9\cdot 10^9 \text{ L}\cdot\text{mol}^{-1}\cdot\text{s}^{-1}$ for MIT and BIT). The rate constants of the reaction of photo-generated
 37 OH radicals with ISOX in MilliQ water was also estimated $2.15\cdot 10^9 \text{ L}\cdot\text{mol}^{-1}\cdot\text{s}^{-1}$) and it was in
 38 good agreement with literature indications obtained in different aqueous matrices. The models
 39 were extended and validated to the case of simultaneous degradation of mixtures of these
 40 compounds and using synthetic wastewater as an aqueous matrix. High resolution-accurate
 41 mass mass spectrometry analysis enabled identification of the main intermediates (BIT200,
 42 B200, saccharin, BIT166) and enabled proposal of a novel degradation pathway for BIT under
 43 UV₂₅₄/H₂O₂ treatment. This study demonstrates an ultrafast method to determine key photo-

44 kinetic parameters of contaminants of emerging concern in water and wastewater, which are
45 needed for design and validation of photochemical water treatment processes of municipal and
46 industrial wastewaters.

47

48 **1. Introduction**

49 Isoxazole and isothiazolinones are five-membered heterocyclic compounds having various
50 pharmacological and antimicrobial properties (Hamada et al., 2011; Lee et al., 2002; Clerici et
51 al., 2008). The large interest in these substances and their derivatives is due to their versatility
52 as synthetic building blocks (Gribble et al., 2003). As a result of their massive adoption in a
53 wide variety of commonly used products, such compounds have been included in the class of
54 emerging pollutants (Ghattas et al., 2017; Shi et al., 2012). The current broad definition of
55 emerging pollutants includes a significant number of chemicals normally employed in
56 detergents, personal care products, pharmaceuticals and drugs, which are usually present in
57 wastewater and surface water at levels from ng to μg per liter (Miraji et al., 2016; Wanda et al.,
58 2017; McCance et al., 2018; Guo et al., 2018). Despite their low levels, their potential
59 ecotoxicological effect cannot be ruled out (Kohanski et al., 2010; Lin et al., 2010) and several
60 studies addressed the problem of their removal from liquid and solid compartments (Stamm et
61 al., 2015; Bollmann et al., 2017; Luo et al., 2014, Margot et al., 2015).

62 2-Methyl-1,2-thiazol-3(2H)-one, also named methylisothiazolinone (MIT), and 1,2-
63 Benzisothiazol-3(2H)-one, or benzisothiazolinone (BIT), are very common biocides employed
64 in personal care products, detergents (Li et al., 2016a; Garcia-Hidalgo et al., 2016), roof and
65 outdoor paints, paper materials, and in other important industrial applications (Jungnickel et
66 al., 2008; Wieck et al., 2016, Wang et al., 2017; Li et al., 2016b), i.e. in reverse osmosis
67 processes for water reclamation and desalination (Li et al., 2016a) and, in high concentrations,
68 in cooling towers, paper mills, and refinery industry (Amat et al., 2015). As a result, significant

69 concentrations of MIT and BIT have been reported in wastewater treatment plants' (WWTPs')
70 influent, effluent, and in surface water (Wieck et al., 2016; Speksnijder et al., 2010; Zhang et
71 al., 2015; Liu et al., 2015). The potential impact of MIT and BIT to the aquatic environment
72 and humans is addressed by several studies (Li et al., 2016a; Van Huizen et al., 2017; Li et al.,
73 2016b; Lugg, 2001; Geier et al., 2012). MIT was named allergen of the year IN 2013 (Van
74 Huizen et al., 2017). The biocidal effect of MIT also affects the efficiency of activated sludge
75 in wastewater treatment and as a result, the efficiency of the nitrification process can decrease
76 from 90 to 20 % (Amat et al., 2015).

77 Previous studies show slow degradation of MIT by divalent ferric ions (Tanji et al., 2007),
78 TiO₂, and ZnO based photocatalysis under UV irradiation (Kandavelu et al., 2004), and by
79 electrochemical methods (Han et al., 2011). Ozonation was found to be effective in the
80 degradation of first- and second- generation by-products of both MIT and BIT and in the
81 reduction of treated sample ecotoxicity for longer treatment times (Li et al., 2016a, Li et al.,
82 2016b), whereas studies on BIT degradation in water under UV-C irradiation were recently
83 conducted by Wang et al., (2017).

84 Isoxazole (ISOX) derivatives are commonly used in different pharmaceuticals as antifungal
85 (Vicentini et al., 2011), anticancer (Yong et al., 2015), anti-HIV (Srivastava et al., 1999), and
86 ulcerogenic (Daidone et al., 1999) agents. Some isoxazole derivatives have antibiotic activity;
87 a typical case is sulfamethoxazole, an antibiotic used worldwide, and prescribed for treatment
88 of urinary infections.

89 Isoxazole-based compounds are also employed as COX-2 inhibitors and anti-inflammatory
90 drugs (Zimecki et al., 2018; Maczynski et al., 2016). Some isoxazole derivatives were detected
91 in different sewage treatment plant effluents, surface waters and drinking waters at low ng·L⁻¹
92 levels (Schriks et al., 2010; Andreozzi et al., 2003; Hirsch et al., 1999).

93 Advanced oxidation processes (AOPs) have been widely adopted for the successful
94 degradation of a wide range of emerging pollutants. Specifically, UV/H₂O₂ offers several
95 advantages, including easy operation, reduced costs and high removal efficiency for both
96 parent compounds and their transformation products (Bensalah et al., 2018; Huang et al., 2018;
97 Li et al., 2007), resulting also in a decrease of the ecotoxicological effects of processed
98 solutions for well-designed treatment times (Siciliano et al., 2018).

99 In this study, the degradation of MIT, BIT, and isoxazole (Fig. 1) was studied under UV_{254nm}
100 and UV_{254nm}/H₂O₂ in ultrapure MilliQ water in order to estimate the main kinetic parameters,
101 such as direct photolysis quantum yields and the rate constants of the reaction of photo-
102 generated OH radicals and these emerging pollutants.

103

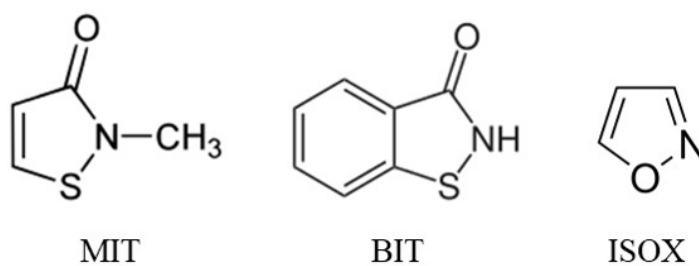


Fig. 1. Structural formulas for MIT, BIT, and ISOX.

107

108 Kinetic experiments were carried out in MilliQ and synthetic wastewater using a microcapillary
109 photo-reactor (Reis and Li Puma, 2015) and were kinetically modelled using previous
110 approaches (Russo et al., 2017). The adoption of this microreactor enabled collection of several
111 experimental samples in a simple, safe, and fast experimental campaign, reducing reaction
112 times, waste solution volumes, and costs associated with the adoption of batch-scale quartz and
glass reactors, high power lamps, waste disposal, and expensive reagents.

113 In addition to kinetic experiments, treated and untreated solutions were analyzed via high
114 resolution-accurate mass mass spectrometry to identify the primary oxidation/degradation
115 products of the three contaminants of interest (MIT, BIT, and ISOX).

116 A novel mechanistic pathway was proposed for BIT utilizing one of two common addition
117 mechanisms known in sulfur chemistry (Atkinson et al., 1997, Barnes et al., 1996, Wine et al.,
118 1981, Hynes and Wine et al., 1995). Oxidation of sulfur-containing compounds often adds
119 oxygen to the sulfur heteroatom, which can somewhat uniquely contain 2, 4, or 6 bonds,
120 through either (i) hydrogen abstraction or (ii) radical addition (Atkinson et al., 1997, Wine et
121 al., 1981; Barnes et al., 1996). Hydrogen abstraction commonly happens when the sulfur
122 heteroatom is adjacent to a methyl or C-H-containing group, where the hydroxyl radical pulls
123 a hydrogen off to form water and an analyte radical; as BIT's sulfur is adjacent to an amide
124 group, this mechanism is unlikely for BIT advanced oxidation (Atkinson et al., 1997; Barnes
125 et al., 1996). The more likely mechanism is radical addition through direct attack of the
126 hydroxyl radical on the sulfur heteroatom and further oxidation by oxygen (O₂) present in the
127 reactor water (Hynes et al., ; Wine et al., 1981). Hydroxyl radicals (*OH) are generated from
128 ultraviolet (UV) treatment of hydrogen peroxide (H₂O₂) and subsequently react with the
129 analyte (Atkinson et al., 1997).

130 To the best of our knowledge, this is the first study investigating the photodegradation of the
131 target compounds by UV₂₅₄ and UV₂₅₄/H₂O₂ processes by ultrafast sample generation, laying
132 the groundwork for future investigations on the removal efficiency in real wastewater matrices
133 and ecotoxicity studies of the treated and untreated compounds on aquatic life. This is also the
134 first UV/H₂O₂ advanced oxidation degradation pathway proposed for BIT.

135

136 **2. Materials and Methods**

137 **2.1. Materials**

138 2-Methyl-4-isothiazolin-3-one (98%), 1,2-benzisothiazol-3(2H)-one (98%), isoxazone (99%),
139 sulfuric acid (1 N), NaOH (97%), NaCl (99.5%), CaCl₂ (99%), meat extract, peptone
140 microbiology grade, urea (98%), K₂HPO₄ (98%), MgSO₄ (99%), hydrogen peroxide solution
141 (35%), benzoic acid (99.5%), methanol (99.99%), and acetonitrile (99.99%) were purchased
142 from Sigma-Aldrich.

143 Synthetic wastewater was prepared by adding peptone (32 mg·L⁻¹), meat extract (22 mg·L⁻¹),
144 urea (6 mg·L⁻¹), K₂HPO₄ (28 mg·L⁻¹), CaCl₂ (4 mg·L⁻¹), NaCl (7 mg·L⁻¹), MgSO₄ (0.6 mg·L⁻¹)
145 to MilliQ water in accordance with OECD guidelines (Organisation for Economic
146 Cooperation and Development, 1999) and stored at 4 °C for less than 24 h. pH was adjusted
147 using diluted solutions of sulfuric acid and sodium hydroxide. No significant pH variations
148 were detected during the experiments.

149

150 **2.2. Continuous flow experiments**

151 The experimental setup has been described in detail elsewhere (Reis and Li Puma, 2015; Russo
152 et al., 2016). Briefly, it consists of a fluoropolymer flat strip containing 10 microcapillaries
153 with a mean diameter of 195 μm, wrapped around a monochromatic (254 nm) germicidal lamp
154 (Germicidal G8T5). The nominal power supplied to the lamp could be varied from 8 W to 4.5
155 W using a variable power supplier. The photonic power per unit reactor volume $\left(\frac{I_{254}}{V}\right)$ emitted
156 were estimated by hydrogen peroxide actinometry (Nicole et al., 1990) and were $1.92 \cdot 10^{-2}$
157 $\text{ein} \cdot \text{s}^{-1} \cdot \text{L}^{-1}$ and $1.27 \cdot 10^{-2} \text{ ein} \cdot \text{s}^{-1} \cdot \text{L}^{-1}$, respectively (Russo et al., 2017). The adopted flow rates
158 through the microcapillary photoreactor were in the range $0.6 - 1 \text{ mL} \cdot \text{min}^{-1}$. The fluid residence
159 time (i.e. space time) was varied changing both the flowrate and the length of the reactor
160 exposed to the UV₂₅₄ radiation. Previously reported tracer experiments showed a fluid-dynamic
161 behaviour approaching plug-flow. In a typical experiment, the reactor was washed with MilliQ
162 water. The lamp was turned on for the same amount of time to reach stationary conditions

163 before adding the MIT, BIT, or ISOX to the feed tank. Samples were collected directly into
164 vials at the outlet of the reactor and analyzed using a spectrophotometer and a high-
165 performance liquid chromatograph (HPLC). The reactor was always operated in single pass
166 without any recirculation of the solutions. Preliminary experiments showed that the solutions
167 were not reactive under dark conditions.

168

169 **2.3. Analytical methods**

170 Absorbance spectra at 254 nm were acquired using a PerkinElmer Lambda 35 UV/Vis
171 spectrometer.

172 Chromatographic analysis was carried out using an Agilent 1100 HPLC equipped with a Restek
173 Ultra C18 LC column (250 x 4.60 mm 5 μ m) and a DAD detector. The column was maintained
174 at 30 °C. The mobile phase consisted of 8% aqueous methanol, 18% aqueous acetonitrile, and
175 6% aqueous MeOH for MIT, BIT, and ISOX, respectively. Retention times were 2.3, 12.3, and
176 8.1 min, respectively.

177 Samples containing 10 parts per million ($\text{mg}\cdot\text{L}^{-1}$) of BIT, MIT, and ISOX reacted with
178 $\text{UV}_{254}/\text{H}_2\text{O}_2$ were loaded on solid phase extraction (SPE) cartridges and kept frozen until
179 analysis. SPE cartridges were eluted with 15 mL 50:50 methanol:acetone, evaporated to 500
180 μL under nitrogen, and a fraction (200 μL) was diluted with purified water and analyzed by
181 LC-mass spectrometry (MS)/MS for transformation product (TP) identification.

182 Transformation products (TPs) of BIT, MIT, and ISOX were analyzed by an Agilent 6545
183 ultra-high-performance liquid chromatograph (UHPLC) quadrupole-time-of-flight (QTOF)
184 mass spectrometer with a Poroshell C18 UHPLC column (2.1 mm \times 150 mm \times 2.7 μm , Agilent
185 InfinityLab). Electrospray ionization (ESI) was used in both positive and negative ion mode.
186 The LC mobile phase consisted of water and methanol, containing 0.1% formic acid and 5 mM
187 ammonium acetate, with a flow of 0.5 $\text{mL}\cdot\text{min}^{-1}$ and an injection volume of 10 μL . A gradient

188 elution was used: 70% water/30% methanol, held for one min, then ramped to 2% water/98%
189 methanol over 9 min, and returned to initial conditions over 2 min. The mass spectrometer was
190 operated at a fragmentation voltage of 110 V, capillary voltage of 4000 V, gas temperature of
191 300°C, drying gas of 12 L·min⁻¹, and nebulizer pressure of 35 psi. The scan range was from
192 m/z 50 to 750, and collision energy for MS/MS analyses was 30 eV.

193

194 **3. Results**

195 *3.1. Absorbance spectra*

196 Absorption spectra of the three investigated compounds are reported in Fig. 2 in the range 200-
197 400 nm at different pH. However, it is worth noting that at 254 nm, the molar extinction
198 coefficients of MIT at different pH are similar, whereas no significant absorbance of ISOX
199 solution could be detected. The estimated molar extinction coefficients of MIT and BIT are
200 summarized in Table 1.

201

202 **Table 1.** Molar absorption coefficients of MIT and BIT at 254 nm.

Compound	ϵ (pH 4-6) / L·mmol ⁻¹ ·cm ⁻¹	ϵ (pH 8) / L·mmol ⁻¹ ·cm ⁻¹
MIT	4.76	5.40
BIT	3.20	3.65

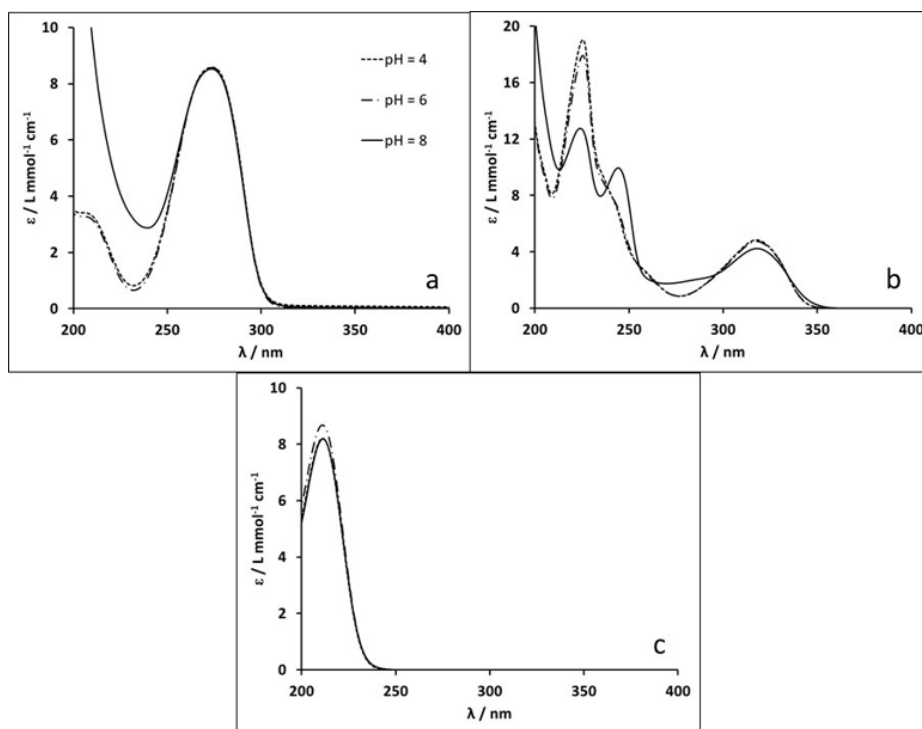


Fig. 2. Absorbance spectra for MIT (a), BIT (b), and ISOX (c) at different pH.

3.2. Direct photolysis in MilliQ water: estimation of quantum yields of direct photolysis

The quantum yields of MIT, BIT and ISOX under direct photolysis in MilliQ water was determined for the experimental conditions summarized in Table S1. The data were modeled according to the kinetic model previously reported (Russo et al., 2016; Russo et al., 2018). The kinetics of photodegradation of the compound $[S_i]$ occurs in accordance to the following modeling equation:

$$\frac{d[S_i]}{dt} = -\frac{I_{254}}{V} \cdot \Phi_{254}^{S_i} \cdot (1 - \exp(-2.3 \cdot l \cdot \epsilon_{254}^{S_i} \cdot [S_i])) \quad (1)$$

where $\frac{I_{254}}{V}$ is the estimated photonic power per unit reactor volume, $\Phi_{254}^{S_i}$ is the quantum yield of direct photolysis, $l = 152 \mu\text{m}$ is the mean optical length of the microcapillary photoreactor (Russo et al., 2016), and $\epsilon_{254}^{S_i}$ the molar absorption coefficient of the reacting species at 254 nm (Table 1). Eq. 1 was fitted to the results of the experiments reported in Table S1 and the quantum yield $\Phi_{254}^{S_i}$ of each reacting species was determined by minimizing the overall mean

217 square error between the experimental and the calculated data, using an optimization routine
 218 in Matlab software (optimization mode). Fig. 3 shows the prediction of the model and the
 219 experimental data for some of the adopted conditions. All the experiments used for the
 220 modelling were reported in the Supplementary Information (Fig. S1, Table S1). The quantum
 221 yield of direct photolysis for BIT was found to be pH dependent, in agreement with the fact
 222 that also the absorbance at 254 nm is a function of pH (Section 3.1). Specifically, BIT
 223 degradation was faster at pH 8. The estimated values were summarized in Table 2, together
 224 with their 97% intervals of confidence. As shown in Fig. 3.C, ISOX does not undergo direct
 225 photolysis at 254 nm since does not absorb at this wavelength (Fig.2). The adopted model is
 226 able to predict the degradation of MIT and BIT under direct photolysis and under different
 227 experimental conditions (initial concentration, pH and photon fluxes).

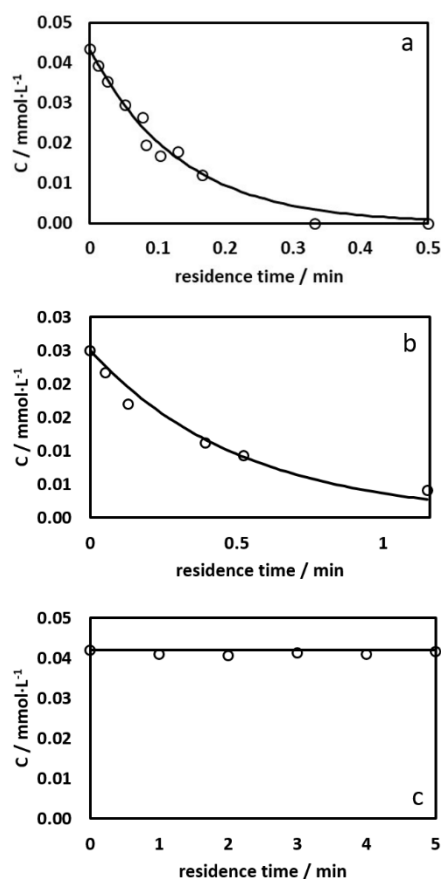
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229

Table 2. Estimated quantum yields.

Compound	$\Phi_{254}^{pH=4-6} (mmol \cdot ein^{-1})$	$\Phi_{254}^{pH=8} (mmol \cdot ein^{-1})$
MIT	35.42 ± 0.88	
BIT	13.45 ± 0.52	55.80 ± 1.33

230



231

232 Fig. 3. Direct photolysis of MIT (a), BIT (b), and ISOX (c) at pH = 6 and nominal P = 8.0 W.

233 Experimental data (O), calculated data (curves). a) $[\text{MIT}]_0 = 0.0434 \text{ mmol}\cdot\text{L}^{-1}$. b) $[\text{BIT}]_0 =$
 234 $0.0434 \text{ mmol}\cdot\text{L}^{-1}$. c) $[\text{ISOX}]_0 = 0.0420 \text{ mmol}\cdot\text{L}^{-1}$.

235

236 3.3. UV_{254}/H_2O_2 treatment in MilliQ water: k_{HO} estimation

237 The reaction of MIT, BIT, and ISOX under UV_{254} and in the presence of H_2O_2 in MilliQ water
 238 was further investigated to determine the second-order kinetic rate constant of reaction of the
 239 target compounds with photogenerated HO radicals (k_{HO}^i) generated by the photolysis of H_2O_2 .

240 The experimental data were modeled according to the modeling equations (2-5) and the k_{HO}^i
 241 was determined by minimizing the mean squared error between calculated and experimental
 242 data. A detailed derivation of eq. 2-5, together with the adopted simplifying assumptions can be
 243 found in (Spasiano et al., 2016a). Briefly, it was assumed that the parent compound and all

244 reaction products react with photogenerated HO radicals with the same kinetic rate constant
 245 k_{HO}^i and that the sum of their concentrations is always equal to the initial concentration of the
 246 target compound $[S_i]_0$.

$$\frac{d[H_2O_2]}{dt} = -F_{H_2O_2} - \frac{F_{H_2O_2} \cdot k_H \cdot [H_2O_2]}{k_{HO}^i [S_i]_0 + k_H [H_2O_2]} \quad (2)$$

$$\frac{d[S_i]}{dt} = -\frac{I_{254}}{V} \Phi_{254}^{S_i} (1 - \exp(-2.3 \cdot l \cdot A_{tot})) \frac{\epsilon_{254}^{S_i} \cdot [S_i]}{A_{tot}} - \frac{2k_{HO}^i [S_i] F_{H_2O_2}}{k_{HO}^i [S_i]_0 + k_H [H_2O_2]} \quad (3)$$

247 where

$$F_{H_2O_2} = \frac{I_{254}}{V} \Phi_{254}^{H_2O_2} (1 - \exp(-2.3 \cdot l \cdot A_{tot})) \cdot \frac{\epsilon_{254}^{H_2O_2} \cdot [H_2O_2]}{A_{tot}} \quad (4)$$

$$A_{tot} = \epsilon_{254}^{H_2O_2} \cdot [H_2O_2] + \epsilon_{254}^{S_i} \cdot [S_i] \quad (5)$$

248 where k_H ($2.7 \cdot 10^7 \text{ L} \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$) is the rate constant for the reaction between HO radicals and
 249 hydrogen peroxide, $\Phi_{254}^{H_2O_2}$ ($0.55 \text{ mol} \cdot \text{ein}^{-1}$) is the quantum yield for direct photolysis of
 250 hydrogen peroxide at 254 nm, and $\epsilon_{254}^{H_2O_2}$ ($18.6 \text{ L} \cdot \text{mol}^{-1} \cdot \text{cm}^{-1}$) is the molar absorption coefficient
 251 of hydrogen peroxide (Russo et al., 2016; Spasiano et al., 2016a). The adopted experimental
 252 conditions are summarized in Table S2. The comparisons between the experimental and
 253 calculated concentrations for hydrogen peroxide and the target compounds for all the adopted
 254 conditions are reported in Fig. 2S A-C whereas Fig. 4 shows the results only for a few
 255 explicative examples.

256 The best estimated values of k_{HO}^i together with their 97% confidence intervals are summarized
 257 in Table 3. The estimated value for ISOX is in good agreement with the one previously reported
 258 in the literature ($3.5 \cdot 10^9 \text{ L} \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$) (Dogan et al., 1990). The discrepancy can be ascribed to
 259 the interference of other compounds in the water matrix adopted in the previous study. It is
 260 worth noticing that ISOX and MIT have very similar rate constant. This can be explained
 261 considering that they have very similar structure and they might undergo H abstraction by OH

262 radicals as previously reported for ISOX (Dogan et al., 1990). On the other hand, the higher
263 value of the rate constant estimated for BIT is in good agreement with those reported for
264 heterocyclic aromatics, for which the aromatic ring hydroxylation is more likely to occur (Sagi
265 et al., 2015).

266 Competition kinetics with benzoic acid as a reference compound were also used to estimate the
267 value of k_{HO}^{ISOX} , since it is reported that this method gives a good estimate of the rate constant
268 when the organic compounds do not undergo direct photolysis or the latter is negligible
269 (Spasiano et al., 2016a). The estimated value of k_{HO}^{ISOX} was $3.0 \cdot 10^9 \text{ L} \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$, in good
270 agreement with the one reported in Table 3. The slight discrepancies between the two methods
271 have been already observed for other compounds (Spasiano et al., 2016a; Spasiano et al.,
272 2016b; Russo et al., 2017; Russo et al., 2018; Garcia Einschlag et al., 2003).

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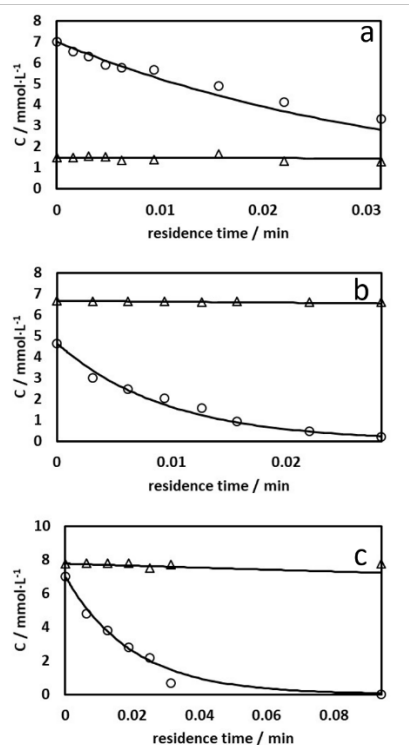
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275 **Table 3.** Estimated k_{HO}^i values for the investigated compounds.

Compound	$k_{HO}^i (\text{L} \cdot \text{mol}^{-1} \cdot \text{s}^{-1})$
MIT	$(2.09 \pm 0.21) \cdot 10^9$
BIT	$(5.90 \pm 0.69) \cdot 10^9$
ISOX	$(2.15 \pm 0.12) \cdot 10^9$

276

277



278

279 **Fig. 4.** Photodegradation of MIT (a), BIT (b), and ISOX (c) by UV_{254}/H_2O_2 in MilliQ water

280 at pH = 6 and nominal P = 8.0 W: experimental data (symbols), calculated data (lines).

281 organics (\circ), H_2O_2 (Δ). BIT concentrations are multiplied by 160 for viewing convenience. a)

282 $[MIT]_0 = 0.044 \text{ mmol}\cdot\text{L}^{-1}$; $[H_2O_2]_0 = 1.48 \text{ mmol}\cdot\text{L}^{-1}$. b) $[BIT]_0 = 0.029 \text{ mmol}\cdot\text{L}^{-1}$; $[H_2O_2]_0 =$

283 $6.68 \text{ mmol}\cdot\text{L}^{-1}$. c) $[MIT]_0 = 0.040 \text{ mmol}\cdot\text{L}^{-1}$; $[H_2O_2]_0 = 7.77 \text{ mmol}\cdot\text{L}^{-1}$.

284

285 3.4. UV_{254}/H_2O_2 treatment in synthetic wastewater

286 Most photodegradation treatment processes take place in real wastewater plants in which a

287 considerable number of other compounds are present. The effect of the water matrix on the

288 system can be complex (Lado Ribeiro et al., 2019) because compounds like nitrates can be an

289 additional source of hydroxyl radical (Mack and Bolton, 1999). However, most photo-

290 degradation kinetics can be successfully modeled, taking into account naturally occurring

291 compounds that act as scavengers for hydroxyl radicals, which decrease the degradation

292 efficiency for target compounds (Spasiano et al., 2016a). In this case, the modeling equations

293 (eq. 6-9) can be modified, taking into account the absorbance of the real aqueous matrix and
 294 introducing a scavenging term k_{sca} as follows:

$$\frac{d[H_2O_2]}{dt} = -F_{H_2O_2} - \frac{F_{H_2O_2} \cdot k_H \cdot [H_2O_2]}{k_{HO}^i [S_i]_0 + k_H [H_2O_2] + k_{sca}} \quad (6)$$

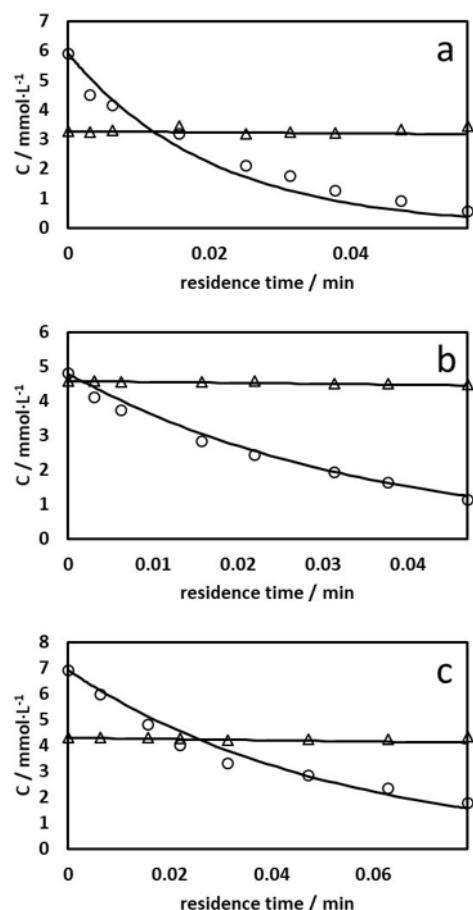
$$\frac{d[S_i]}{dt} = -\frac{I_{254}}{V} \Phi_{254}^{S_i} (1 - \exp(-2.3 \cdot l \cdot A_{tot})) \frac{\varepsilon_{254}^{S_i} \cdot [S_i]}{A_{tot}} - \frac{2k_{HO}^i [S_i] F_{H_2O_2}}{k_{HO}^i [S_i]_0 + k_H [H_2O_2] + k_{sca}} \quad (7)$$

295 where

$$F_{H_2O_2} = \frac{I_{254}}{V} \Phi_{254}^{H_2O_2} (1 - \exp(-2.3 \cdot l \cdot A_{tot})) \cdot \frac{\varepsilon_{254}^{H_2O_2} \cdot [H_2O_2]}{A_{tot}} \quad (8)$$

$$A_{tot} = \varepsilon_{254}^{H_2O_2} \cdot [H_2O_2] + \varepsilon_{254}^{S_i} \cdot [S_i] + A_{matrix} \quad (9)$$

296 and where A_{matrix} is the total absorbance at 254 nm of the synthetic aqueous matrix, which
 297 often may be considerably negligible with respect to the absorbance of hydrogen peroxide and
 298 the aromatic compounds. As reported by Spasiano et al., 2016a, $k_{sca} = k'[SCA]$, where k' is
 299 the kinetic rate constant of the reaction between OH radicals and the scavengers species (SCA).
 300 As a result, it can be considered as a constant for a selected aqueous matrix assuming that the
 301 concentration of the scavengers [SCA] is much greater than the one of the pollutants. To further
 302 support this point and validate previous models (Sections 3.2 and 3.3) and the kinetic
 303 parameters estimated in this work, kinetic experiments were carried out by dissolving the target
 304 compounds in synthetic wastewater prepared according to the OECD guidelines as specified
 305 in Section 2.1. Equations 6-9 were simultaneously solved for the chosen experimental
 306 conditions using the previously estimated value for the k_{sca} ($4.01 \cdot 10^5 \text{ s}^{-1}$) (Spasiano et al.,
 307 2016a; Russo et al., 2017) without any further adjustment of any of the previously estimated
 308 kinetic parameters (simulation mode). As shown in Fig. 5, the model is still capable of
 309 predicting degradation of the target compounds by UV_{254}/H_2O_2 in synthetic wastewaters.



311

312 **Fig. 5.** Degradation of (a) MIT; (b) BIT; (c) ISOX by UV/ H_2O_2 in synthetic wastewater.

313 Pollutant (\circ), H_2O_2 (Δ). Pollutant concentrations are multiplied by 160 for viewing

314 convenience. (a) $[S_i]_0 = 0.037$ mM, $[\text{H}_2\text{O}_2]_0 = 3.28$ mM, overall $\sigma(\%) = 2.16$; (b) $[S^i]_0 =$

315 0.030 mM, $[\text{H}_2\text{O}_2]_0 = 4.58$ mM, overall $\sigma(\%) = 0.85$; (c) $[S_i]_0 = 0.043$ mM, $[\text{H}_2\text{O}_2]_0 = 4.30$

316 mM, overall $\sigma(\%) = 2.45$; pH=6.0; P = 8 W.

317 3.5. Mixture of MIT, BIT, and ISOX in MilliQ water

318 Mixtures of MIT, BIT, and ISOX in MilliQ water were further irradiated with UV_{254} only and

319 in the presence of H_2O_2 to validate the model and the level of confidence of the quantum yields

320 and OH rate constants for the three species reported in Tables 2 and 3. The direct photolysis of

321 the mixture with UV_{254} , can be modeled using eq. (1) modified for the absorption of the three

322 species as shown in eq. (10):

$$\frac{d[S_i]}{dt} = -\frac{I_{254}}{V} \cdot \Phi_{254}^{S_i} \cdot \left(1 - \exp\left(-2.3 \cdot l \cdot \sum_i \varepsilon_{254}^{S_i} \cdot [S_i]\right)\right) \cdot \frac{\varepsilon_{254}^{S_i} \cdot [S_i]}{\sum_i \varepsilon_{254}^{S_i} \cdot [S_i]} \quad (10)$$

323 assuming that the interaction of the photogenerated by-products with their parent compounds
 324 negligibly affected their degradation. This assumption was partially corroborated by the
 325 experimental evidence that ISOX concentration profiles were invariant under the adopted
 326 conditions. Results of the simulation without any further adjustment of the previous estimated
 327 kinetic parameters are reported in Fig. 6 a-b (simulation mode). The same procedure was
 328 applied in the presence of hydrogen peroxide (UV₂₅₄/H₂O₂), modifying the kinetics as follows
 329 (eq. 11-14). The results of the simulations are reported in Fig. 6 c-d.

$$\frac{d[H_2O_2]}{dt} = -F_{H_2O_2} - \frac{F_{H_2O_2} \cdot k_H \cdot [H_2O_2]}{\sum_i k_{HO}^i [S_i]_0 + k_H [H_2O_2]} \quad (11)$$

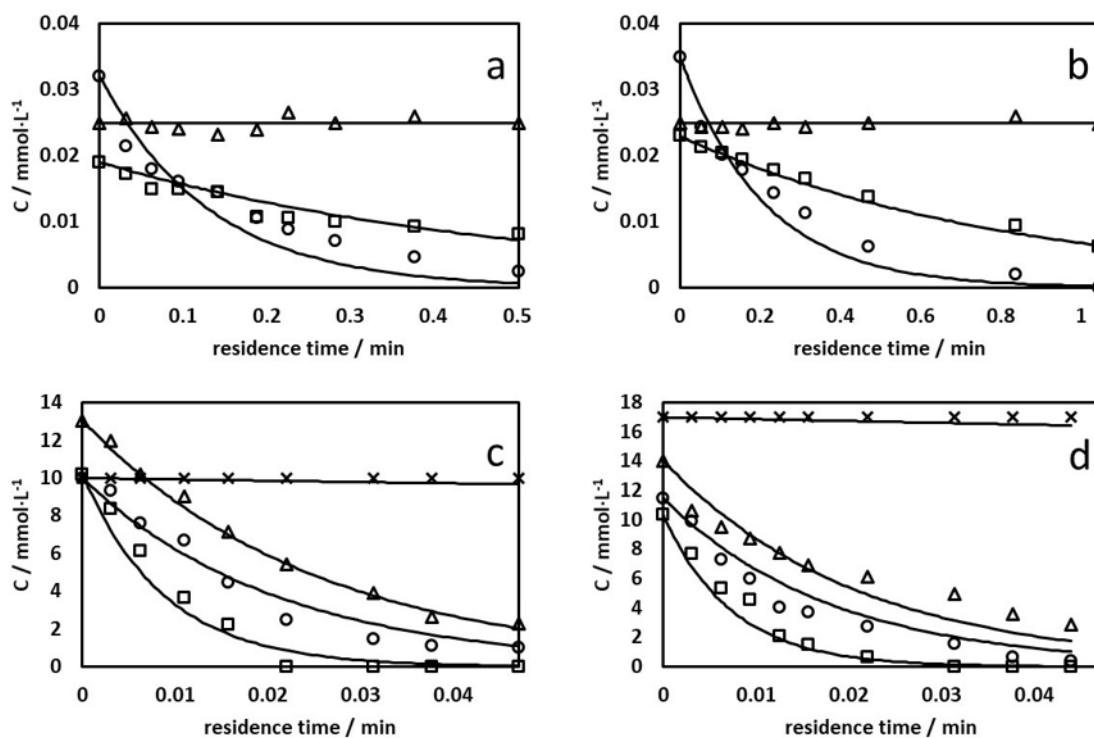
$$\frac{d[S_i]}{dt} = -\frac{I_{254}}{V} \Phi_{254}^{S_i} (1 - \exp(-2.3 \cdot l \cdot A_{tot})) \frac{\varepsilon_{254}^{S_i} \cdot [S_i]}{A_{tot}} - \frac{2k_{HO}^i [S_i] F_{H_2O_2}}{\sum_i k_{HO}^i [S_i]_0 + k_H [H_2O_2]} \quad (12)$$

330 where

$$F_{H_2O_2} = \frac{I_{254}}{V} \Phi_{254}^{H_2O_2} (1 - \exp(-2.3 \cdot l \cdot A_{tot})) \cdot \frac{\varepsilon_{254}^{H_2O_2} \cdot [H_2O_2]}{A_{tot}} \quad (13)$$

$$A_{tot} = \varepsilon_{254}^{H_2O_2} \cdot [H_2O_2] + \sum_i \varepsilon_{254}^{S_i} \cdot [S_i] \quad (14)$$

331



332

333 **Fig. 6.** Photodegradation of mixtures of MIT, BIT, and ISOX using UV₂₅₄ (a,b) and
 334 UV₂₅₄/H₂O₂ (c,d) in MilliQ water at pH = 6.0. (a): [MIT]₀ = 0.032 mM, [BIT]₀ = 0.019 mM,
 335 [ISOX]₀ = 0.025 mM, P = 8.0 W; (b): [MIT]₀ = 0.035 mM, [BIT]₀ = 0.023 mM, [ISOX]₀ =
 336 0.025 mM, P = 4.5 W; (c): [MIT]₀ = 0.020 mM, [BIT]₀ = 0.020 mM, [ISOX]₀ = 0.026 mM,
 337 [H₂O₂]₀ = 10 mM, P = 8.0 W; (d): [MIT]₀ = 0.023 mM, [BIT]₀ = 0.021 mM, [ISOX]₀ =
 338 0.028 mM, [H₂O₂]₀ = 17 mM, P = 4.5 W. (○) MIT; (□) BIT; (Δ) ISOX; (x) H₂O₂.

339

340 3.6. Transformation product identification

341 Several UV₂₅₄/H₂O₂ TPs of BIT were tentatively identified using UHPLC–high resolution–
 342 accurate mass-tandem spectrometry (UHPLC-HR-MS/MS). No TPs of MIT or ISOX were
 343 observed by UHPLC-MS/MS, despite their rapid degradation. This is likely due to either
 344 mineralization of these molecules or degradation to small molecules that are not amenable to
 345 electrospray ionization. Based on the observed TPs, the most likely pathway of degradation of
 346 BIT is radical addition of oxygen to the heterocyclic ring.

347 A mechanistic pathway for BIT degradation via UV/H₂O₂ advanced oxidation has been
348 proposed (Fig. 7). Hydroxyl radical formation is catalyzed via reaction of ultraviolet light with
349 hydrogen peroxide; the resulting radicals, along with O₂ in the non-degassed water reacted with
350 BIT to form several transformation products. Based on reaction rates in literature for dimethyl
351 sulfide (DMS), dimethyl sulfoxide, and dimethyl sulfone (Atkinson et al., 1997), the rates of
352 steps including unobserved intermediates are expected to be very fast, which is likely the reason
353 the intermediates weren't seen via mass spectrometry. Partial pressure of O₂ is also known to
354 affect reaction rates (Ramirez-Anguita et al., 2008).

355 BIT reacts first with hydroxyl radicals to form hydroxylated BIT (BIT-OH), a fast intermediate
356 that oxidizes further via O₂ in the reactor water to form BIT166 (BIT Sulfoxide (BIT-SO)).
357 BIT166 is the first observed TP, with addition of one oxygen to the sulfur heteroatom. The
358 observed accurate mass ([M-H]⁻: m/z 165.9965, C₇H₅O₂NS) is within 2.0 ppm of the theoretical
359 mass. The fragmentation (m/z 134.0249 and m/z 122.9914) observed also supports the
360 proposed structure, corresponding to loss of sulfur (m/z 134.0249) and loss of an amide (m/z
361 122.9914), respectively, both likely through rearrangement. While loss of sulfur is unusual,
362 there is supporting evidence from the National Institute of Standards and Technology (NIST)
363 library of this occurring in a similar structure, dibenzothiophene 5-oxide, which also has a ring-
364 bound sulfoxide group, as well as MS/MS evidence of this specific product loss from a prior
365 ozonation study conducted by Li et al. (Li et al., 2016b; NIST., 2018) (Fig. 8a).

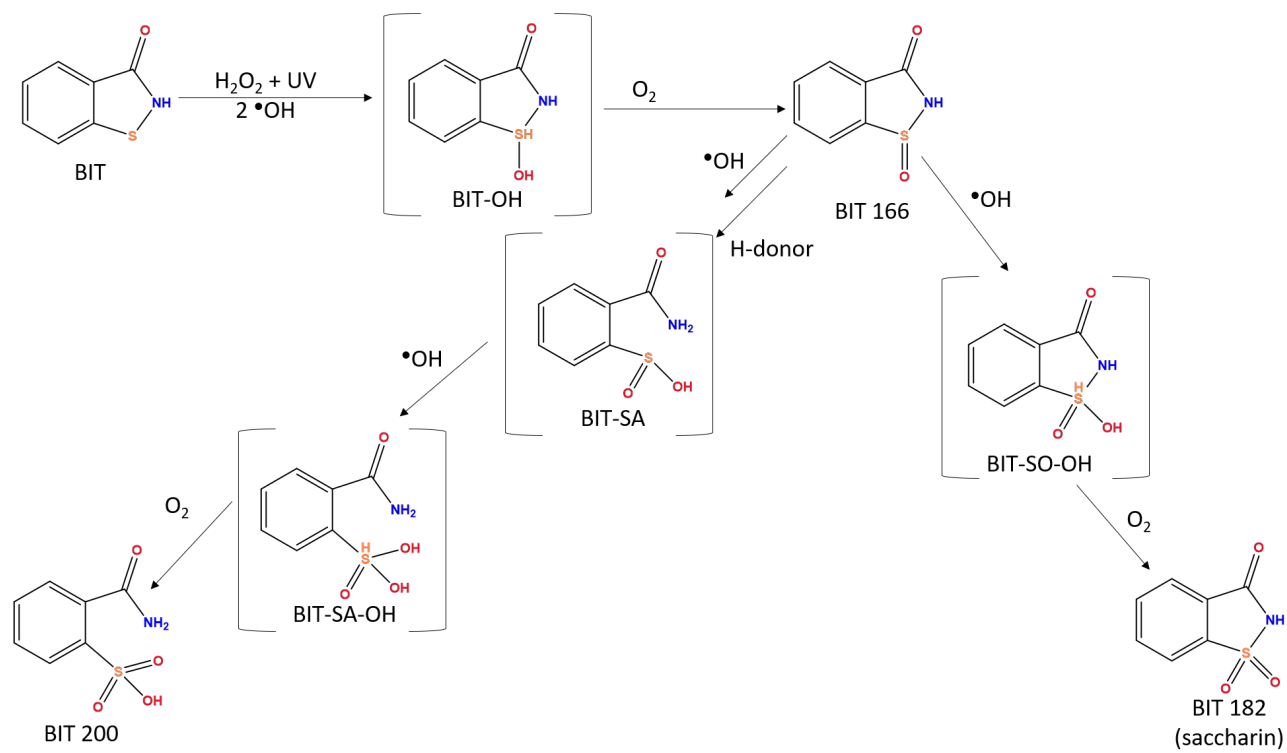
366 BIT166 then oxidizes further, split into two potential pathways. The first pathway involves the
367 same mechanism of radical addition/hydroxylation at the sulfur heteroatom to BIT-SO-OH, a
368 fast unobserved intermediate, subsequently oxidized via O₂ to Saccharin (BIT182, a BIT-
369 sulfone). Saccharin has two oxygens attached to the heterocyclic ring's sulfur. The proposed
370 structure is supported by two strong fragments and high mass accuracy (Fig. 8b). The observed
371 accurate mass ([M-H]⁻: m/z 181.9920, C₇H₅O₃NS) is within 1.4 ppm of the theoretical mass.

372 Fragments m/z 118.0300 and m/z 105.9607 are proposed to be due to the loss of SO_2 and C_6H_4 ,
373 respectively. The latter fragment shows cleavage down the center of the molecule (Fig. 8b).

374 The second pathway is more radical driven. BIT166 is oxidized via hydroxyl radical reaction
375 (hydroxylating the sulfur heteroatom) and receives a hydrogen on the adjacent nitrogen.
376 Subsequent heterocyclic ring breakage separates the sulfur and nitrogen moieties, forming
377 unobserved intermediates BIT-sulfinic acid (BIT-SA) and hydroxylated BIT-SA (BIT-SA-OH)
378 in succession. This is further oxidized via radical reaction to BIT200, a BIT-sulfonic acid. The
379 proposed structure includes a sulfate moiety that is likely cleaved during further degradation.
380 The mass measurement accuracy for this molecular formula ($[\text{M-H}]^-$: m/z 200.0034,
381 $\text{C}_7\text{H}_7\text{O}_4\text{NS}$) is 5.5 ppm. The fragment ion m/z 156.9968 is due to cleavage between the
382 aromatic ring and the amide moiety of the TP, and m/z 118.0299 is due to loss of the HSO_3
383 group (Fig. 8c).

384 The formation of these three TPs agrees well with the chemistry of sulfur containing
385 compounds subjected to the attack of OH radicals. It is known that the sulfur atom of alkyl
386 sulfide is oxidized by OH radical to sulfoxide and the latter to sulfone and sulfonic acid (Arsene
387 et al. 2002).

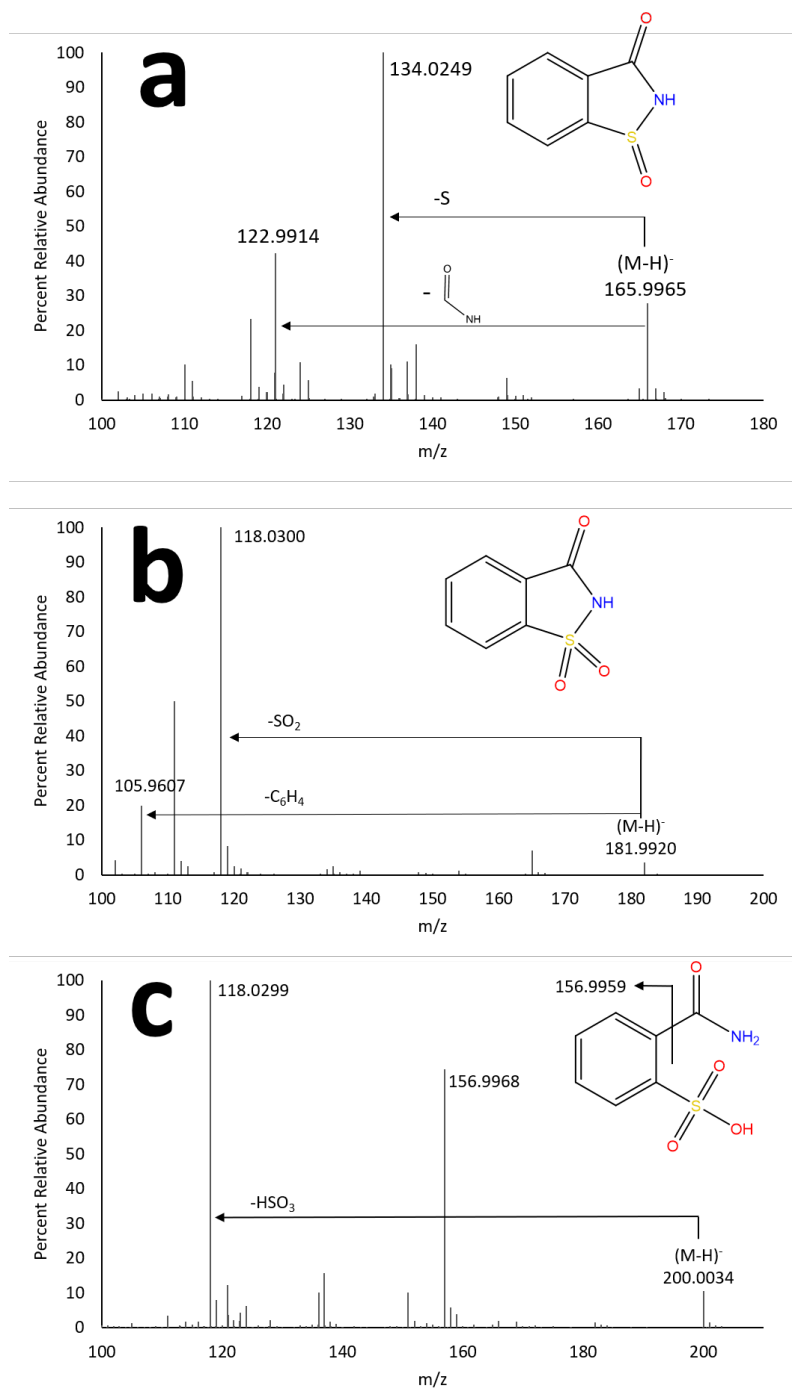
388 These three TPs have also been reported in ozonation reactions of benzisothiazolinone,
389 although there are notable mechanistic differences between ozonation and UV/ H_2O_2
390 degradation. Li et al. (2016b) proposed a transformation pathway for the ozonation degradation
391 of BIT. The addition of oxygen occurs primarily at the electron-rich divalent sulfur in the
392 heterocyclic ring. In this mechanism, BIT is fully degraded to sulfate ions, small organic acids,
393 inorganic carbon, and organic nitrogen. Li et al. (2016b) confirmed the second TP
394 (BIT182/saccharin) via standard comparison, as well as a final degradation product of sulfate
395 (Li et al., 2016b).



396

397 **Fig. 7.** Proposed mechanistic pathway for UV/H₂O₂ advanced oxidation degradation of BIT.

398



399

400 **Fig. 8.** a) MS/MS spectrum of benzisothiazolinone TP BIT166 with [M-H]⁻: m/z = 165.9965.

401 b) MS/MS spectrum of benzisothiazolinone TP BIT182 (saccharin) with [M-H]⁻: m/z =

402 181.9920. c) MS/MS spectrum of benzisothiazolinone TP BIT200 with [M-H]⁻: m/z =

403 200.0034. For all three transformation products, the scan range was m/z 50-750, but no

404 fragment ions were seen below m/z 100.

405

406 CONCLUSIONS

407 In this study, the photodegradation of MIT, BIT, and isoxazole by UV_{254} and UV_{254}/H_2O_2
408 processes was investigated in a highly efficient microcapillary photoreactor, which allows rapid
409 investigation of the degradation kinetics.

410 The collected data were used to develop kinetic models for the estimation of the quantum yields
411 of direct photolysis and the rate constant of reaction with the photogenerated OH radicals. The
412 accuracy of the determined rate constants was demonstrated by predicting the photodegradation
413 of mixtures of the three target compounds in both ultrapure water and in synthetic wastewater.

414 The estimated values are in agreement with those reported in the literature for compounds with
415 a similar molecular structure. In consequence, this study has shown a fast method for
416 determination of water contaminants reactions rate constants which can be of use for the design
417 of advanced water treatment processes. Furthermore, the use of a microphotoreactor allows for
418 the faster identification of the reaction mechanism and of the photo-degradation byproducts.

419 As a result, a mechanistic pathway was proposed for UV/H_2O_2 advanced oxidation degradation
420 of BIT, the first such pathway for this treatment of BIT. The main transformation products of
421 BIT photo-degradation proposed in the novel mechanistic pathway were tentatively identified
422 via high resolution accurate mass MS/MS, suggesting the addition of oxygens to the
423 heterocyclic ring

424 The identification of the key transformation byproducts and the evaluation of the kinetic
425 parameters would allow the further development of complex models that address the
426 degradation of key target compounds in real wastewater matrices, as well as the evaluation of
427 the ecotoxicity of parent compounds and their by-products on aquatic organisms. The ultrafast
428 micro-photoreactor methodology described in this study lays the groundwork for an

429 environmentally friendly, cost effective, time-saving experimental protocol for studies of
430 homogeneous phase AOPs.

431

432

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438

439

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Supplementary Information

Ultrafast photodegradation of isoxazole and isothiazolinones by UV₂₅₄ and UV₂₅₄/H₂O₂ photolysis in a microcapillary reactor

Danilo Russo^{a,d*}, Kristin H. Cochran^b, Danielle Westerman^b, Gianluca Li Puma^c, Raffaele Marotta^d, Roberto Andreozzi^d, Susan D. Richardson^{b,*}.

^a Present address: Department of Chemical Engineering and Biotechnology, University of Cambridge, UK.

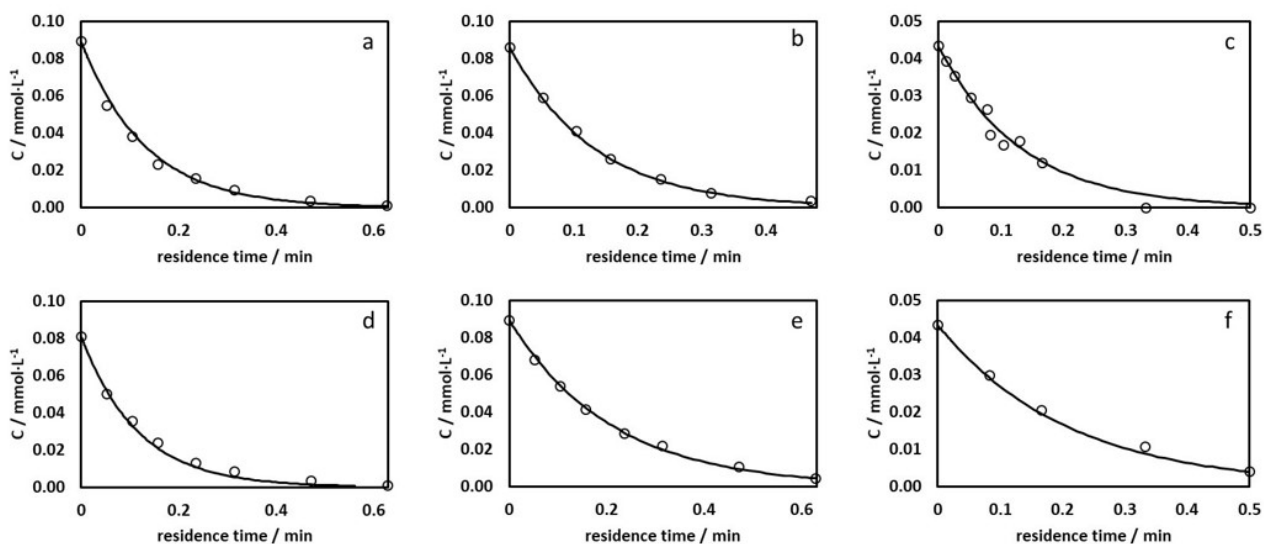
^b Department of Chemistry and Biochemistry, University of South Carolina, USA.

^c Environmental Nanocatalysis & Photoreaction Engineering, Department of Chemical Engineering, Loughborough University, UK.

^d Dipartimento di Ingegneria Chimica, dei Materiali e della Produzione Industriale, Università di Napoli Federico II, Italy.

*Corresponding author: Danilo Russo: danilo.russo3@unina.it; dr473@cam.ac.uk; Susan D. Richardson, RICHA545@mailbox.sc.edu.

Keywords: micropollutants; advanced oxidation processes; isoxazole; water reclamation; water treatment; isothiazolinones.



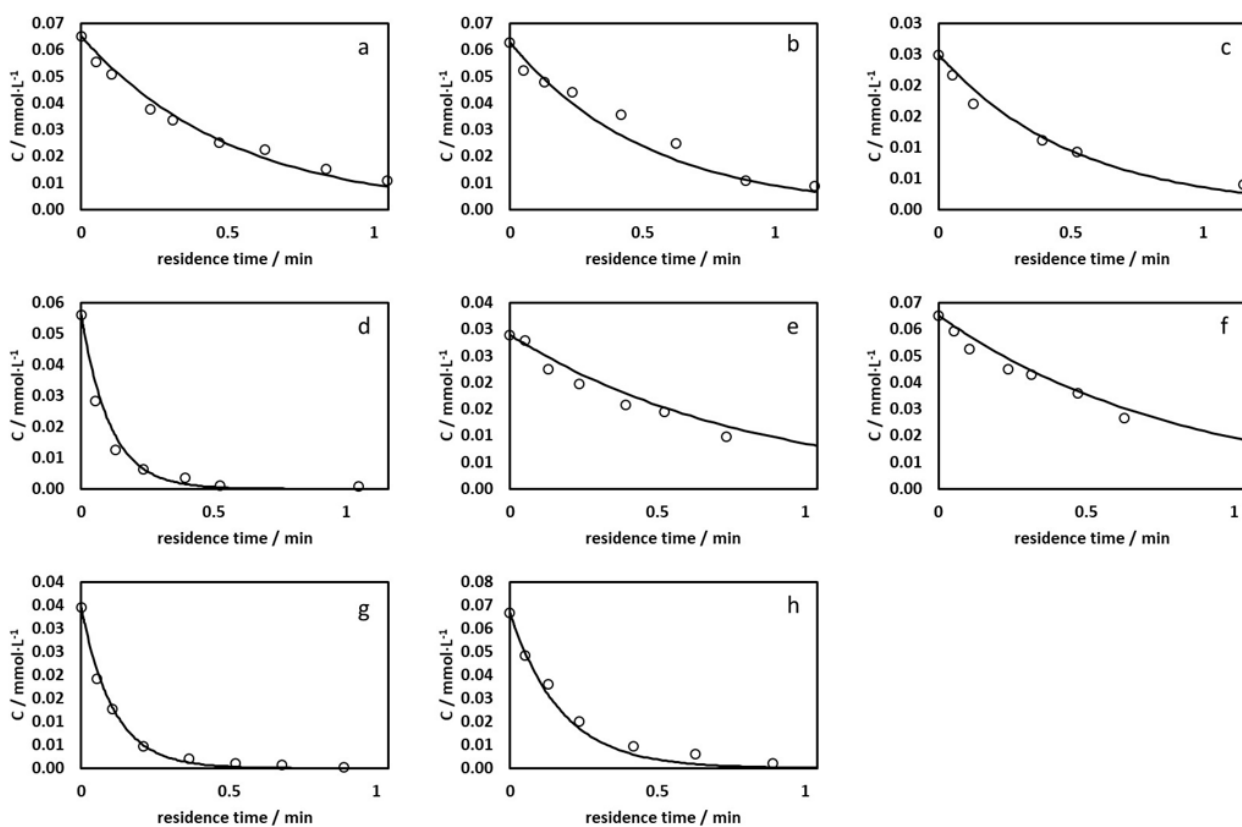
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711 **Fig. S1.A.** Direct photolysis of MIT. Experimental data (O), calculated data (curves).

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Experimental conditions are reported in Table S1.

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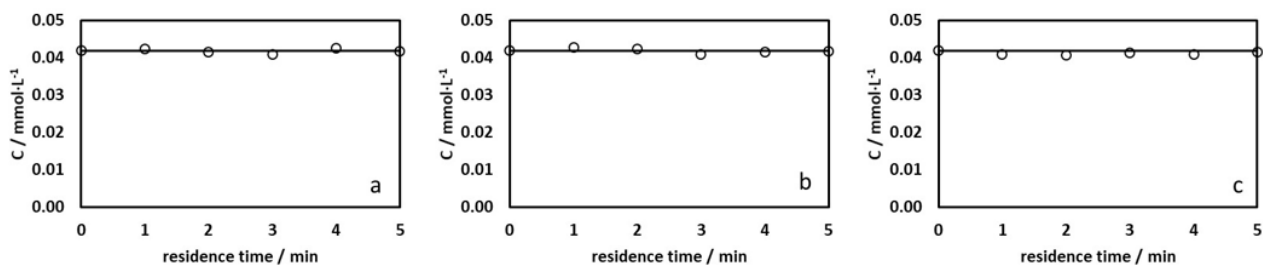
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715 **Fig. S1.B.** Direct photolysis of BIT. Experimental data (O), calculated data (curves).

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Experimental conditions are reported in Table S1.

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719 **Fig. S1.C.** Direct photolysis of ISOX. Experimental data (○), calculated data (curves).

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Experimental conditions are reported in Table S1.

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722 Table S1. Experimental conditions adopted for quantum yield estimation. σ (%) is the overall

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percentage standard deviation.

Reference Fig. S1	Compounds	$[S_i]_0$ ($\text{mmol}\cdot\text{L}^{-1}$)	pH	Nominal P (W)	σ (%)
A-a	MIT	0.0894	6	8.0	1.37
A-b	MIT	0.0862	4	8.0	0.43
A-c	MIT	0.0434	6	8.0	0.15
A-d	MIT	0.0809	8	8.0	0.49
A-e	MIT	0.0809	6	4.5	0.27
A-f	MIT	0.0434	6	4.5	1.16
B-a	BIT	0.0653	6	8.0	1.61
B-b	BIT	0.0630	4	8.0	1.62
B-c	BIT	0.0250	6	8.0	0.88
B-d	BIT	0.0562	8	8.0	2.48
B-e	BIT	0.0290	6	4.5	1.13
B-f	BIT	0.0653	6	4.5	2.12
B-g	BIT	0.0346	8	8.0	2.54

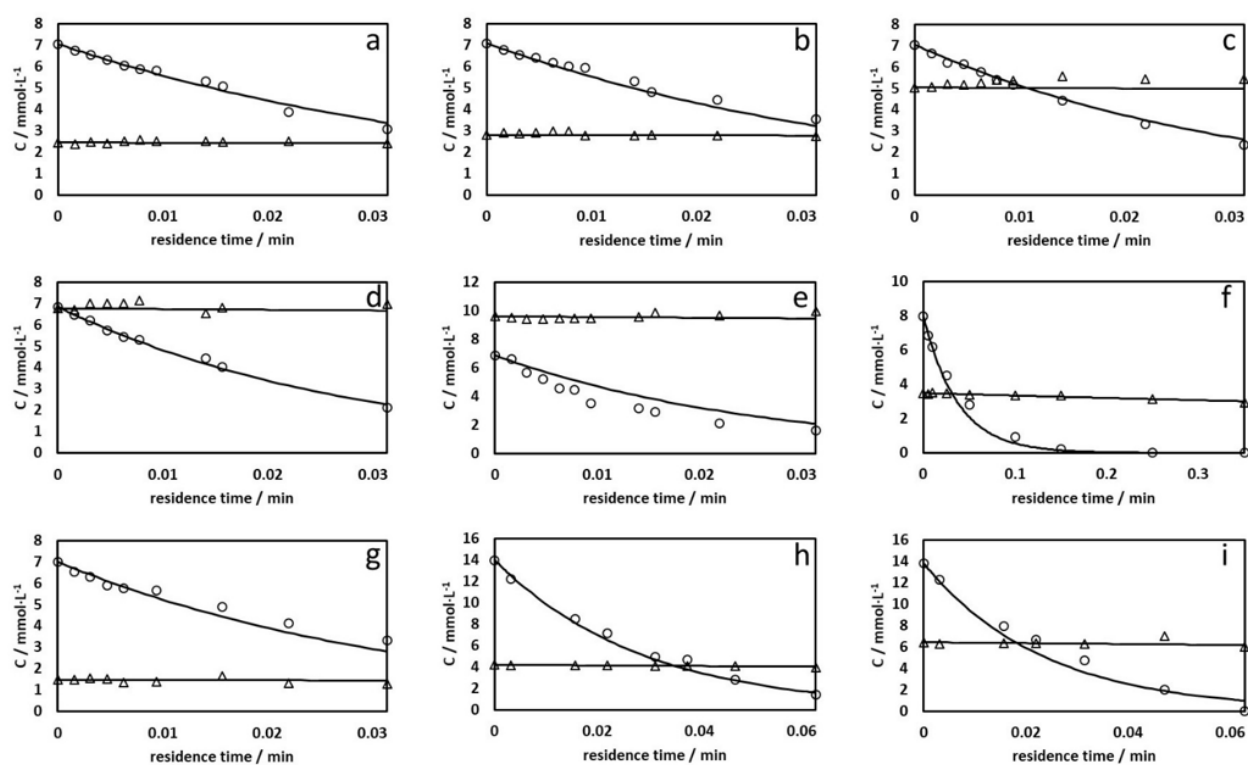
B-h	BIT	0.0669	8	4.5	1.80
C-a	ISOX	0.0420	4	8.0	/
C-b	ISOX	0.0420	6	8.0	/
C-c	ISOX	0.0420	8	8.0	/

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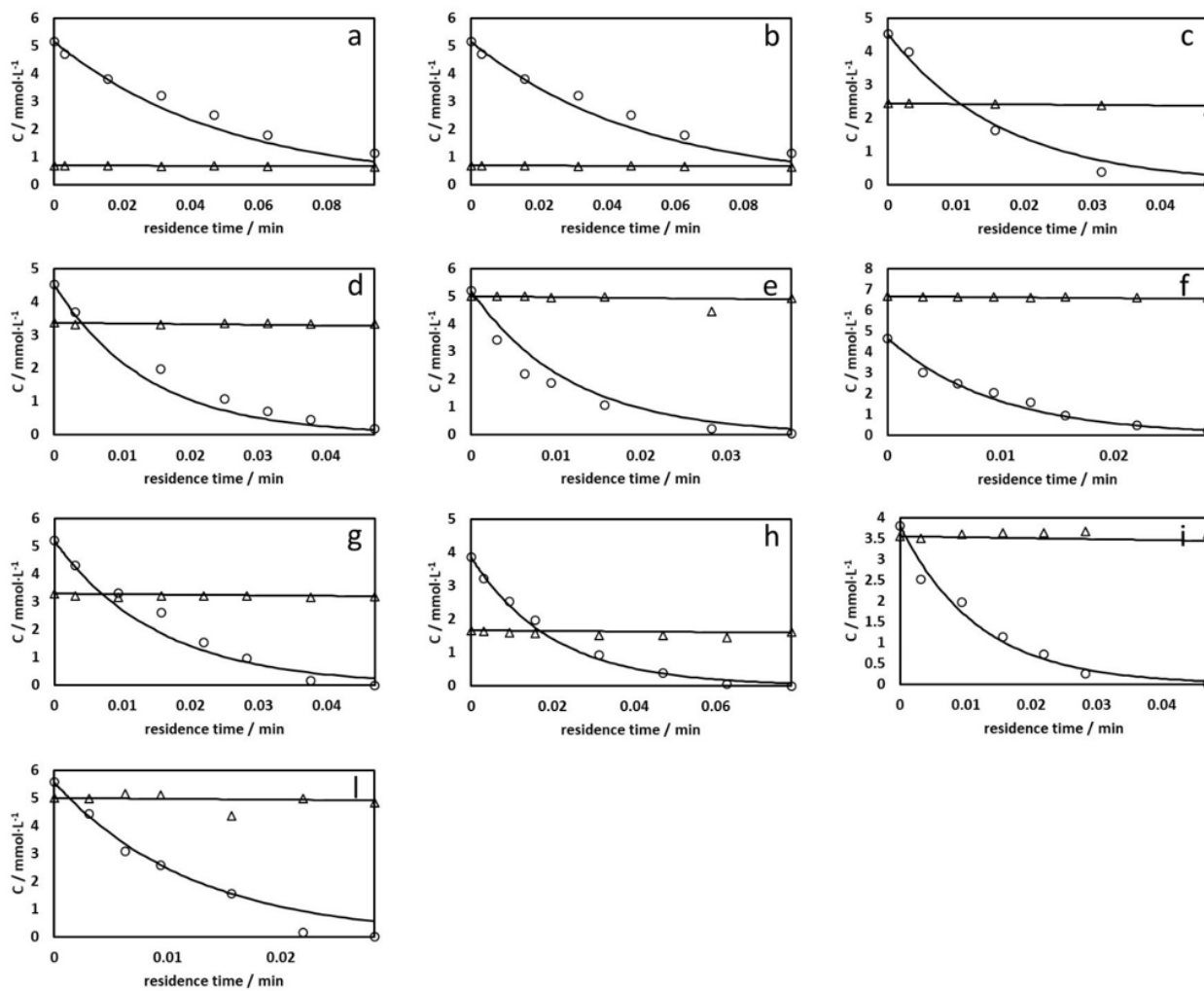
729 **Fig. S2.A.** Photodegradation of MIT by UV_{254}/H_2O_2 in MilliQ water: experimental data

730 (symbols), calculated data (lines). MIT (\circ), H_2O_2 (Δ). MIT concentrations are multiplied by

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160 for viewing convenience.

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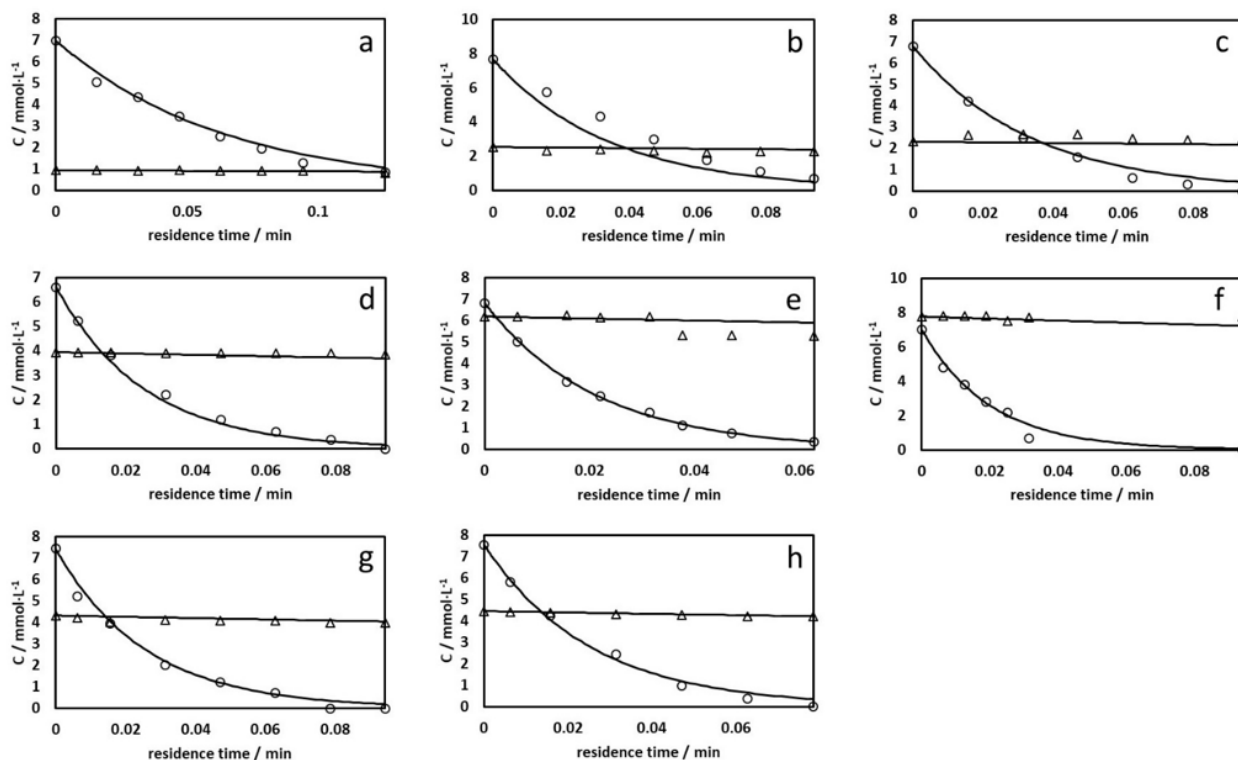
734 **Fig. S2.B.** Photodegradation of BIT by UV₂₅₄/H₂O₂ in MilliQ water: experimental data

735 (symbols), calculated data (lines). BIT (○), H₂O₂ (Δ). BIT concentrations are multiplied by

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739 **Fig. S2.C.** Photodegradation of ISOX by UV₂₅₄/H₂O₂ in MilliQ water: experimental data

740 (symbols), calculated data (lines). ISOX (○), H₂O₂ (Δ). ISOX concentrations are multiplied

741 by 160 for viewing convenience.

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744 Table S2. Experimental conditions adopted for k_{HO}^i estimation. σ (%) is the overall

745 percentage standard deviation.

Reference Fig. S2	Compounds	$[S_i]_0$ (mmol·L ⁻¹)	$[H_2O_2]_0$ (mmol·L ⁻¹)	pH	Nominal P (W)	σ (%)
A-a	MIT	0.044	2.45	6	4.5	0.95
A-b	MIT	0.044	2.82	6	4.5	0.79
A-c	MIT	0.044	5.04	6	4.5	1.68
A-d	MIT	0.043	6.77	6	4.5	2.12
A-e	MIT	0.043	9.60	6	4.5	3.39

A-f	MIT	0.050	3.49	8	4.5	0.73
A-g	MIT	0.044	1.48	6	8.0	0.63
A-h	MIT	0.088	4.20	6	8.0	0.80
A-i	MIT	0.086	6.44	6	8.0	2.44
B-a	BIT	0.032	0.69	6	8.0	2.00
B-b	BIT	0.032	1.57	6	8.0	3.38
B-c	BIT	0.028	2.44	6	8.0	1.25
B-d	BIT	0.028	3.37	6	8.0	2.21
B-e	BIT	0.033	5.00	6	8.0	4.73
B-f	BIT	0.029	6.68	6	8.0	0.34
B-g	BIT	0.033	3.30	4	8.0	2.98
B-h	BIT	0.024	1.67	8	8.0	2.24
B-i	BIT	0.024	3.56	8	8.0	1.64
B-l	BIT	0.035	5.01	8	8.0	0.55
C-a	ISOX	0.044	0.93	6	8.0	1.29
C-b	ISOX	0.048	2.55	6	8.0	6.22
C-c	ISOX	0.042	2.32	6	8.0	4.91
C-d	ISOX	0.041	3.95	6	8.0	1.77
C-e	ISOX	0.043	6.20	6	8.0	1.33
C-f	ISOX	0.040	7.77	6	8.0	1.22
C-g	ISOX	0.047	4.33	8	8.0	2.24
C-h	ISOX	0.047	4.46	4	8.0	0.49

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