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3 **Correlation between circuital current, Cu(II) reduction and cellular**
4 **electron transfer in EAB isolated from Cu(II)-reduced biocathodes**
5 **of microbial fuel cells**

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17

18 **Abstract**

19 The performance of four indigenous electrochemically active bacteria (EAB)
20 (*Stenotrophomonas maltophilia* JY1, *Citrobacter* sp. JY3, *Pseudomonas aeruginosa*
21 JY5 and *Stenotrophomonas* sp. JY6) was evaluated for Cu(II) reduction on the
22 cathodes of microbial fuel cells (MFCs). These EAB were isolated from well
23 adapted mixed cultures on the MFC cathodes operated for Cu(II) reduction. The
24 relationship between circuital current, Cu(II) reduction rate, and cellular electron
25 transfer processes was investigated from a mechanistic point of view using X-ray
26 photoelectron spectroscopy, scanning electronic microscopy coupled with energy
27 dispersive X-ray spectrometry, linear sweep voltammetry and cyclic voltammetry.
28 JY1 and JY5 exhibited a weak correlation between circuital current and Cu(II)
29 reduction. A much stronger correlation was observed for JY3 followed by JY6,
30 demonstrating the relationship between circuital current and Cu(II) reduction for
31 these species. In the presence of electron transfer inhibitors (2,4-dinitrophenol or
32 rotenone), significant inhibition on JY6 activity and a weak effect on JY1, JY3 and
33 JY5 was observed, confirming a strong correlation between cellular electron transfer
34 processes and either Cu(II) reduction or circuital current. This study provides
35 evidence of the diverse functions played by these EAB, and adds to a deeper
36 understanding of the capabilities exerted by diverse EAB associated with Cu(II)
37 reduction.

38

39 **Keywords:** biocathode; microbial fuel cell; electrochemically active bacteria; Cu(II)
40 reduction; electron transfer inhibitor

41

42 **1 Introduction**

43 Microbial fuel cells (MFCs) are emerging as new, sustainable and effective
44 technologies for the recovery of heavy metals from waste and wastewater [1].
45 Among diverse heavy metals, Cu(II), which is common in the electroplating and
46 mining industries [2-3], has attracted significant attention due to the potential for its
47 recovery and simultaneous wastewater detoxification. The recovery of Cu(II) with
48 abiotic cathode MFCs has been demonstrated over a wide range of operating
49 conditions and cell architectures [4-9]. However, abiotic cathodes often require the
50 use of costly noble or non-noble co-catalysts in addition to an acidic medium.
51 Therefore, the development of biocathodic MFCs, which are based on the catalysis
52 of self-regenerating electrochemically active bacteria (EAB) under a neutral
53 environment, may provide a sustainable and green alternative to abiotic systems.
54 Biocathodic MFCs avoid the use of expensive materials and toxic organic reagents,
55 and reduce the consumption of energy and acids [10-14]. Biocathodes are also able
56 to reduce electrode overpotentials, the production of sludge, and the overall cost and
57 the maintenance of MFCs. MFCs, utilizing mixed cultures, have been shown to be
58 efficient in the recovery of Cu(II) from mixed metal influent and also a promising
59 system for the synthesis of copper [15]. In contrast, MFCs with biocathodes operated
60 with pure cultures have been used to study specific EAB and their electrochemical
61 performance [10-14]. The exogenous EAB of *Shewanella* is one of the few examples
62 which is able to reduce a metal (Cr(VI)) in MFCs [16-17].

63 Microorganisms possess endurance to aqueous Cu(II) through a variety of
64 mechanisms due to their intrinsic abilities and habitat sites [18-20]. Therefore, well
65 adapted microorganisms could provide new insights with regards to heavy metal
66 reduction in MFCs. A limited number of microorganisms exhibiting efficient rates of
67 Cu(II) reduction have been cultivated under Cu(II)-adaptive conditions [20-24].
68 Similar considerations, in principle, hold true for their use in cathodic reductive
69 environments in MFCs, under which the activities of different indigenous EAB may
70 exhibit various Cu(II) reduction rates. In parallel, EAB immobilized on the surface
71 of cathodes may also be able to utilize cathodic electrons for their internal
72 metabolism [11,25]. The operation of MFCs at different concentrations of Cu(II) in
73 the catholyte is expected to clarify the correlation between the circuit current and
74 the rate of Cu(II) reduction associated with the use of isolated EAB.

75 The bacteriological reduction of Cu(II), in the absence of a circuit current, is
76 believed to be associated with cellular electron transfer processes through the
77 cytoplasmic membrane and with the flux of protons through ATP-synthase [26-27].
78 Such mechanisms can be unravelled using cellular electron transfer inhibitors, such
79 as 2,4-dinitrophenol (DNP) and rotenone (C₂₃H₂₂O₆). DNP dissipates the proton
80 motive force associated with cellular electron transfer processes, and decreases
81 hydrogen production by inhibiting the ATP synthesis by photophosphorylation, in
82 the absence of a circuit current [28]. In contrast, rotenone inhibits the activity of
83 NADH-dehydrogenase and blocks the reduction of U(VI) by facultative anaerobic
84 bacteria in the absence of a circuit current [29]. The utilization of rotenone and
85 DNP, in the presence and absence of a circuit current passing through the EAB

86 cathodes of MFCs is thus expected to establish whether the circuital current and
87 Cu(II) reduction are associated with cellular electron transfer processes in the EAB
88 species.

89 In this study, we elucidate from a mechanistic point of view the performance
90 and impact of four indigenous different EAB on Cu(II) reduction in MFCs. The EAB
91 tentatively identified as *Stenotrophomonas maltophilia* JY1, *Citrobacter* sp. JY3,
92 *Pseudomonas aeruginosa* JY5 and *Stenotrophomonas* sp. JY6, were isolated from
93 well adapted mixed cultures grown on the surface of MFC cathodes operated for
94 Cu(II) reduction [15]. X-ray photoelectron spectroscopy (XPS), scanning electronic
95 microscopy (SEM) coupled with energy dispersive X-ray spectrometry (EDS), linear
96 sweep voltammetry (LSV) and cyclic voltammetry (CV) were used to investigate the
97 effect of circuital current on the speciation of the deposited copper, the morphologies
98 of the cathodes and the cathodic redox reactions for each EAB species. The
99 relationship between circuital current, the rate of Cu(II) reduction and the cellular
100 electron transfer processes associated with each of the four EAB were clarified
101 through the system response to a step change of Cu(II) concentration in the catholyte
102 and reaction mechanisms elucidated in the presence or absence of DNP or rotenone
103 electron transfer inhibitors.

104

105 **2 Materials and Methods**

106 *2.1 EAB isolation, incubation and identification*

107 Bacterial isolates were obtained from mixed culture cultivated in the
108 Cu(II)-reduced biocathodes of MFCs [15]. The isolation and incubation processes
109 are detailed in the Supplementary Material (SM). The DNA of these EAB isolates
110 was extracted using a Qubit2.0 DNA kit (Sangon Biotech (Shanghai) Co. Ltd., China)
111 according to the manufacturer's procedure. The 16S rRNA gene was amplified by
112 PCR using universal primers 518 F (5' CAGAGTTTGATCCTGGCT3') and 1540R
113 (5'AGGAGGTGATCCAGCCGCA3'), as described in SI. The sequence data were
114 compared with the GenBank database using the Blast server at NCBI
115 (<http://www.ncbi.nlm.nih.gov/BLAST/>) to accurately identify the bacterial strains.
116 All tests were performed in duplicate.

117

118 *2.2 MFC reactors setup and operation*

119 Identical two-chamber MFCs with cylindrical chambers 4.0 cm long by 3.0 cm
120 in diameter were used in all experiments. The anodic and cathodic chambers were
121 separated by a cation exchange membrane (CEM) (CMI-7000 Membrane
122 International, Glen Rock, NJ) with a projected surface area of 7.1 cm². Both the
123 anode and cathode were filled with graphite felt (1.0 cm × 1.0 cm × 0.5 cm, 8 pieces,
124 Sanye Co., Beijing, China) and carbon rods were used as current collectors in both
125 anode and cathode. For each of the duplicate reactors three replicate experiments
126 were performed. The MFCs were operated at a fixed external resistance of 510 Ω.

127 The anodes were inoculated with suspended bacteria collected from a previous
128 acetate-fed MFC reactor and an equivalent volume of nutrient solution containing
129 acetate (1.0 g/L) was added [30-31]. The cathodes were fed using the same medium,

130 except acetate was replaced by NaHCO₃ (10 mg/L), with further addition of Cu(II)
131 (5 mg/L) to the cathodic chambers. Cathodes were quantitatively inoculated with the
132 isolates with a total of 3×10^8 colony forming unit. The anolyte and catholyte were
133 sparged with N₂ gas for 15 min prior to adding the solutions into the electrode
134 chambers. No measurable Cu(II) in the anolyte and acetate in the catholyte were
135 observed during each cycle operation, excluding the possibility of Cu(II) and acetate
136 diffusion between the chambers, although the retention of Cu(II) on the ion
137 exchange membrane could not be precluded [15]. Other catholyte and operational
138 conditions are described in SM.

139 The performance of the biocathodes was evaluated against four control
140 experiments, including (i) the operation of the reactors under the open circuit
141 condition (OCC), (ii) the operation with a closed circuit but without the inoculation
142 of the EAB (abiotic control), (iii) the cathodes covered with the EAB but in the
143 absence of Cu(II), and (iv) the cathodes tested in the absence of both EAB and
144 Cu(II). The last two control experiments were used to evaluate the CVs performance
145 of the cell.

147 2.3 Measurement, analysis and calculation

148 The circuit current, dissolved oxygen, biomass, organics and Cu(II)
149 concentration were determined according to the methodology reported in SM. The
150 rate of Cu(II) removal and charge distribution were calculated as detailed in SM.

151 Maximum power was obtained by running LSV at a scan rate of 0.1 mV/s
152 [30-31]. Power and current densities were normalized to the projected surface area of
153 the membrane. EAB cathode redox behavior was studied using CV (CHI 650,
154 Chenhua, Shanghai). The potential was scanned between -0.36 V and +0.46 V (vs
155 SHE) at a scan rate of 1.0 mV/s using a standard three-electrode arrangement with the
156 biocathode as the working electrode, platinum plate as the counter electrode, and
157 Ag/AgCl as the reference electrode. One-way ANOVA in SPSS 19.0 was used to
158 analyze the statistical variation of the data, and all of the data indicated significance
159 levels of $p < 0.05$.

160 The surfaces of the Cu-laden biomass were analyzed by X-ray photoelectron
161 spectroscopy (XPS, Thermo Fisher Scientific, ESCALAB 250, US) with a Mono Al
162 K α X-ray source (1486.6 eV of photons). The X-ray source was run at a reduced
163 power of 150 W. The morphology of the electrodes after Cu(II) reduction were
164 examined with a SEM (QUANTA450, FEI company, USA) equipped with an EDS
165 (X-MAX 20 mm²/50 mm², Oxford Instruments, UK) according to the method
166 described previously [15,30].

168 3 Results and Discussion

169 3.1 EAB Isolation

170 Four EAB were successfully isolated from well adapted mixed cultures grown on
171 the surface of MFC cathodes operated for Cu(II) reduction [15] (Table S1). All
172 bacteria were gram-negative and major opportunistic to facultative or survived from
173 an anaerobic environment. JY1 matching *Stenotrophomonas maltophilia*, is known to

174 convert Cu(II) into Cu(0) on the cell surface, in the absence of cathodic electrons
175 [22-24]. *S. maltophilia* has been isolated previously from a copper polluted area [22],
176 and has never been reported in MFCs. JY3 closely related to *Citrobacter* sp., is able to
177 remove Cu(II) in a medium of SO_4^{2-} through the formation of CuS precipitate in the
178 absence of cathodic electrons [20]. It has been isolated previously from anodic MFC
179 biofilms in the absence of Cu(II) [32]. JY5 matching *Pseudomonas aeruginosa*, is
180 able to remove Cu(II) in the absence of cathodic electrons [21]. It has been reported in
181 either denitrification autotrophic biocathodes of MFCs [33], or in MFCs operated for
182 the degradation of phenol and glycerol through mediated electron transfer [34-37].
183 Finally, JY6 corresponding to *Stenotrophomonas* sp., can tolerate high concentrations
184 of metals including Ag, Cu, Cd, Hg and Mn [38-39] and has been isolated previously
185 from a wide range of environments.

186

187 3.2 EAB activity assessment

188

Here Fig. 1

189 All four EAB played a significant role in the reduction of Cu(II) in the MFCs and
190 displayed rates of Cu(II) reduction higher than those found in both OCC and abiotic
191 CCC controls (Fig. 1A). Previous studies with mixed culture biocathodes using
192 nitrobenzene, pentachlorophenol, Cr(VI), Co(II) or Cu(II) as an electron acceptor
193 [31,40-44] support these findings. The Cu(II) reduction rates in the range $(0.82 \pm 0.05$
194 $- 1.11 \pm 0.01 \text{ mg/L/h})$ were close to those found in mixed cultures $(1.07 \pm 0.01$
195 $\text{mg/L/h})$ at the same Cu(II) concentration (5 mg/L) [15], reflecting the robust capacity
196 of these isolates for reducing Cu(II).

197

Here Fig. 2

198 The results in Figs. 1 and 2 show that the EAB catalytic process produced higher
199 circuitual currents (Fig. 1B), open circuit potentials (Fig. 2A and B) and maximum
200 power production (Fig. 2C and D) in comparison with the values under abiotic control,
201 irrespective of the Cu(II) concentrations of 5 mg/L (Figs. 1, 2A and 2C) and 20 mg/L
202 (Figs. 1, 2B and 2D). The background circuitual current, voltage output, power
203 production and electrode potential in the absence of Cu(II) (Figs. 1B, 2A and 2C, and
204 Fig. S1) were attributed to the reduction of residual dissolved oxygen [15,43].

205 Higher circuitual currents and rates of Cu(II) reduction were observed by
206 increasing the concentration of Cu(II) in the cathodic chamber from 5 mg/L to 20
207 mg/L (Fig. 1). This effect was more significant for JY3 and JY6, demonstrating the
208 significant impact of circuitual current on the rate of Cu(II) reduction for these two
209 species. Conversely, the circuitual currents observed with JY1 and JY5 were
210 insignificant (Fig. 1B), in relation to the significant increase observed in the rate of
211 Cu(II) reduction (Fig. 1A). The reduction of Cu(II) can therefore be ascribed to the
212 effect of the abiotic cathodes only and to the effect of the individual JY1 or JY5
213 bacteria in response to the increase in Cu(II) concentration (Fig. 1A). These results
214 illustrate the weak correlation between circuitual current and the rate of Cu(II)
215 reduction for both JY1 and JY5, a result that will be further supported by the XPS

216 analyses.

217 The majority of the EAB cathodes displayed significant overshoots in voltage
218 output and power density in comparison with the abiotic controls, at a Cu(II)
219 concentration of 20 mg/L (Fig. 2B and D). This suggests that the demand for electrons
220 in these experiments exceeded the rate of electrons supplied by microbial activity, and
221 this resulted in the depletion of electrons and ions in the catholyte. Such observations
222 have also been reported in other MFC studies using O₂ as electron acceptor [45-47].
223 The cathode with bacterial JY3 displayed the highest performance with the highest
224 circuital current (Fig. 1B) and most importantly without displaying an overshoot in
225 power density, indicating that the microbial activity with this species was significant.

226 The cathodic potentials of all EAB were found to vary much more than the
227 anodic potentials, over the current density range investigated (Fig. S2A, initial Cu(II)
228 of 5 mg/L; Fig. S2B, initial Cu(II) of 20 mg/L). In consequence, the performance of
229 the MFCs was controlled by the reduction of copper at the biocathode, rather than the
230 microbial phenomena that occurred at the anode. The presence of the EAB at the
231 cathode, therefore, had a significant impact on the propensity of the cathodes for
232 electricity generation and voltage output.

233 Increasing the concentration of Cu(II) in the catholyte diverted a larger fraction
234 of electrons from the anodic oxidation of organics towards the reduction of Cu(II),
235 with JY6 showing the highest value among the different EAB ($11.2 \pm 0.1\%$ from a
236 total of 2.9 C and at a Cu(II) of 20 mg/L). The remaining $0.4 \pm 0.0\%$ was used for
237 oxygen reduction, $52.3 \pm 0.0\%$ for organics production, and 33.5 ± 0.0 for biomass
238 growth (Table S2). A large fraction of the cathodic electrons from $2.6 \pm 0.1\%$ for JY6
239 up to 43.2 ± 0.4 for JY3 were involved in other parallel reactions or unknown
240 processes.

241 The abiotic cathodes displayed reductive peak potentials of 0.033 V at a Cu(II)
242 of 5 mg/L (Fig. S3A and Table S3) and 0.037 V at 20 mg/L (Fig. S3B and Table S3),
243 reflecting the positive shift of reductive peak potential at a higher Cu(II)
244 concentration. Reductive onset potentials for all EAB cathodes were more positive
245 than the abiotic controls ($0.272 - 0.297$ V vs. 0.264 V at a Cu(II) of 5 mg/L and
246 $0.278 - 0.328$ V vs. 0.267 V at a Cu(II) of 20 mg/L) (Table S3) and the shift was
247 more significant for the reductive peak potentials of all EAB cathodes with respect
248 to the abiotic controls ($0.040 - 0.063$ V vs. 0.033 V at a Cu(II) of 5 mg/L, $0.043 -$
249 0.079 V vs. 0.037 V at a Cu(II) of 20 mg/L). These results, in combination,
250 demonstrate the varying degree of influence exerted by each EAB on the catalytic
251 activity toward Cu(II) reduction, which is consistent with the effect of EAB on the
252 reduction of Co(II) and chloramphenicol on mixed culture cathodes [43,48]. The JY1
253 and JY5 bacteria exhibited much lower reductive onset potentials than JY3 and JY6,
254 implying a weaker interaction between cathodic electrons and the reduction of Cu(II)
255 through the mediation of these two species.

256 The reductive peak currents, at a Cu(II) concentration of 5 mg/L, observed on
257 the cathodes covered by the EAB were lower than values registered with the abiotic
258 cathode (0.973 mA) with the exception of JY6 (Table S3), suggesting some degree
259 of mass transfer inhibition for Cu(II) due to the contact between the EAB and the

260 electrode surface [47]. At a higher concentration of Cu(II) (20 mg/L), the mass
261 transfer inhibition became less significant, as expected. Similar observations have
262 been reported for the reduction of other electron acceptors such as Cr(VI) and Co(II)
263 in mixed culture cathodes [41,43].

264 The lack of a significant difference observed between CVs of the abiotic controls
265 and the biotic cathodes in the absence of Cu(II) (Fig. S4), in concert, reflected the
266 importance of Cu(II) ions on the occurrence of reduction reactions on the EAB,
267 despite the expected variability due to the redox species present on the surfaces of
268 these EAB cells (Insets in Fig. S4).

269

270 3.3 Electrode morphology and product analysis

271 SEM examination showed that the EAB covered the surface of the cathodes only
272 sparsely (Fig. S5A, D, G, and J). EDS analysis confirmed the presence of Cu
273 precipitates on the surfaces of EAB cells (Fig. S5B, E, H and K) while no Cu, or very
274 little Cu precipitate, was observed on the bare surface of the electrodes (Fig. S5C, F, I
275 and L). EDS detection of carbon, oxygen, sodium and phosphorus was attributed to
276 the cellular components of EAB on the electrodes, while gold was associated with the
277 sample pretreatment.

278 XPS analyses (Fig. S6) indicated that the whole Cu2p region comprises 2p_{1/2}
279 and 2p_{3/2} peaks, while only the Cu2p_{3/2} peaks could be used for the assignment of
280 copper chemical states [49]. The abiotic control reported the exclusive presence of
281 Cu(0) (Fig. S6A), shown with its characteristic peak at the Cu2p_{3/2} region of 932.4
282 eV [49], while under OCC only adsorbed Cu(II) was observed (Fig. S6B), as expected.
283 This result clearly demonstrates the importance of the effect of circuital current on the
284 reduction of Cu(II) to Cu(0) with the abiotic cathodes.

285

Here Fig. 3

286 The XPS analysis on the EAB cathodes in the presence of a circuital current (Fig.
287 3), reported the exclusive presence of Cu(0), while under OCCs, both Cu(0) and Cu(II)
288 were observed for JY1 (Fig. 4A) and JY5 (Fig. 4C), and only Cu(II) for both JY3 (Fig.
289 4B) and JY6 (Fig. 4D). JY5 had a net Cu(0) production of 1.81 ± 0.11 mg and JY1
290 exhibited a 1.45 ± 0.05 mg, both of which were nearly equivalent to the sum of $1.17 \pm$
291 0.07 mg in the abiotic controls and 0.70 ± 0.09 mg (JY5) or 0.44 ± 0.03 mg (JY1) in
292 the absence of a circuital current (Table S4). These results in concert confirm the
293 weak correlation between circuital current and the rate of Cu(II) reduction for both
294 JY1 and JY5, which is consistent with the results shown in Fig. 1. The observation of
295 Cu(0) in JY1 in the absence of a circuital current is consistent with previous studies,
296 where *S. maltophilia* converted Cu(II) into Cu(0) under facultative conditions [22-24].

297

Here Fig. 4

298

299 3.4 Effect of electron transfer inhibitors (rotenone and DNP)

300

Here Fig. 5

301 In the presence of either rotenone or DNP, the rate of Cu(II) reduction (Fig. 5A)
302 or the circuital current (Fig. 5B) registered in the MFCs with JY1 or JY5 EAB,
303 changed little, suggesting a weak correlation between the cellular electron transfer
304 processes and either Cu(II) reduction or the circuital current. Conversely, the cathode
305 with the JY6 species, returned an appreciable decrease in both the rate of Cu(II)
306 reduction and circuital current, suggesting a strong interaction between the cellular
307 electron transfer processes in JY6 and either Cu(II) reduction or circuital current. This
308 strong interaction observed with JY6 rather than with JY1, JY3 and JY5, was also
309 supported by the apparent decrease in cathodic electrons used for Cu(II) reduction in
310 the former, in the presence of rotenone or DNP, while little change in was observed
311 with the other three EAB (Table S2). The negative effects of rotenone or DNP
312 electron transfer inhibitors on JY6 was also reflected by a decrease in the voltage
313 output (Fig. S7A and B), maximum power density (Fig. S7C and D) and cathode
314 potential (Fig. S7E and F), in addition to the negative shifts observed in reductive
315 onset potential, reductive peak potential and reductive peak current (Table S3; Fig.
316 S8). In contrast, little change on the above characterization parameters was observed
317 for JY1, JY3 and JY5. These results further support the weak dependence between the
318 cellular electron transfer processes and either Cu(II) reduction or circuital current for
319 JY1, JY3 and JY5, and confirm the significant correlation observed between the
320 cellular electron transfer processes and either Cu(II) reduction or circuital current for
321 JY6. The findings of this study are summarized graphically in Fig. 6.

322 **Here Fig. 6**

323 **4 Conclusions**

324 Metal reduction in MFCs is known to be dependent upon the availability of
325 cathodic electrons and upon the composition of bacterial communities on the
326 biocathodes [11,15,40]. On the basis of the results obtained with indigenous EAB JY1,
327 JY3, JY5 and JY6 isolated from well adapted mixed cultures grown on the surface of
328 MFC cathodes used for Cu(II) reduction, this study demonstrates the close correlation
329 among circuital current, the rate of Cu(II) reduction and the cellular electron transfer
330 processes for JY6, and the weak dependence of these for JY1 and JY5 (Fig. 6). We
331 therefore suggest the possibility of a mechanism involving direct electron transfer
332 from the surfaces of the cathodes to JY6, followed by the subsequent cellular electron
333 transfer to Cu(II) for its reduction. This mechanism is not reflected in JY3, which only
334 exhibited a close correlation between circuital current and the rate of Cu(II) reduction
335 (Fig. 6). In summary, this study provides an evidence of the diverse functions played
336 by these EAB species in the mixed cultures and the corresponding effect on MFC
337 characterization parameters. The results in this study add to a deeper understanding of
338 the capabilities exerted by diverse EAB associated with Cu(II) reduction, and provide
339 new insights into the potential application of metallurgical biocathode MFCs for Cu(II)
340 recovery at industrial scale.

341

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502 **Figure captions**

503 **Fig. 1** Comparison of Cu(II) removal rate (A) and circuit current (B) with various
504 EAB at an initial Cu(II) of either 5 mg/L or 20 mg/L.

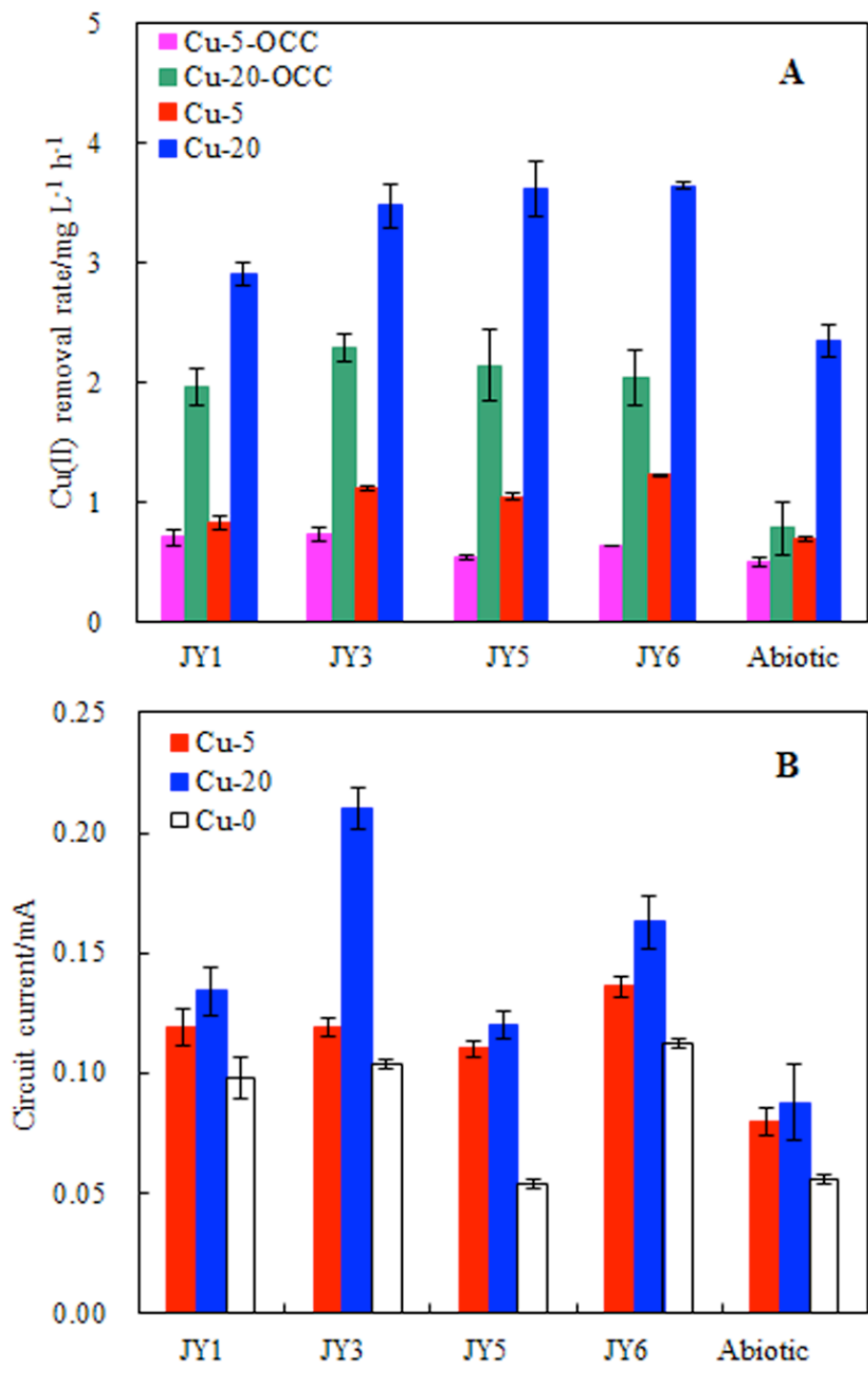
505 **Fig. 2** Voltage output (A and B), power density (C and D) as a function of current
506 density with various EAB at an initial Cu(II) of 5 mg/L (A and C) or 20 mg/L (B and
507 D).

508 **Fig. 3** XPS spectra of Cu precipitates on the cathodes catalyzed by EAB of JY1 (A),
509 JY3 (B), JY5 (C) or JY6 (D) (initial Cu(II): 20 mg/L; 20 batch cycles).

510 **Fig. 4** XPS spectra of Cu precipitates on the cathodes catalyzed by EAB of JY1 (A),
511 JY3 (B), JY5 (C) or JY6 (D) in the absence of circuit current (initial Cu(II): 20
512 mg/L; 20 batch cycles).

513 **Fig. 5** Comparison of Cu(II) removal rate (A) and circuit current (B) in response to
514 the inhibitor of rotenone or DNP (initial Cu(II): 20 mg/L).

515 **Fig. 6** Summary of correlation between circuit current, Cu(II) reduction and cellular
516 electron transfer in EAB of JY1, JY3, JY5 and JY6.

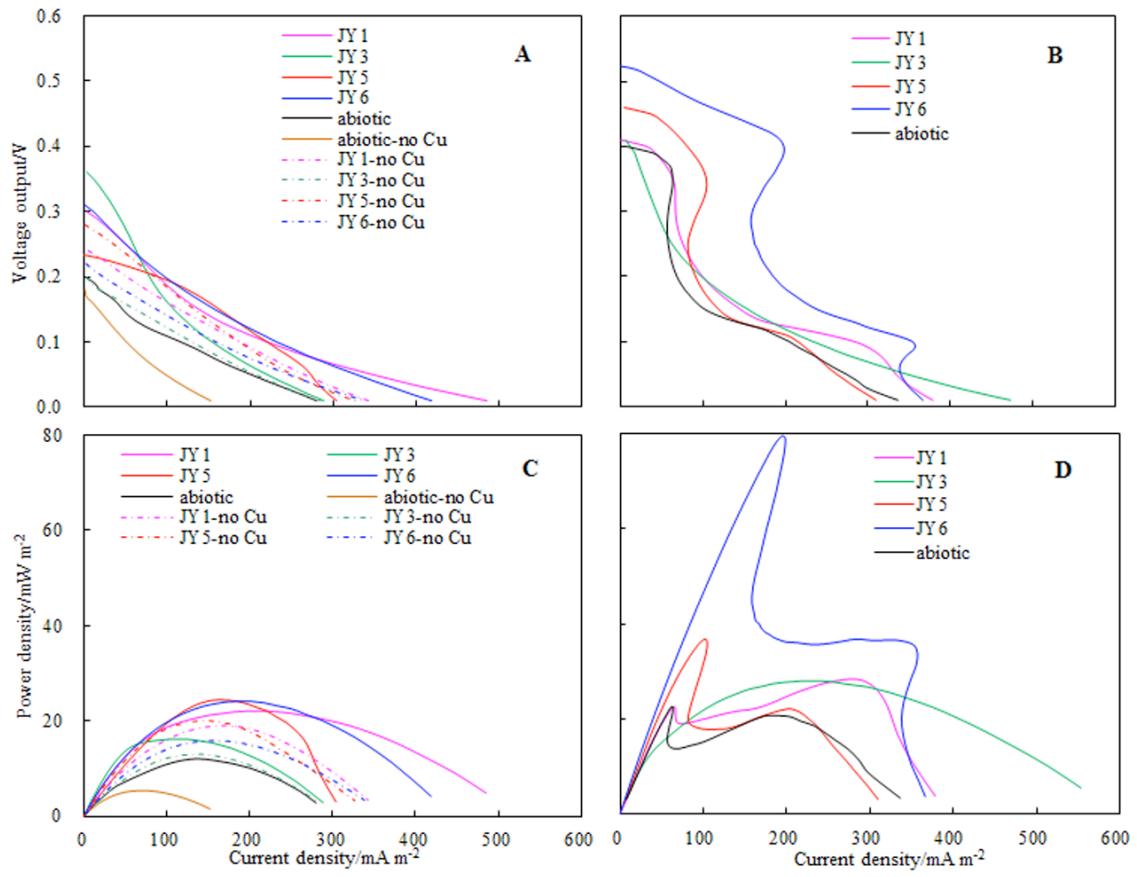


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519 Figure 1

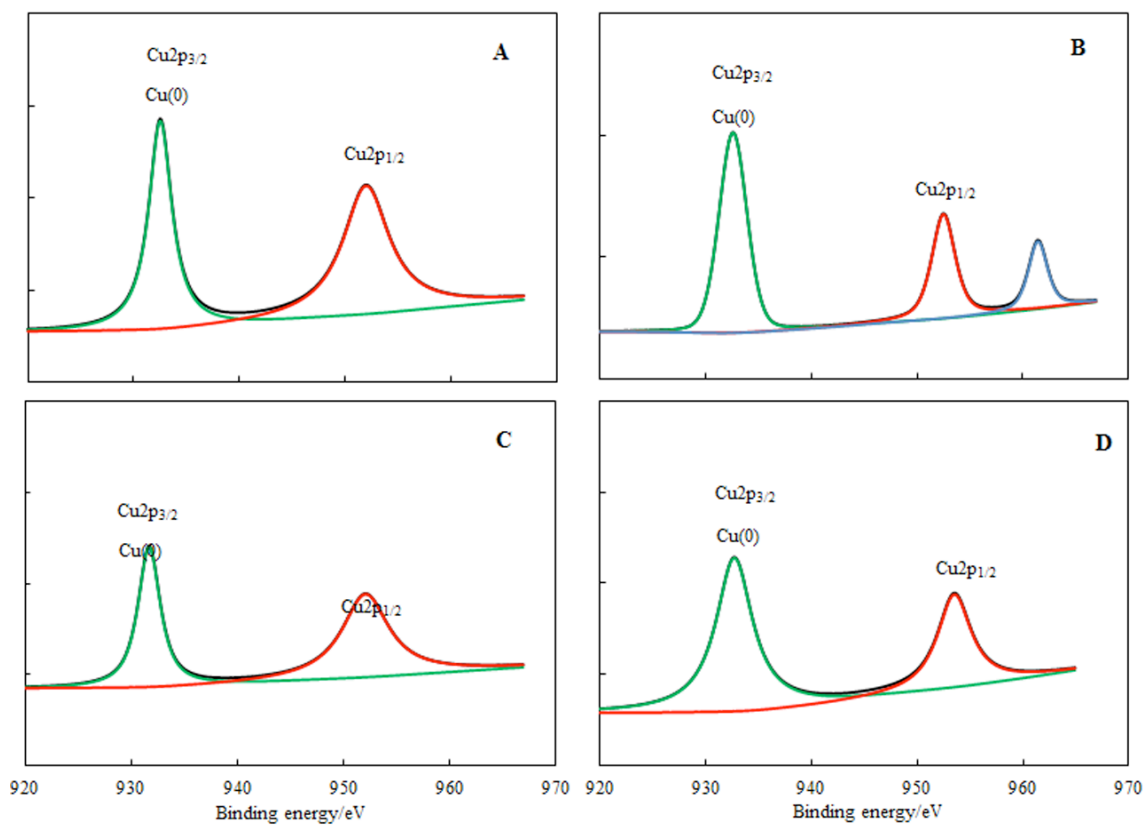
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522 **Figure 2**

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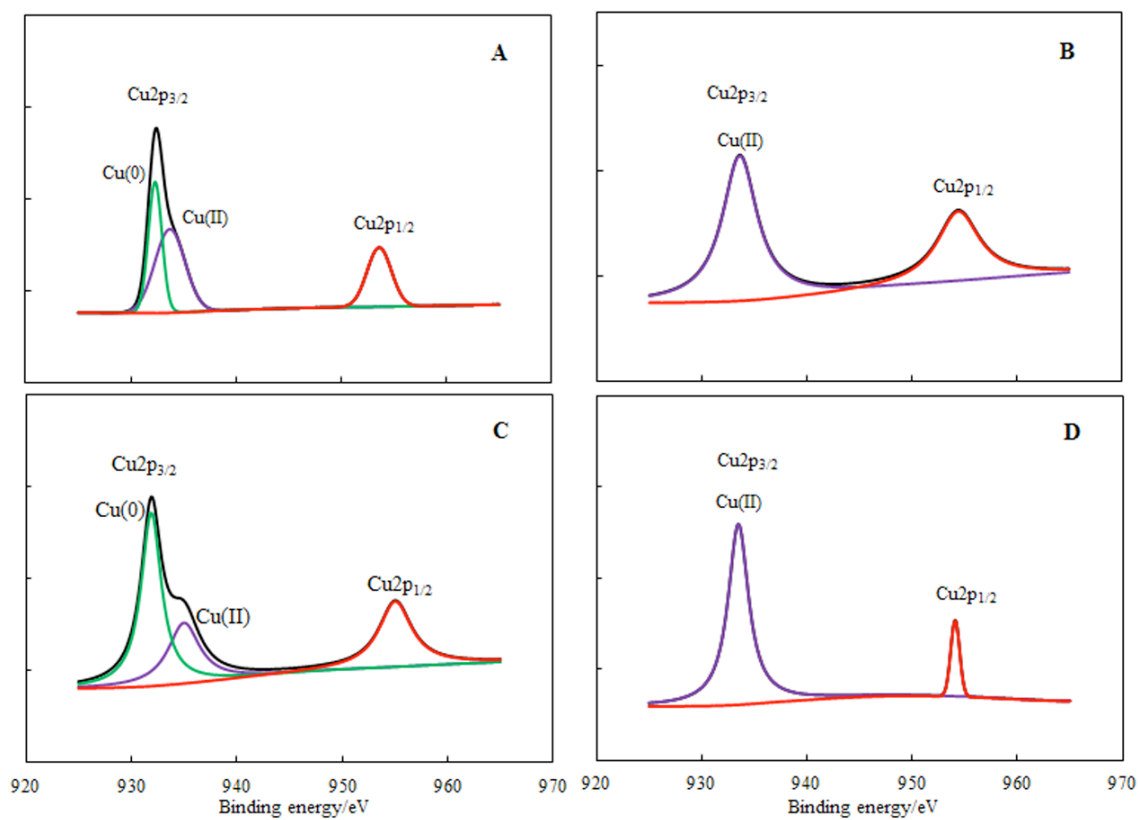


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Figure 3

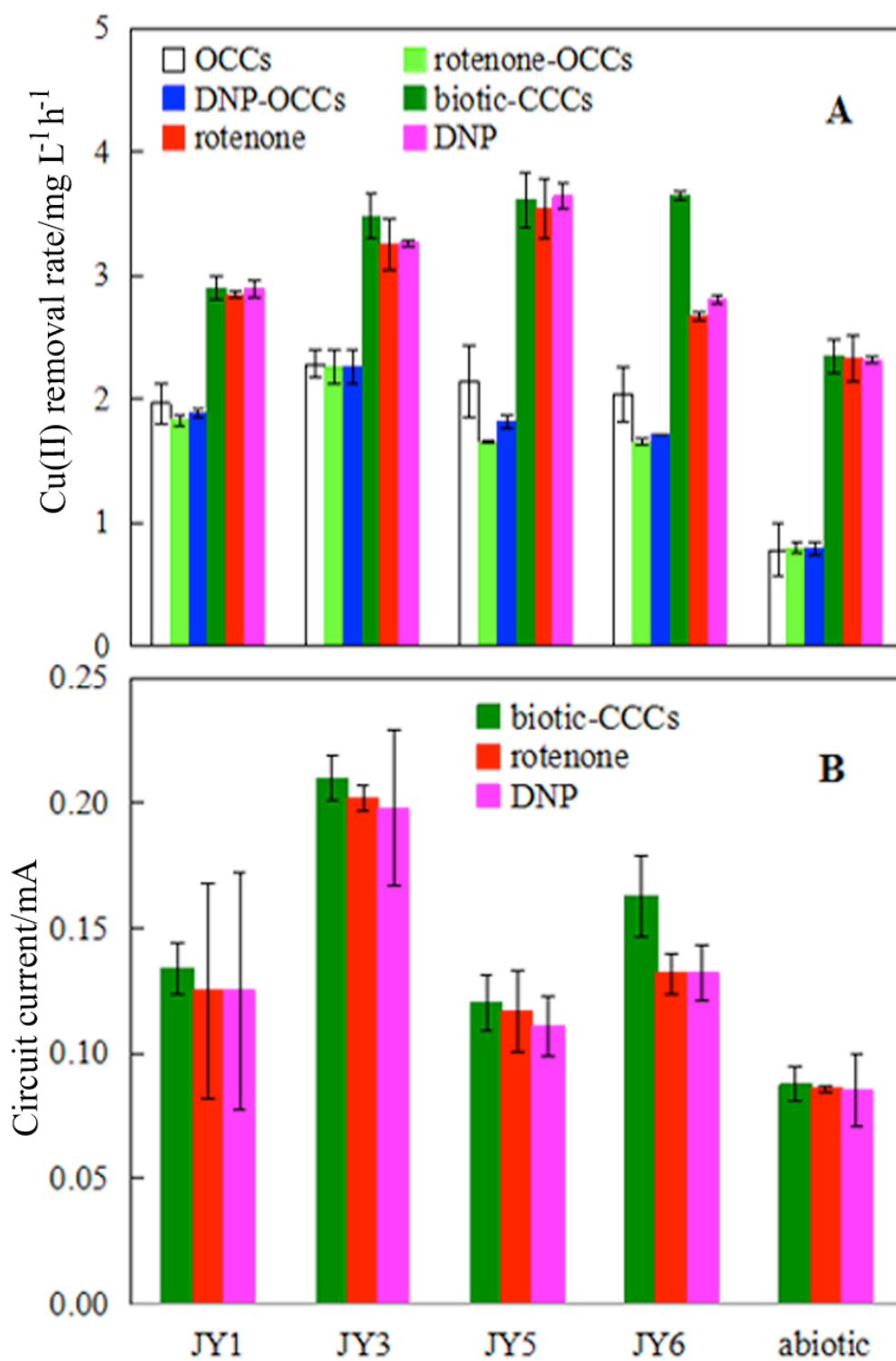
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528 Figure 4

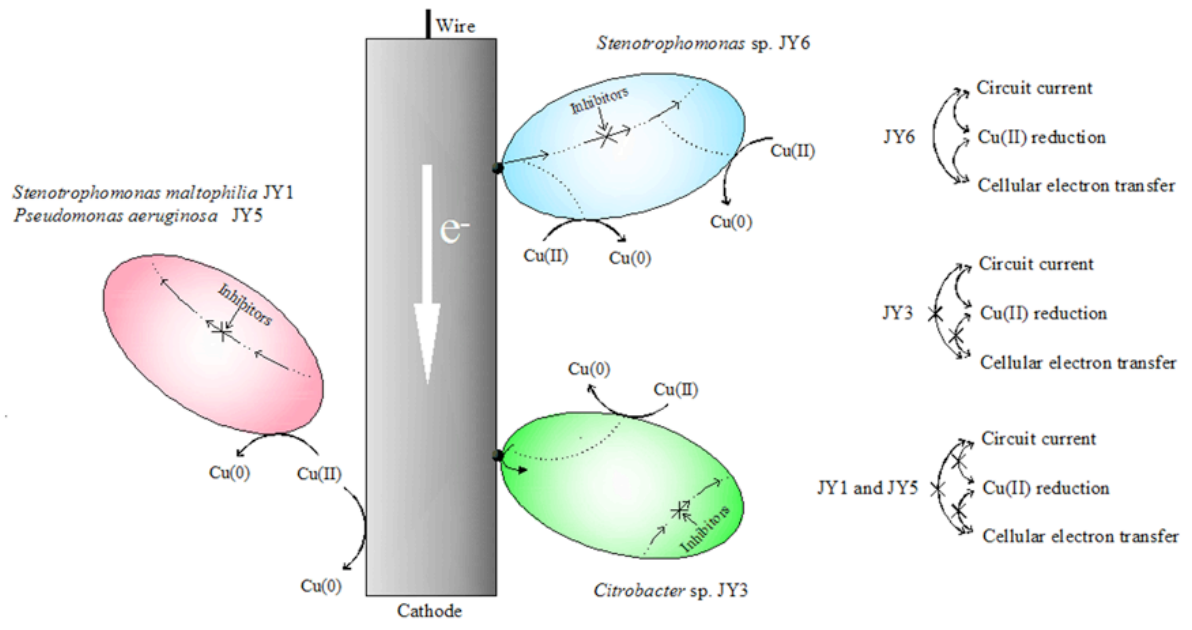
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531 Figure 5

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535 Figure 6